

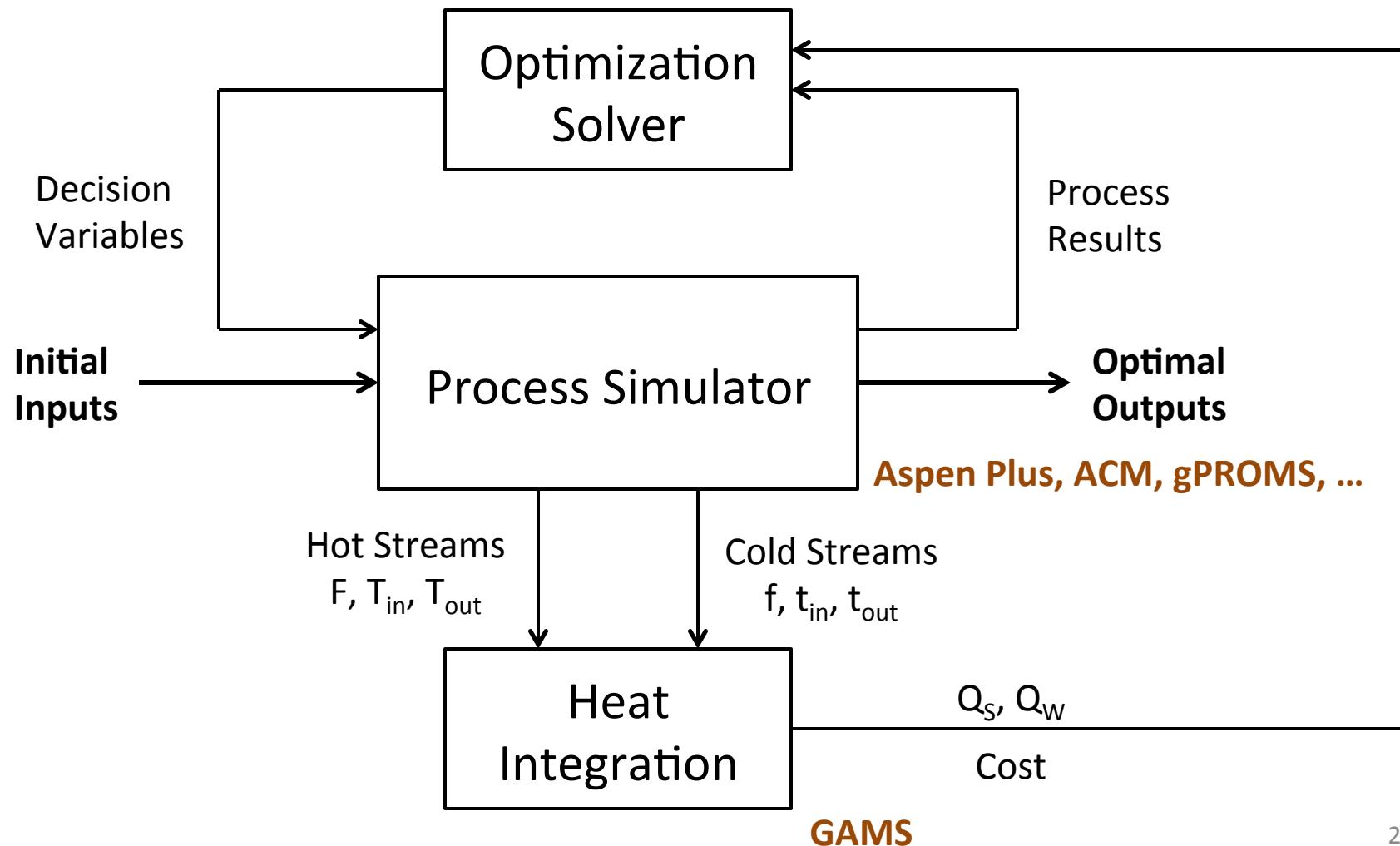
Optimization and Heat Integration in Simulation Models

Yang Chen
Ignacio Grossmann
David Miller

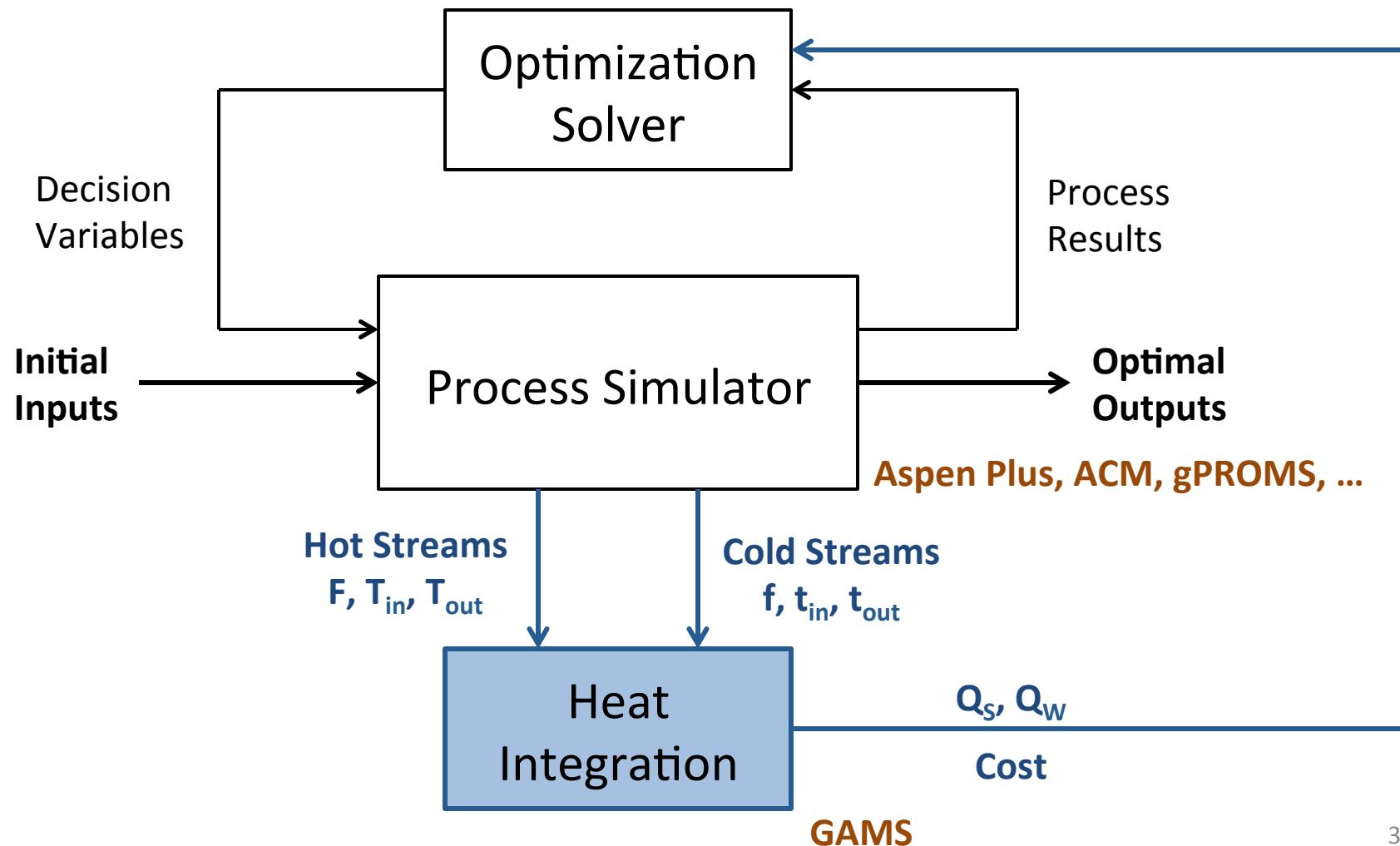
March 10, 2013



Simulation-Based Optimization Framework



Simulation-Based Optimization Framework



Transshipment Model

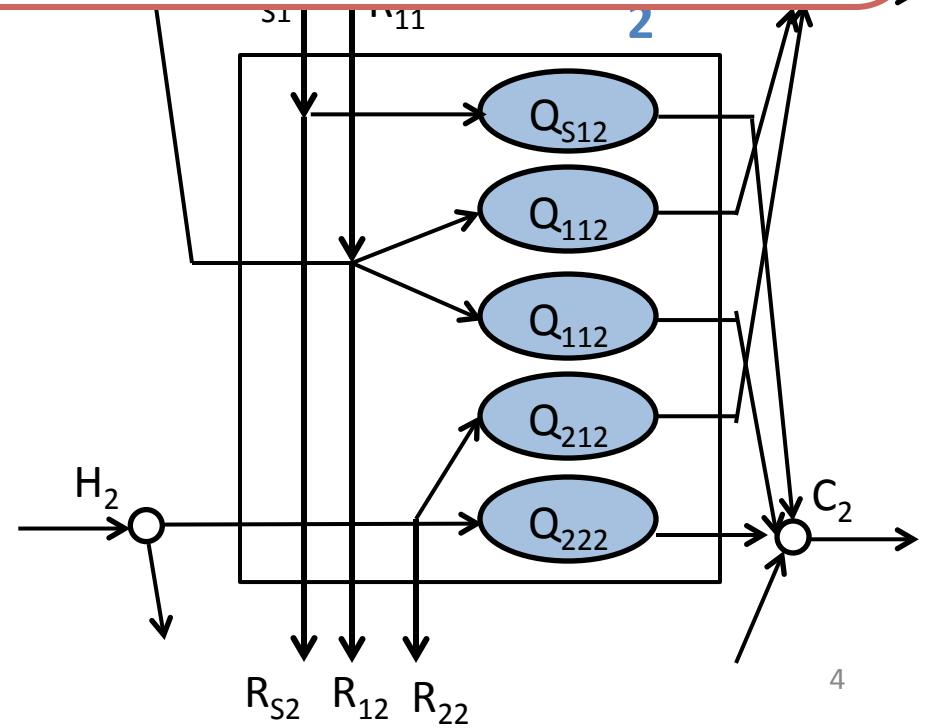
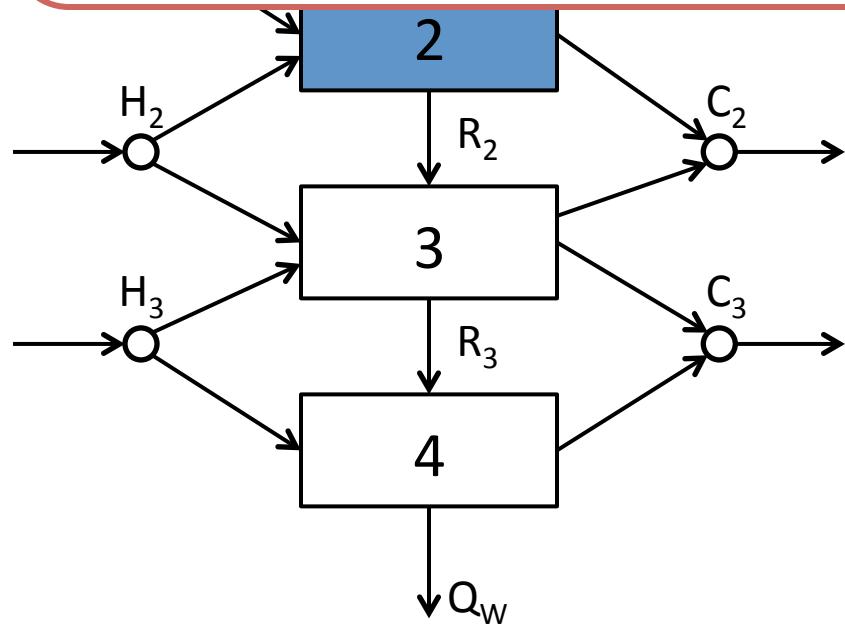
Compact

Expanded

$\int Q_S$

1

Extend to multiple utilities (HP, MP, LP steams, fuels, cooling water, refrigeration)



Transshipment Model (LP Version)

- 1st Step: LP transshipment model
 - Minimum hot and cold utility consumption
 - Minimum utility cost

$$\min Z = \sum_{m \in S} c_m Q_m^S + \sum_{n \in W} c_n Q_n^W$$

$$\text{s.t. } R_{ik} - R_{i,k-1} + \sum_{j \in C_k} Q_{ijk} + \sum_{n \in W_k} Q_{ink} = Q_{ik}^H \quad i \in H'_k$$

$$R_{mk} - R_{m,k-1} + \sum_{j \in C_k} Q_{mjk} - Q_m^S = 0 \quad m \in S'_k$$

$$\sum_{i \in H_k} Q_{ijk} + \sum_{m \in S_k} Q_{mjk} = Q_{jk}^C \quad j \in C_k$$

$$\sum_{i \in H_k} Q_{ink} - Q_n^W = 0 \quad n \in W_k \quad k = 1, \dots, K$$

$$R_{ik}, R_{mk}, Q_{ijk}, Q_{mjk}, Q_{ink}, Q_m^S, Q_n^W \geq 0$$

$$R_{i0} = R_{iK} = 0$$

Q^S	heat load of hot utility
Q^W	heat load of cold utility
Q	exchange of heat
R	heat residual
c	unit cost of utility
k	temperature interval
i	hot process stream
j	cold process stream
m	hot utility
n	cold utility

Transshipment Model (MILP Version)

- 2nd Step: MILP transshipment model
 - Matches between process streams and utilities
 - Minimum number of heat exchangers
 - Minimum capital cost for heat exchange

network

$$\min \sum_{i \in H} \sum_{j \in C} y_{ij}^q$$

$$\text{s.t. } R_{ik} - R_{i,k-1} + \sum_{j \in C_k} Q_{ijk} = Q_{ik}^H \quad i \in H'_k$$

$$\sum_{i \in H_k} Q_{ijk} = Q_{jk}^C \quad j \in C_k \quad k = 1, \dots, K_q$$

$$\sum_{k=1}^{K_q} Q_{ijk} - U_{ij} y_{ij}^q \leq 0$$

$$R_{ik}, Q_{ijk} \geq 0$$

y	stream match
Q	exchange of heat
R	heat residual
U	upper bound of heat load
q	subnetwork
k	temperature interval
i	hot stream
j	cold stream

Case Study Problems – Similar Flows (FCp)

	Hot Streams			Cold Streams		
	FCp (MW/°C)	Tin (°C)	Tout (°C)	FCp (MW/°C)	Tin (°C)	Tout (°C)
1	1	400	120	1	1.5	160
2	2	340	120	2	1.3	100
3	1.5	380	150	3	2.5	50
4	2.5	300	100	4	2.8	200
5	1.7	420	160	5	1.9	150
6	0.8	390	110	6	0.8	100
7	1.2	360	200	7	1.7	200
8	1.8	280	130	8	1.6	120
9	1.1	250	80	9	0.9	110
10	1.3	330	170	10	2.1	190
11	2.1	430	300	11	1.8	260
12	2.2	200	100	12	1.2	80
13	1.2	150	70	13	1.6	130
14	1.6	330	180	14	1.4	180
15	1.9	370	115	15	2	155
16	1.4	355	105	16	1	95
17	0.9	310	130	17	1.1	175
18	1.3	260	90	18	1.5	130
19	1.1	300	115	19	2.2	210
20	2.3	265	190	20	1.7	230

Steam: HP 500°C, MP 350°C

Cooling Water: 20 - 50°C

Case Study Problems – Dissimilar Flows (FCp)

	Hot Streams			Cold Streams		
	FCp (MW/°C)	Tin (°C)	Tout (°C)	FCp (MW/°C)	Tin (°C)	Tout (°C)
1	6	400	120	1	14	160
2	2	340	120	2	3	100
3	0.5	380	150	3	0.4	50
4	8	300	100	4	2.5	200
5	3	420	160	5	2	150
6	4	390	110	6	6	100
7	0.2	360	200	7	1.5	200
8	0.6	280	130	8	0.2	120
9	1.5	250	80	9	5.5	110
10	4	330	170	10	3	190
11	12	430	300	11	8	260
12	8	200	100	12	12	80
13	5	150	70	13	0.3	130
14	0.6	330	180	14	4.5	180
15	0.3	370	115	15	1	155
16	6	355	105	16	0.1	95
17	0.9	310	130	17	7	175
18	3	260	90	18	2	130
19	1	300	115	19	0.5	210
20	0.3	265	190	20	1.7	230

Steam: HP 500°C, MP 350°C

Cooling Water: 20 - 50°C

Case Study Results – Similar Flows (FCp)

Problem Size # of Hot Streams * # of Cold Stream	LP Transshipment Model				MILP Transshipment Model			
	# of Continuous Variables	QS (MW)	QW (MW)	CPU Time (seconds)	# of Continuous Variables	# of Binary Variables	Minimum Matches	CPU Time (seconds)
2 * 2	38	45	210	0.031	38	10	8	0.156
3 * 3	72	115	0	0.031	72	17	8	0.047
5 * 5	235	307	60	0.031	235	67	24	0.421
10 * 10	1057	474	197	0.031	1057	219	42	1059.309
15 * 15	2692	711	391.5	0.031	2692	421	(57)	-----
20 * 20	6284	1473	684.5	0.031	6284	778	(83)	-----

----- : global optimal solution was not obtained within 100,000 seconds.

Case Study Results – Dissimilar Flows (FCp)

Problem Size # of Hot Streams * # of Cold Stream	LP Transshipment Model				MILP Transshipment Model			
	# of Continuous Variables	QS (MW)	QW (MW)	CPU Time (seconds)	# of Continuous Variables	# of Binary Variables	Minimum Matches	CPU Time (seconds)
2 * 2	38	1910	220	0.047	38	12	9	0.187
3 * 3	72	1861	186	0.031	72	24	14	0.189
5 * 5	235	1105	760	0.031	235	67	26	0.311
10 * 10	1057	825	755	0.047	1057	196	39	23.104
15 * 15	2692	786	514.5	0.016	2692	392	55	760.583
20 * 20	6284	1351.5	1283	0.031	6284	712	(81)	-----

----- : global optimal solution was not obtained within 100,000 seconds.

Next Step: Link Heat Integration Tool to Simulators

- Link the heat integration tool (GAMS model) to process simulators (including ACM and Aspen plus) and optimization solver through Python or C-based programs.
- Test some simple ACM models at first.
- Initial demonstration: solid sorbent absorber/regenerator ACM model for CO₂ capture
- Variable FCp: piecewise linear approximation

Disclaimer

This presentation was prepared as an account of work sponsored by an agency of the United States Government under the Department of Energy. Neither the United States Government nor any agency thereof, nor any of their employees, makes any warranty, express or implied, or assumes any legal liability or responsibility for the accuracy, completeness, or usefulness of any information, apparatus, product, or process disclosed, or represents that its use would not infringe privately owned rights. Reference herein to any specific commercial product, process, or service by trade name, trademark, manufacturer, or otherwise does not necessarily constitute or imply its endorsement, recommendation, or favoring by the United States Government or any agency thereof. The views and opinions of authors expressed herein do not necessarily state or reflect those of the United States Government or any agency thereof.