

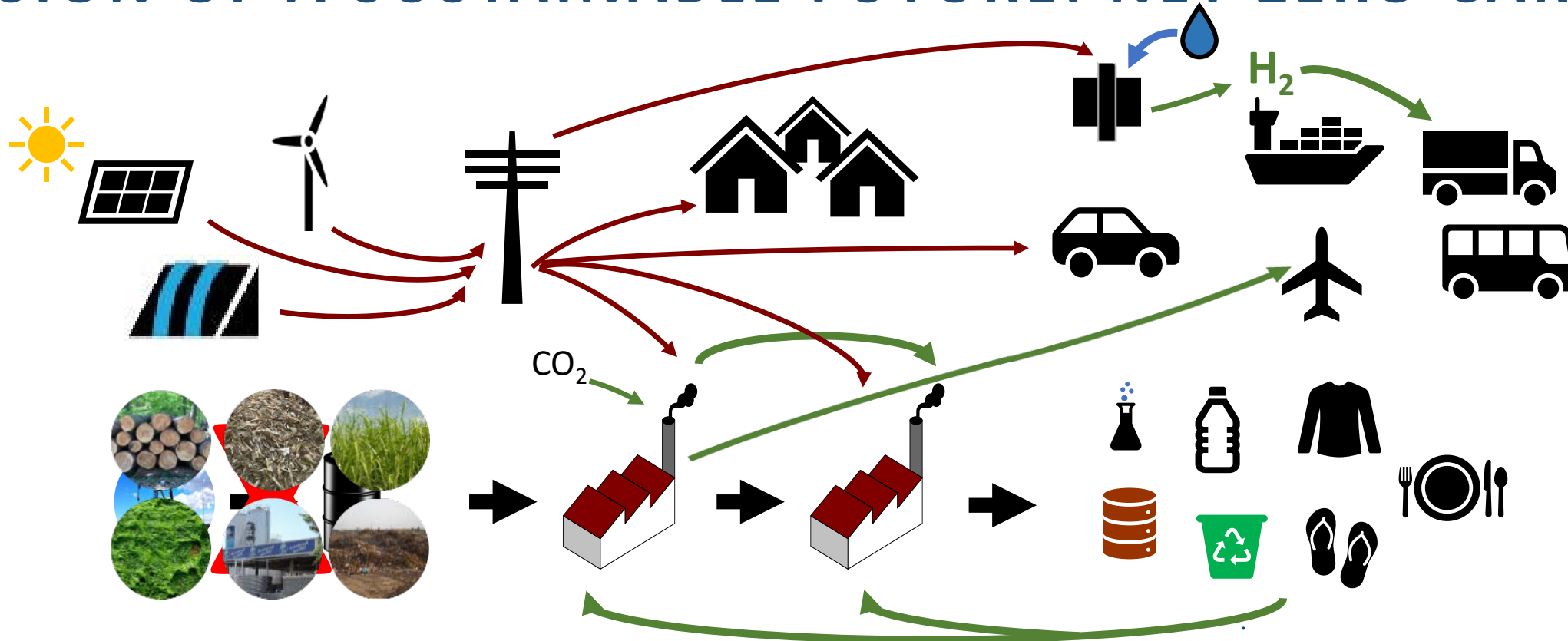


RENEWABLE ENERGY STORAGE AND CONVERSION TOWARDS NET ZERO CARBON ECONOMIES

**Ana Inés Torres - Instituto de Ingeniería Química, Facultad de Ingeniería, UdelaR
Seminar Energy Systems Initiative- CAPD- December 4, 2021**



VISION OF A SUSTAINABLE FUTURE: NET ZERO CARBON



- Energy - electricity : wind, solar, hydropower => houses, industries
 - transportation: electrification → passenger cars
 - low carbon fuels → heavy duty, maritime and aviation
- Chemicals, materials, consumer products: renewable carbon sources

Figure: Wikimedia Commons,

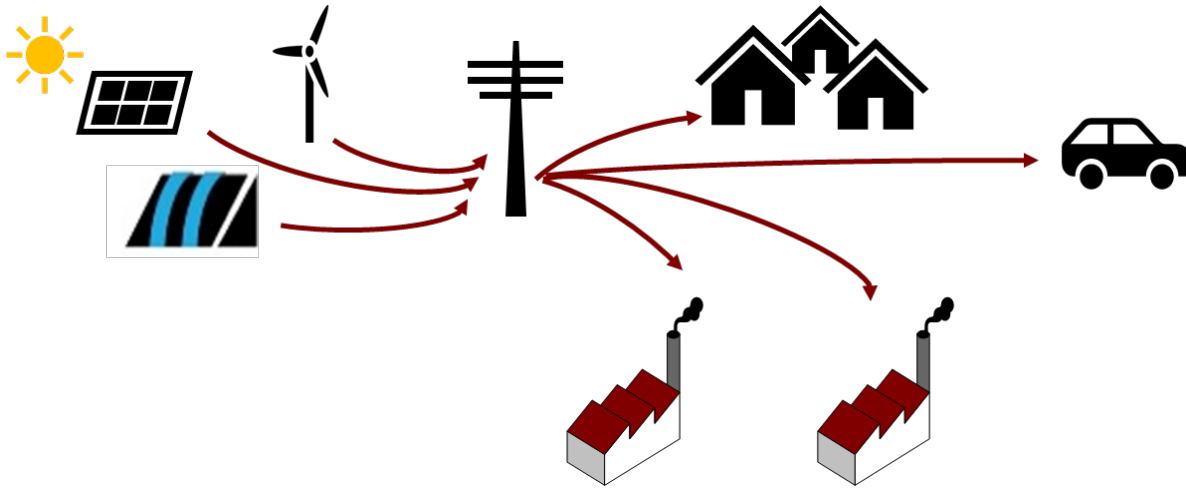
UNITED NATIONS SUSTAINABLE DEVELOPMENT GOALS

- Collection of global goals and targets set for the 2030 Agenda



STATUS: RENEWABLE ENERGY- ELECTRICITY

- RE Sources: already integrated in the grid



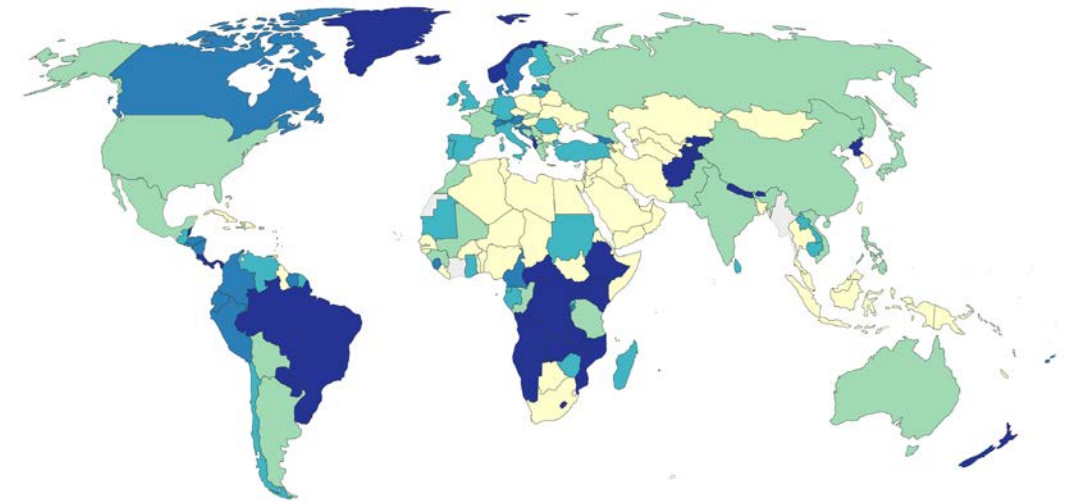
- **Programmable sources:** hydropower, hydrothermal, nuclear, biomass & waste
- **Non-programmable sources:** wind, sun

Figures: Wikimedia Commons,

Share of electricity production from renewables

Renewables includes electricity production from hydropower, solar, wind, biomass, and waste, geothermal, wave and tidal sources.

Our World in Data



Source: Our World in Data based on BP Statistical Review of World Energy & Ember (2021)

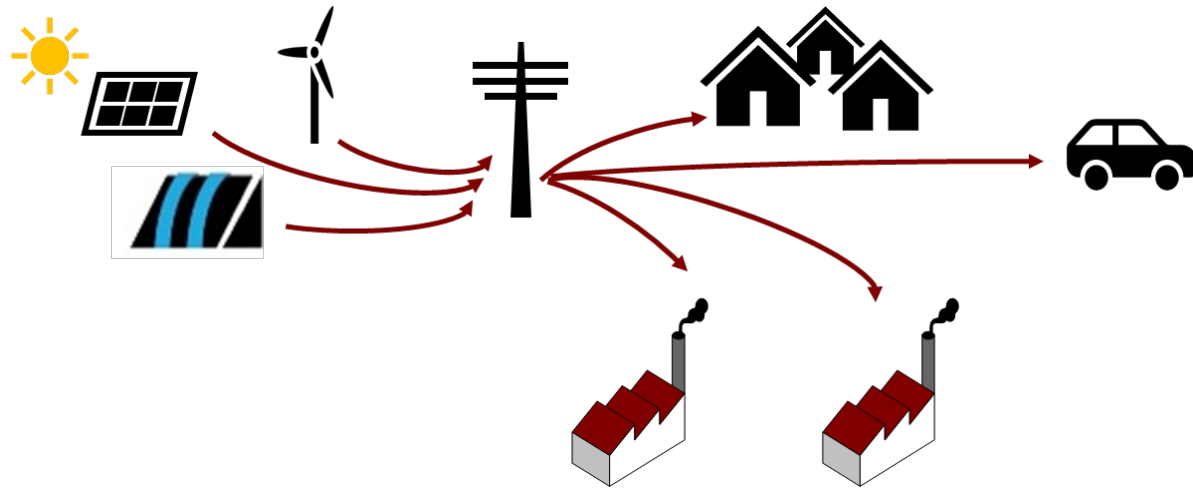
OurWorldInData.org/energy • CC BY

2019: 10 countries > 99% share

Figure: On the basis of Our world in data <https://ourworldindata.org/grapher/share-electricity-renewables>

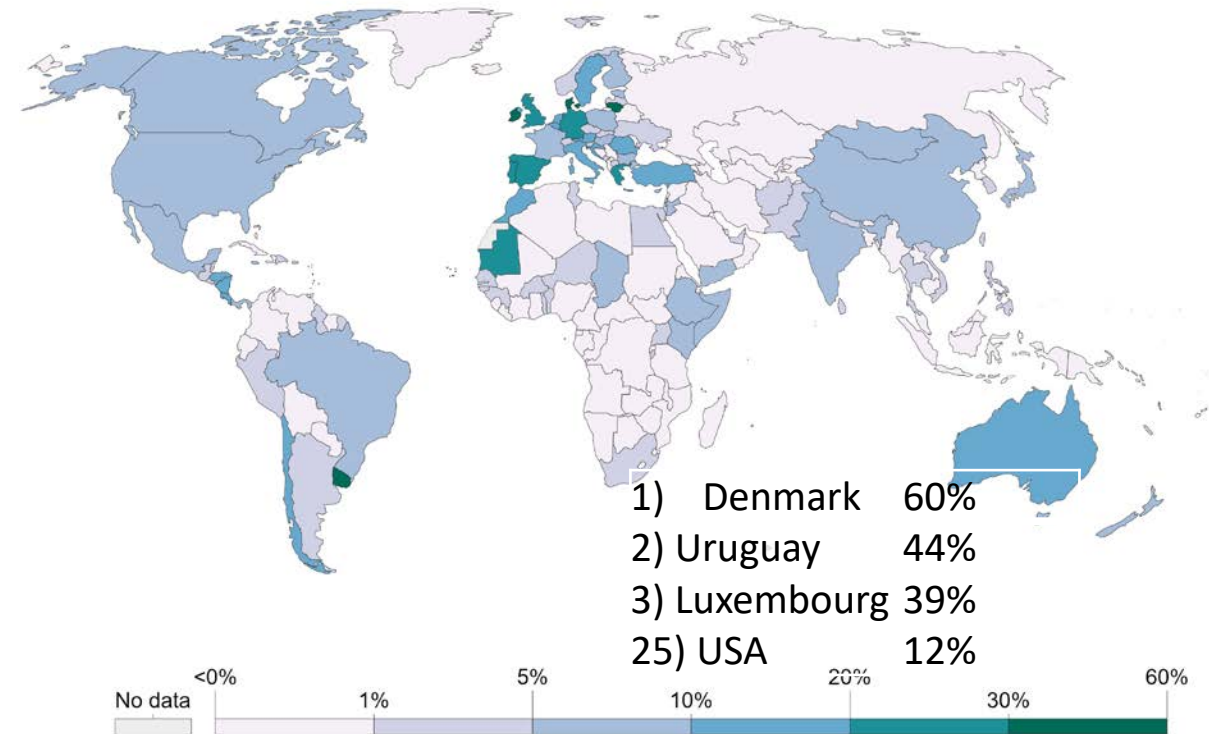
STATUS: RENEWABLE ENERGY- ELECTRICITY

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- **Programmable sources:** hydropower, hydrothermal, nuclear, biomass & waste
- **Non-programmable sources:** wind, sun

Share of wind + solar

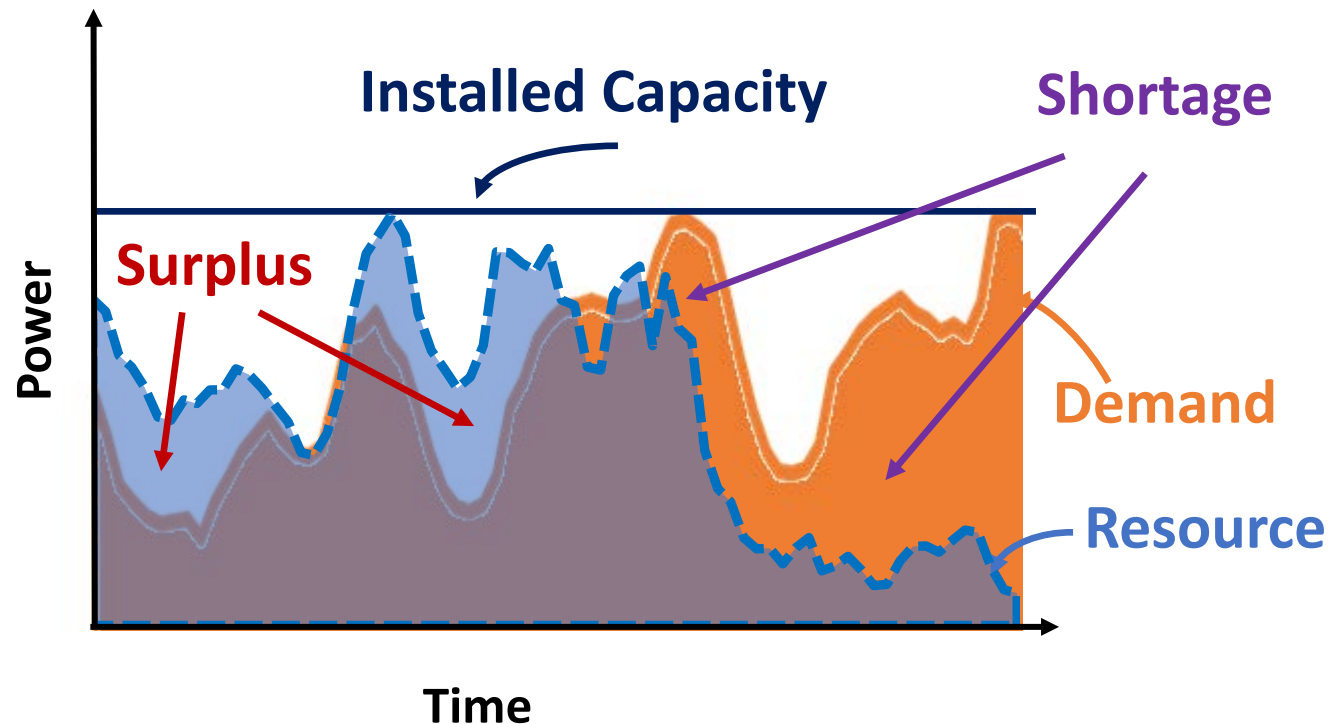


Figures: Wikimedia Commons,

Figure: Our world in data <https://ourworldindata.org/grapher/share-electricity-renewables>

STATUS: RENEWABLE ENERGY-ELECTRICITY

- Modern non-programmable renewable energy sources complicate operations

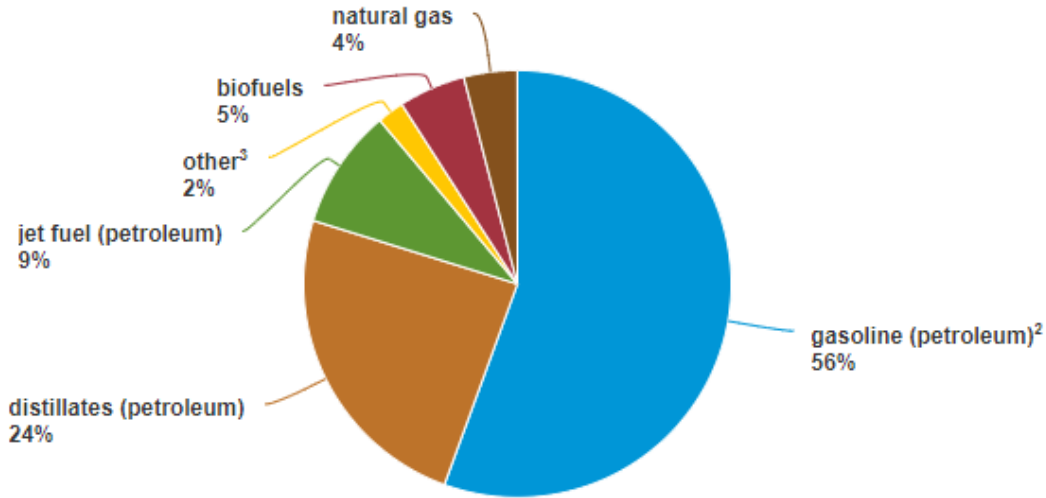


- Large shares of wind/solar energy => imbalances between availability and demand

Challenge: keep growing and use surpluses

STATUS: TRANSPORTATION SECTOR

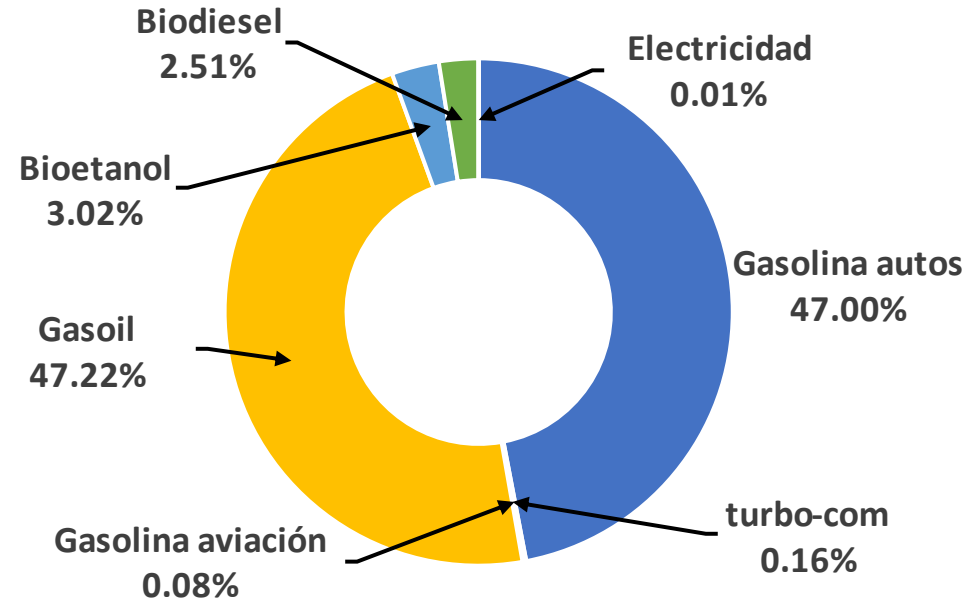
- USA 2020



1. Based on energy content
 2. Motor gasoline and aviation gas; excludes ethanol
 3. Includes residual fuel oil, lubricants, hydrocarbon gas liquids (mostly propane), and electricity (includes electrical system energy losses).
 Source: U.S. Energy Information Administration, *Monthly Energy Review*, Tables 2.5, 3.8c, and 10.2b, April 2021, preliminary data

Note: Sum of individual components may not equal 100% because of independent rounding.

- Uruguay, 2020 ⁽¹⁾



- Europe⁽²⁾: 8% renewables 2018

=> more than 90% fossil based

Challenge: Advance on decarbonization of transportation sector

Figure: <https://www.eia.gov/energyexplained/use-of-energy/transportation.php>

(1) Balance Energético Nacional (MIEM)

(2) Eurostat <https://ec.europa.eu/eurostat/web/products-eurostat-news/-/ddn-20200123-2>

STATUS: CHEMICALS MATERIALS END PRODUCTS

- Bio-refineries: Process biomass into fuels materials and chemicals

• The “Green”

October 2019
SUSTAINABILITY

From traditional to green refinery: The transformation of Eni’s Gela plant

The need for a more sustainable energy mix is setting a challenge for refinery operators.

Gravame, F., Nardi, A., Gioli, G., Corti, F., Baker Hughes

REUTERS®
World Business Legal Markets Breakingviews Technology

August 12, 2021
8:56 PM -03
Last Updated 4 months ago

Middle East

EXCLUSIVE Exxon, Chevron look to make renewable fuels without costly refinery upgrades -sources

By Laura Sanicola

5 minute read



Energy Transition: Total Is Investing to Convert Its Grandpuits Refinery to Biofuels and Bioplastics

Press release - 24 September 2020

... to france’s roadmap for deploying sustainable aviation **fuel** , which calls for an incorporation target into aviation **fuel** of 2% by 2025 and 5% by 2030 . the new unit, to be ... which will contribute to total’s ambition to provide **green** electricity to all its industrial sites in europe . the ...

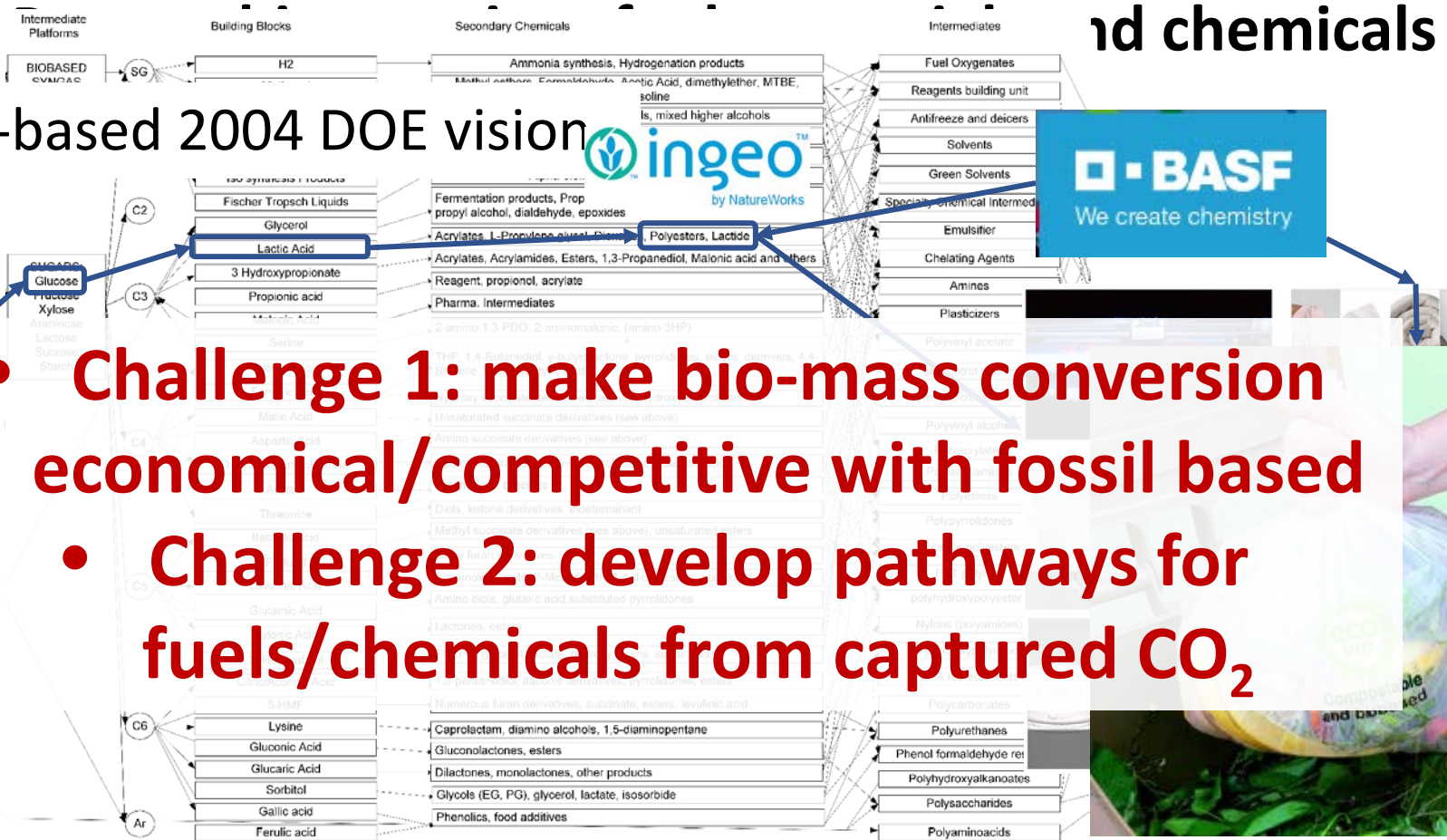
- Popular among oil companies as it uses existing infrastructure
- Keeps petrochemical industry “as is”

Figures: Wikimedia Commons Eni’s website
Honeywell Uop’s website Total’s website

CURRENT STATUS: MATERIALS & CHEMICALS

- **Bio-refineries:**

- The older sugar-based 2004 DOE vision



Challenge 1: make bio-mass conversion economical/competitive with fossil based

Challenge 2: develop pathways for fuels/chemicals from captured CO₂

- Analogues of current petrochemicals
- Popular in industries that already process biomass

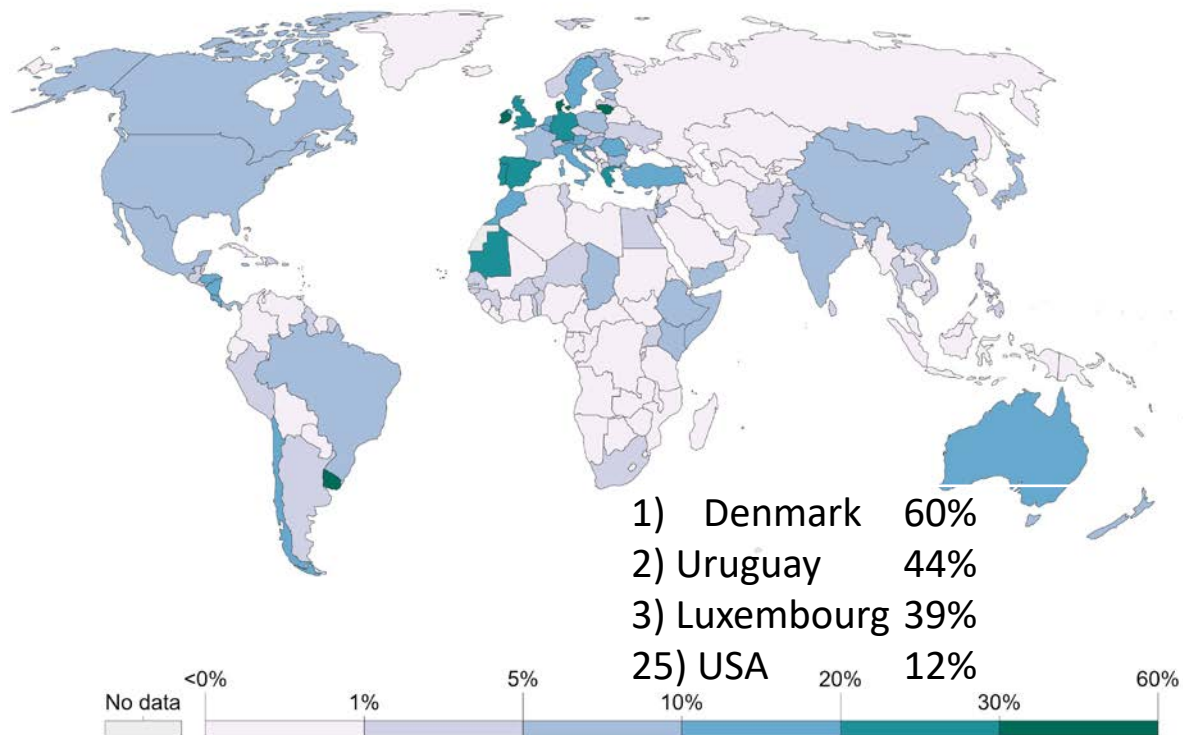
Figures: Wikimedia Commons, Natureworks LLC website, Cargill's website, BASF website

OUTLINE OF THE TALK

- **Research group: Analysis & Development of tools for transitioning to a zero/low carbon future**
- **Today: Processes that may be coupled to intermittent renewable energy (P2X)**
 1. Self-storage as a solution to imbalances between generation and demand: tools for assessing self-storage convenience/TOU policies (P2P)
 2. Production of green-hydrogen using surpluses (P2G): selection of technology and production capacities
 3. Electro-reduction of CO₂: Recent advances in reaction network definition
- **Focus mostly on Uruguay, ideas & discussion useful for other regions**

HOW DID URUGUAY BECAME A LEADER IN RENEWABLE ENERGY?

Share of wind + solar

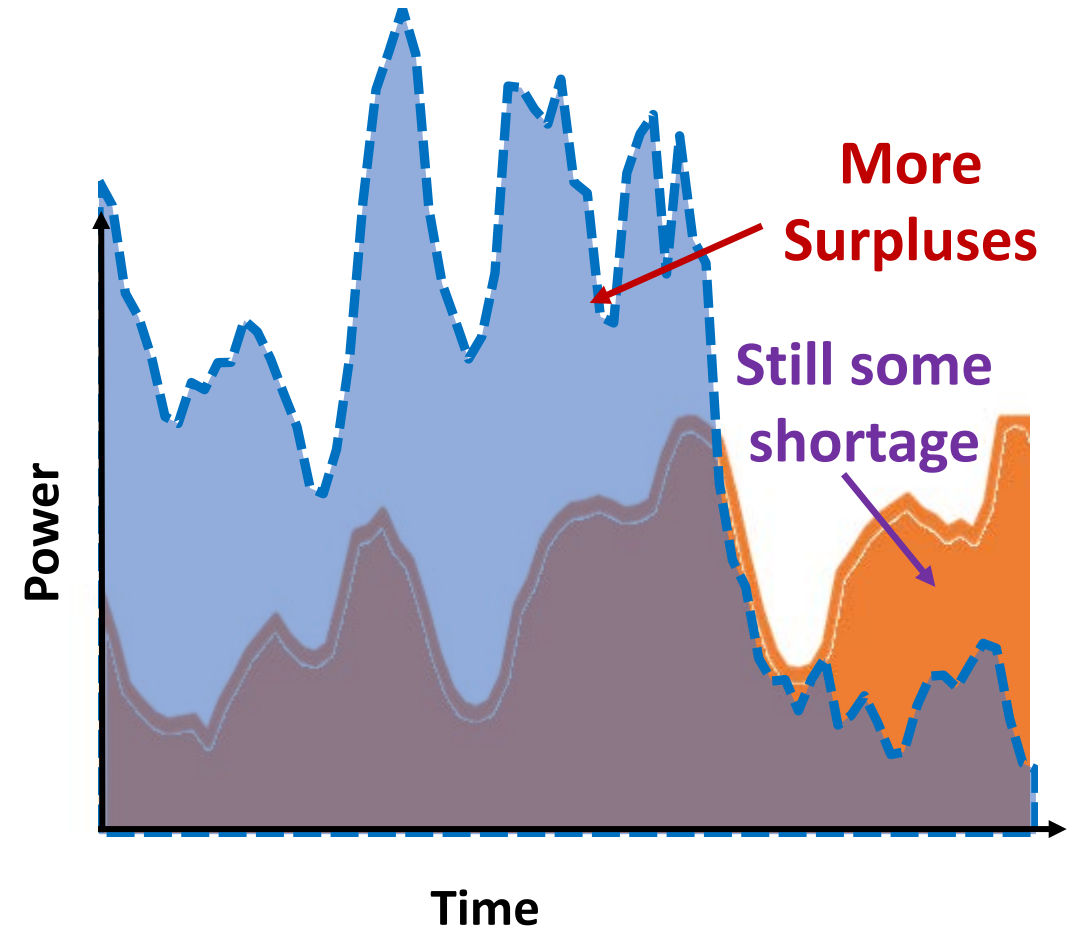
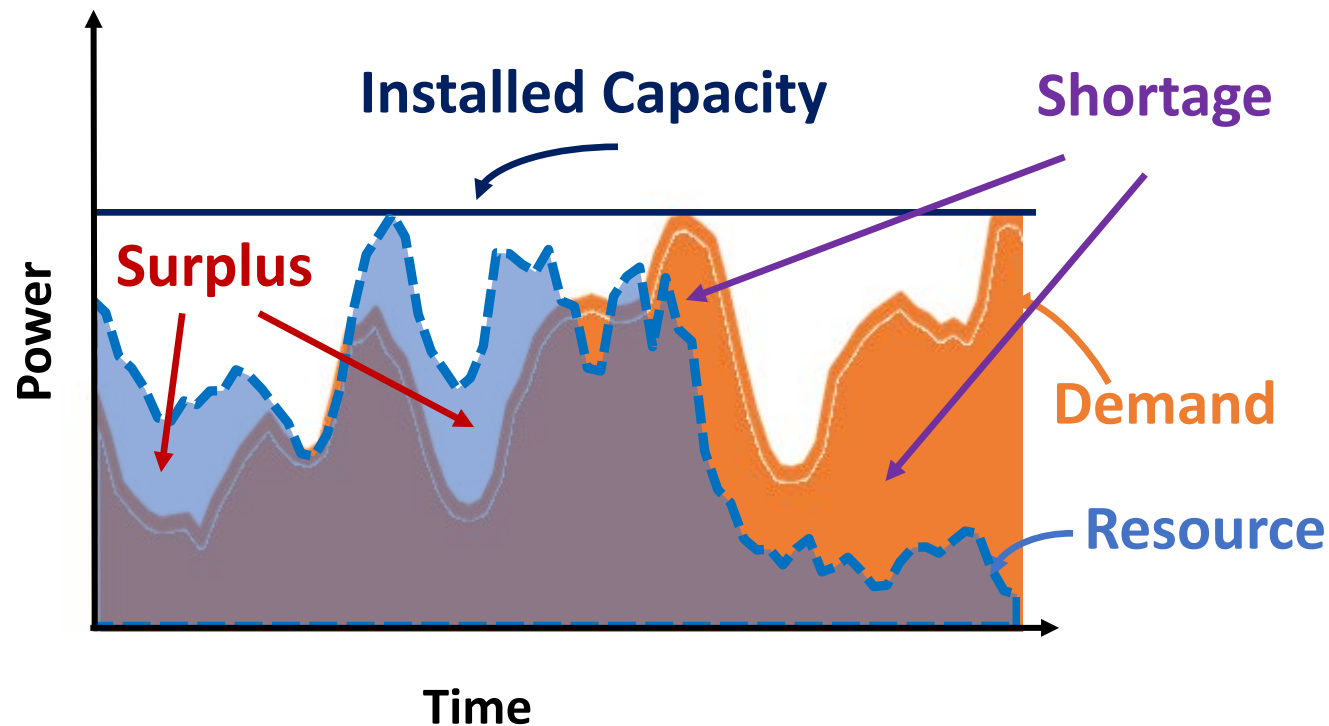


- 0 fossil fuels: import 100% petroleum & gas needs
- 2005: Big energy problem: scheduled blackouts
- 2006: Industries self-generate using biomass -> grid
- 2009: First 10 MW wind park
- 2017: Doubled 2005 generation capacity, 70% non-programmables

Figure: Our world in data <https://ourworldindata.org/grapher/share-electricity-renewables>

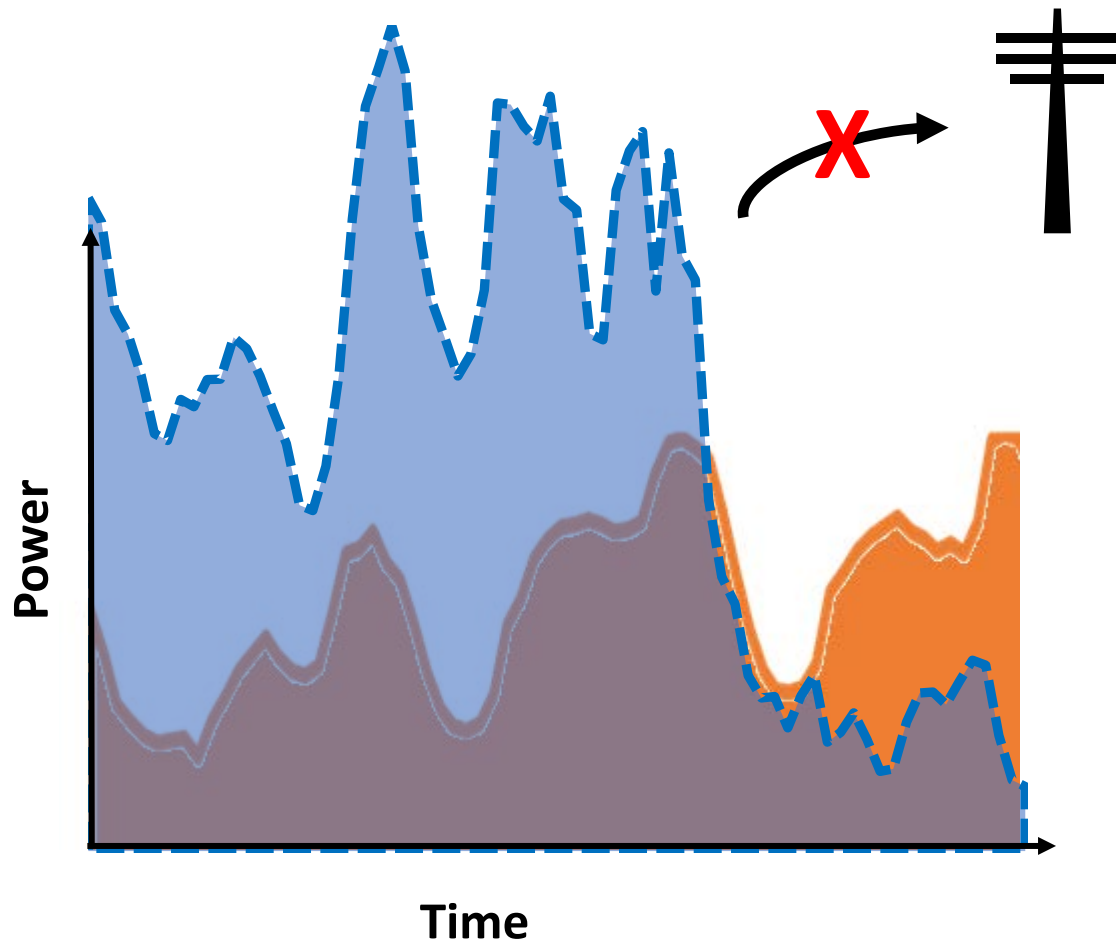
TRANSITION TO RENEWABLE ENERGY

- Not that planned process = > satisfy demand installing very large capacities



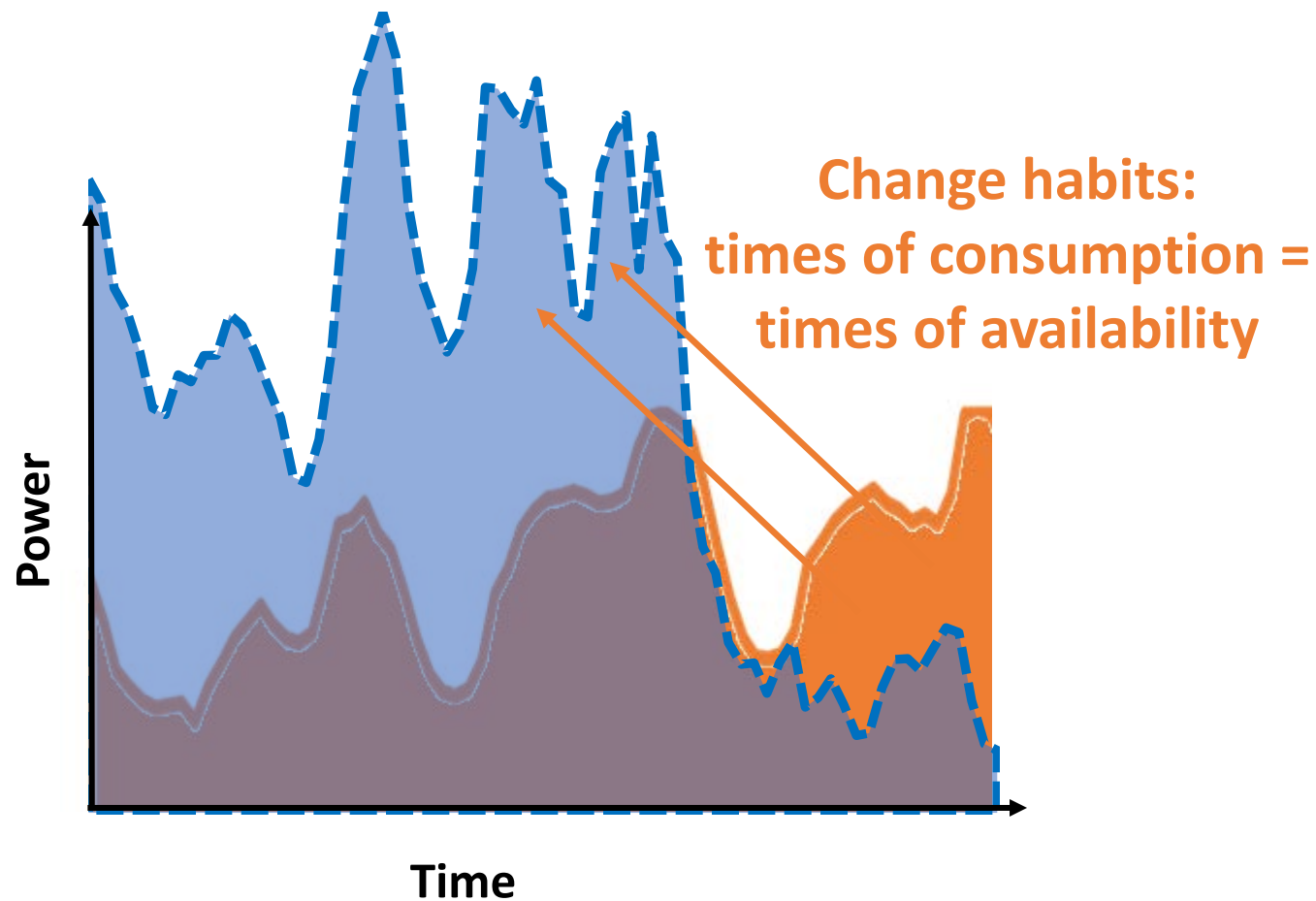
- Planned: Lara et. al, *EJOR*, 2018

OPTIONS TO BALANCE DEMAND AND AVAILABILITY



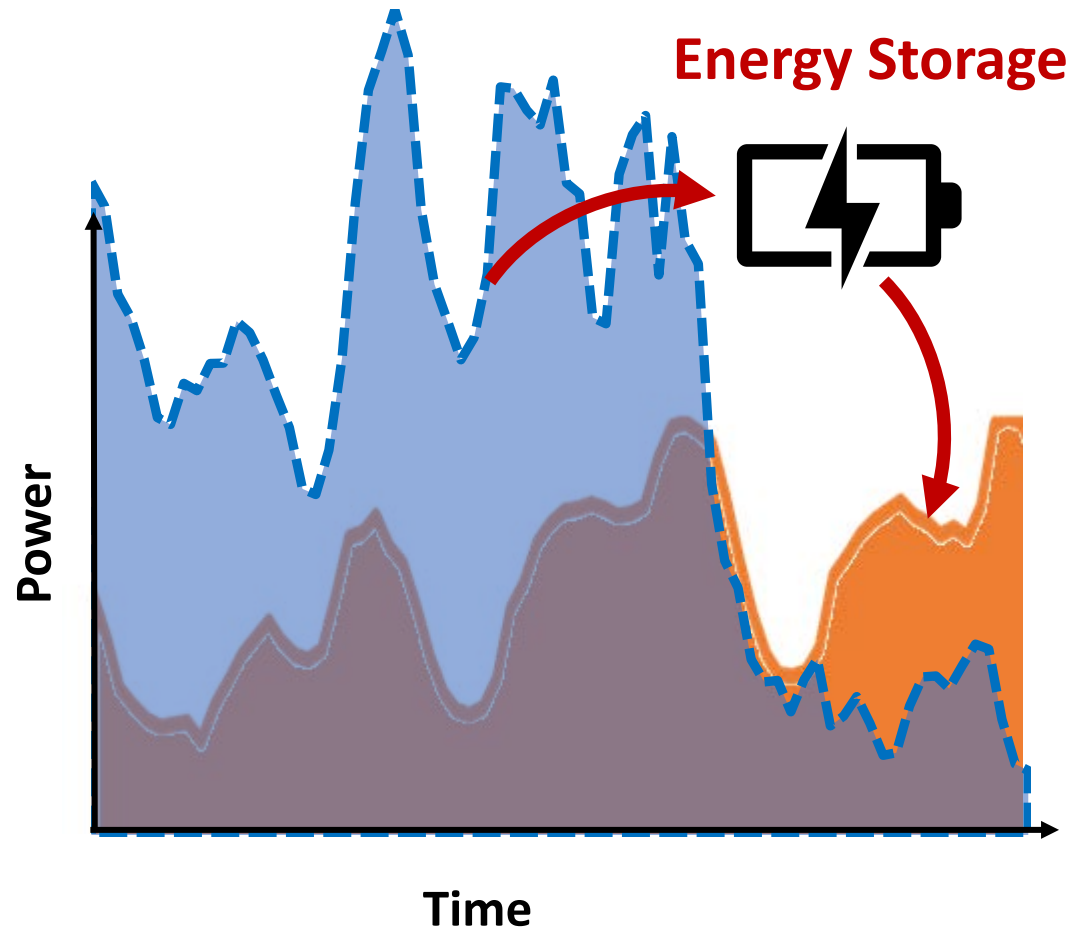
1. Curtailment: Discard any excess energy: do not turn on generators

OPTIONS TO BALANCE DEMAND AND AVAILABILITY



1. Curtailment: Discard any excess energy/ do not turn on generators
2. Demand response programs: time of use (TOU) pricing

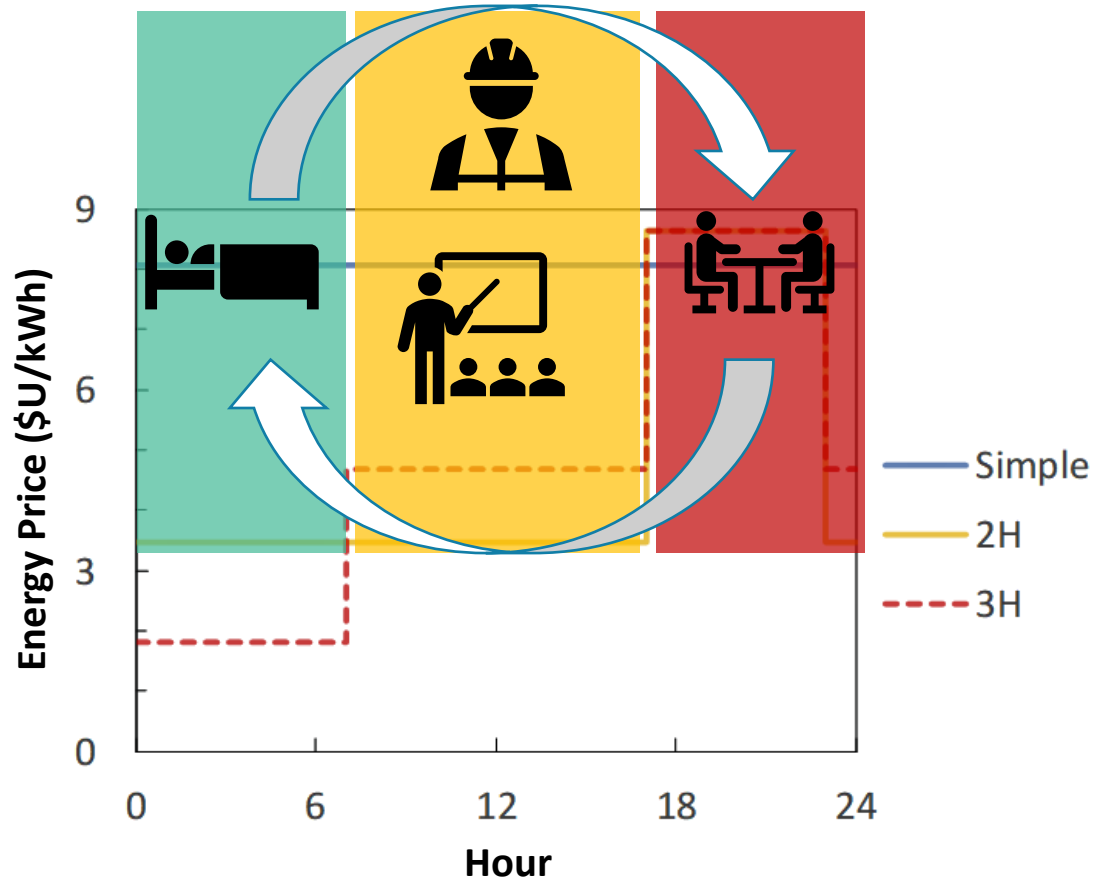
OPTIONS TO BALANCE DEMAND AND AVAILABILITY



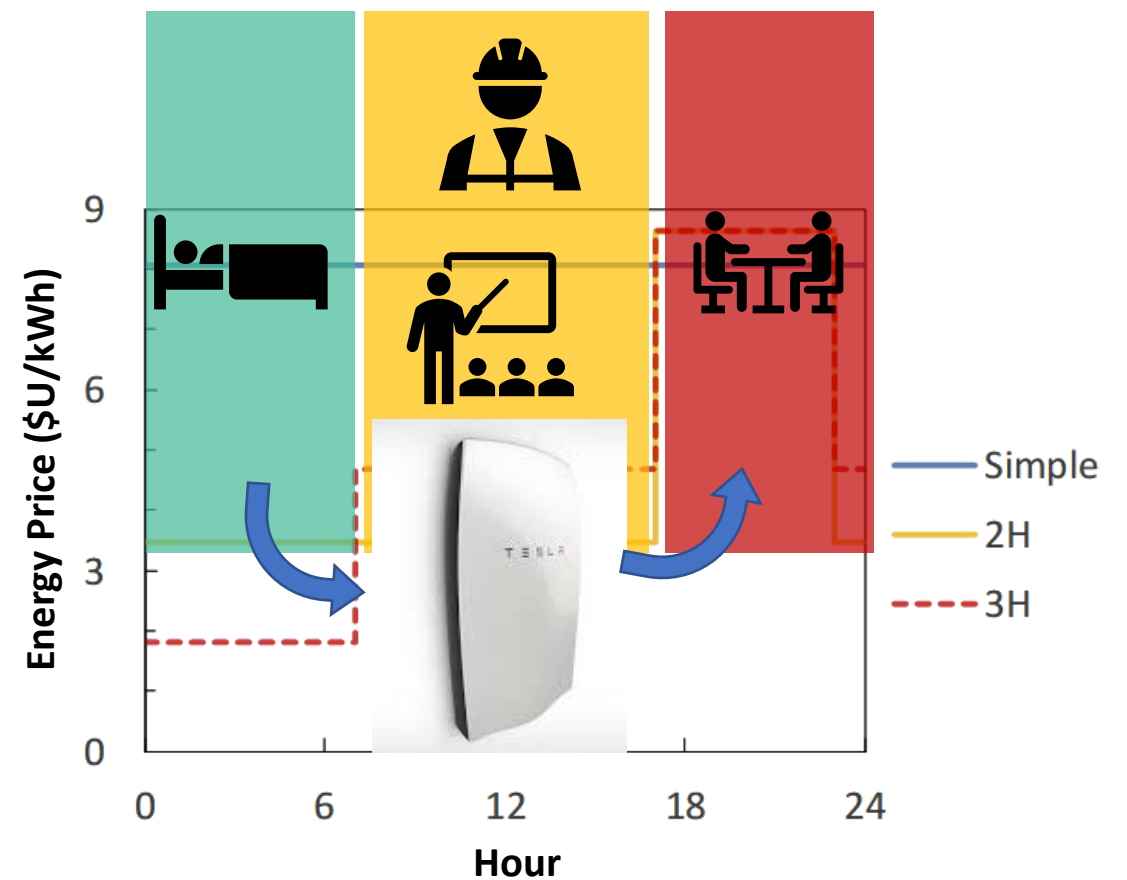
1. Curtailment: Discard any excess energy/ do not turn on generators
2. Demand response programs: time of use (TOU) pricing
3. Energy Storage: P2P, P2X industrial or consumer level

SMART TARIFFS?

- Demand response programs



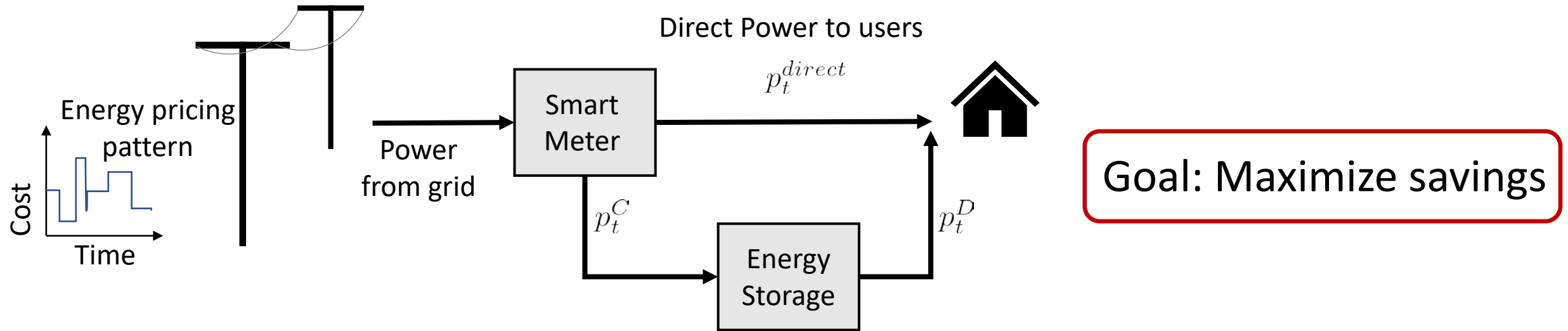
- Behind the meter storage



- Major habit changes

- Batteries degrade when used

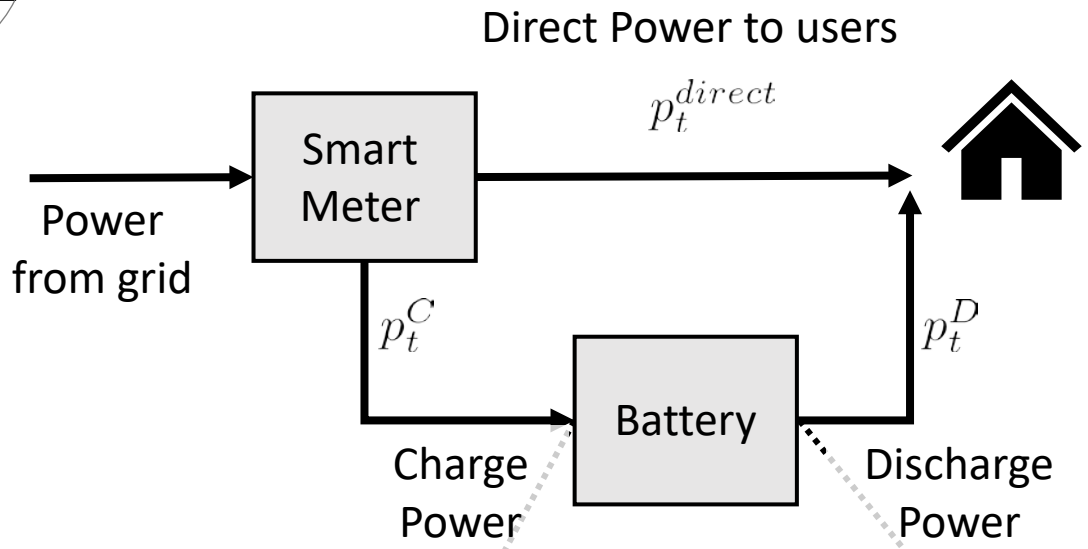
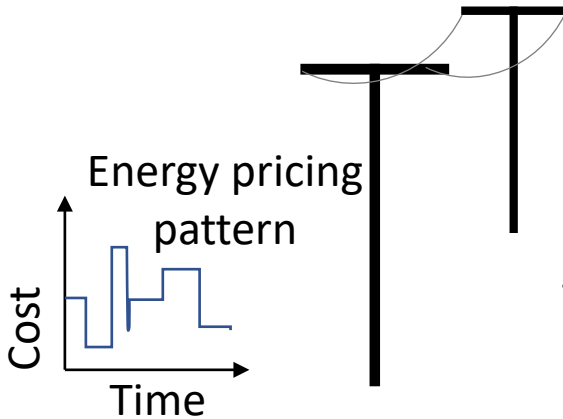
STATING THE PROBLEM



Goal: Maximize savings

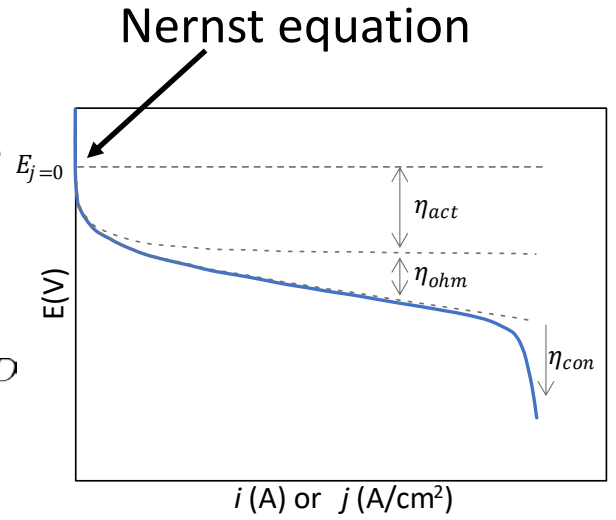
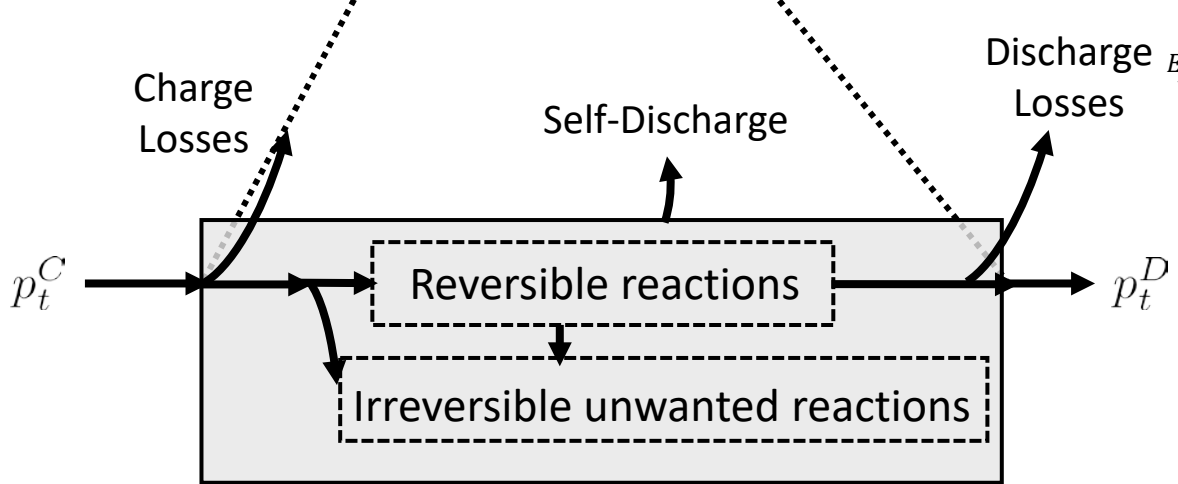
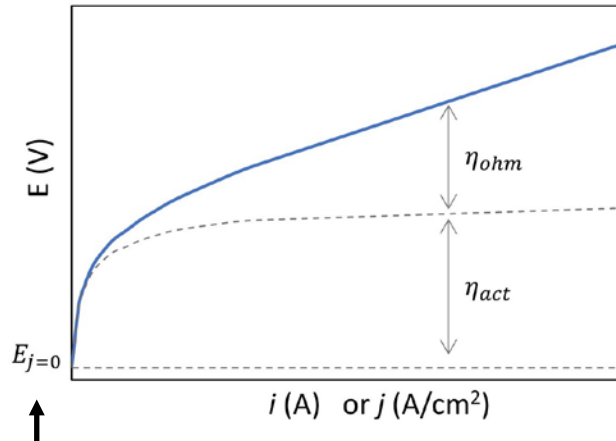
- Strategy: Time-shift power signal
 - Consume & charge at power p_t^C when energy cost ($\$_t$) is low
 - Discharge (& consume a rest if needed) at power p_t^D when $\$_t$ high

STATING THE PROBLEM



Charge/discharge patterns affect efficiency and life of the battery

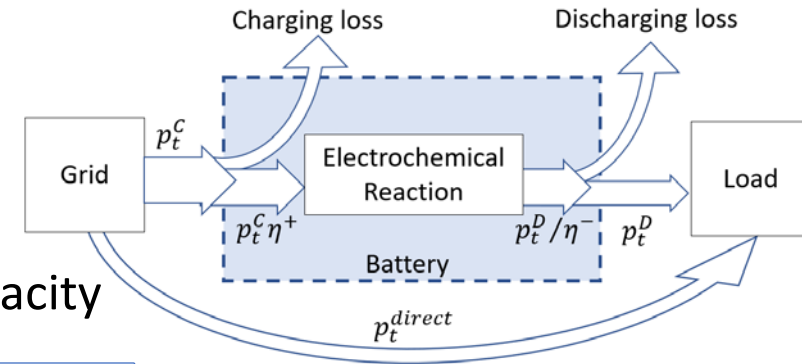
↑
ChemE phenomena



Nernst equation

FORMULATION OF THE OPTIMIZATION PROBLEM

- Objective function



In the electricity bill

Penalty for losing capacity

$$\text{Savings} = \sum_t (\$ p_t^D \Delta t - \$ p_t^C \Delta t)$$

Power not consumed from the grid when price is high

Power consumed from the grid when price is low

Fraction of capacity lost due to operation @ t
 Installed capacity (@ t=0)

“Discretization” of the price signal

Cost of the device

- p_t^D, p_t^C, x_t^{CL} Degrees of freedom

FORMULATION OF THE OPTIMIZATION PROBLEM

- Main constraints

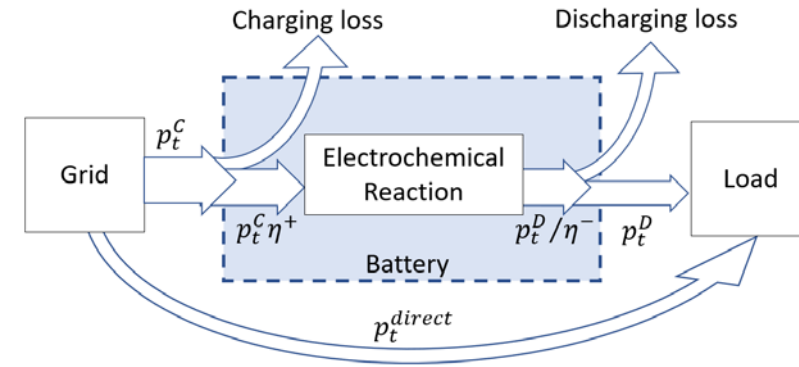
1. Energy balance $SoC_t = SoC_{t-1} + \Delta t p_t^C \eta^+ - \Delta t \frac{p_t^D}{\eta^-}$

2. Non-simultaneous charge/discharge $p_t^C p_t^D = 0$

3. Models for capacity loss

$$x_t^{CL} = \Delta t (\alpha_1 (c_{rate,t})^2 + \alpha_2 c_{rate,t})$$

Introduce non-linearity to the problem



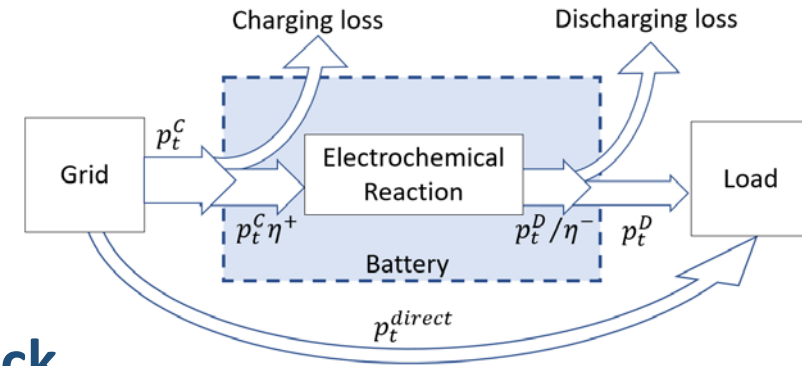
⇒ Limits solving the problem for short time spans

FORMULATION OF THE OPTIMIZATION PROBLEM

- Convex relaxation

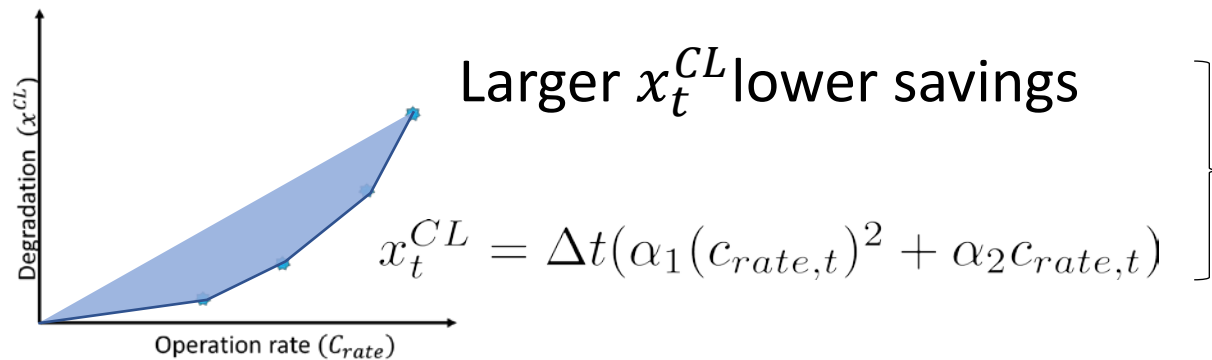
- Energy balance $SoC_t = SoC_{t-1} + \Delta t p_t^C \eta^+ - \Delta t \frac{p_t^D}{\eta^-}$

- ~~Non simultaneous charge/discharge $p_t^C p_t^D = 0$~~ **Drop & check**



“... simultaneous charge and discharge will not occur if marginal prices are positive”
 (Castillo & Gayme, IEEE Conference on Decision and Control, 2013)

- Models for capacity loss



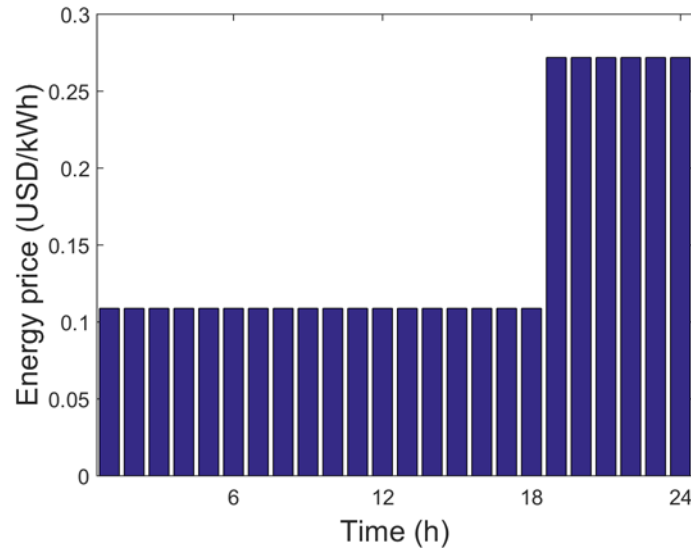
$$\Rightarrow x_t^{CL} \geq \Delta t (\alpha_1 (C_{rate,t})^2 + \alpha_2 C_{rate,t})$$

\Rightarrow Equivalent convex problem

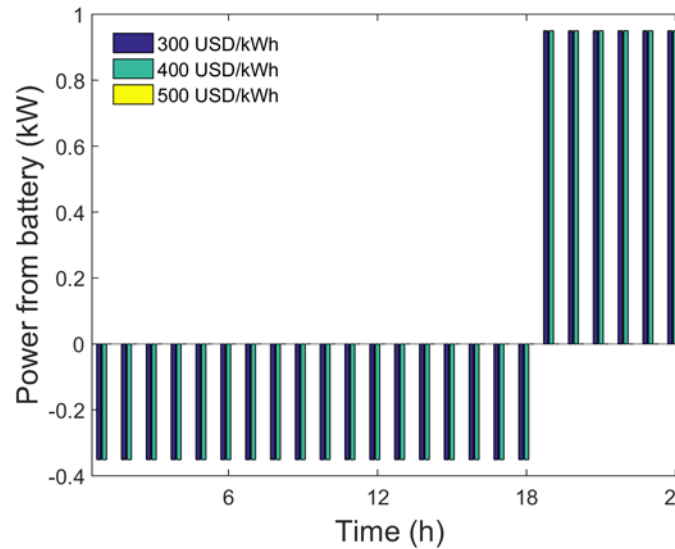
- ✓ global optimum
- ✓ Also strict \Rightarrow unique

CASE STUDY-SIMPLE SMART TARIFF (Corengia & Torres, *Processes*, 2018)

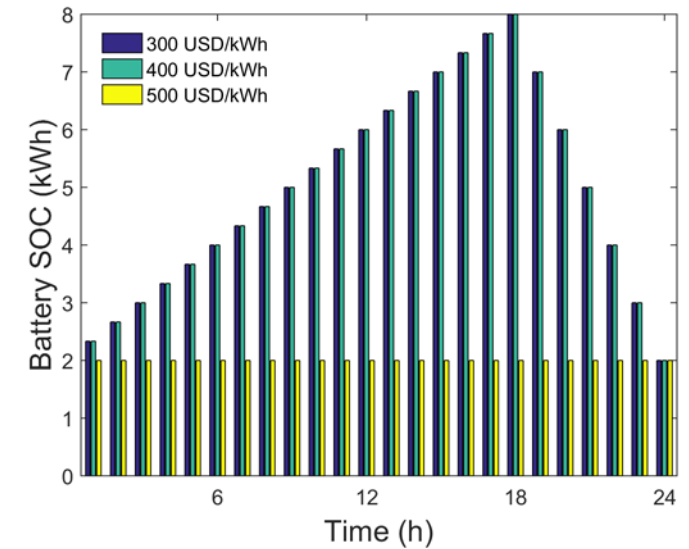
- Uruguay's 2H



- Charge/discharge schedule
(Li-ion battery, Sarker et al *Power Syst. Res.* 2017)



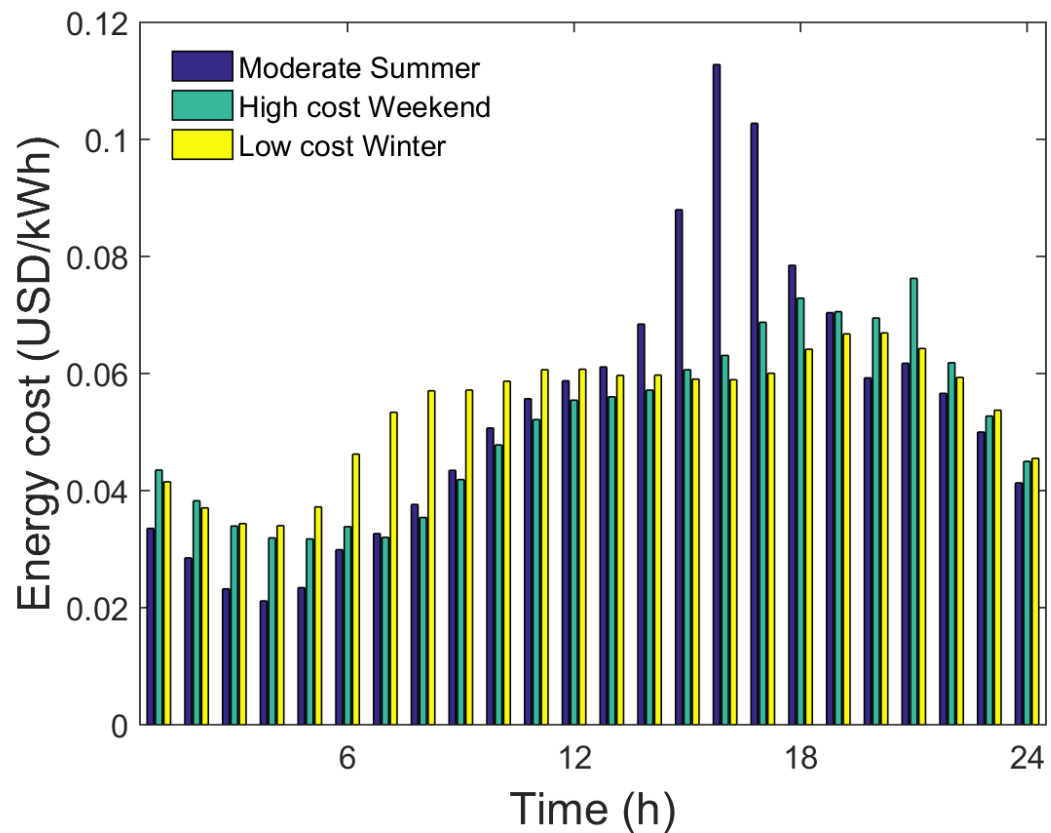
- Battery SoC



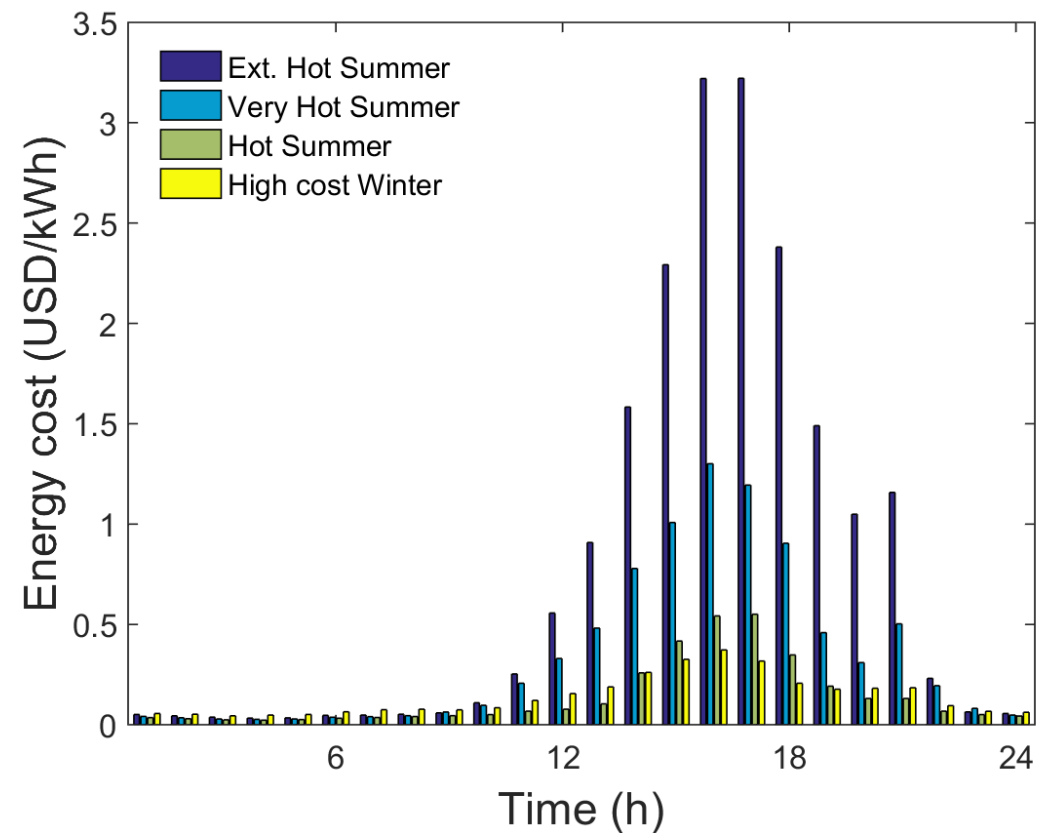
- Optimal solution: charge/discharge the battery as slowly as possible @ constant power
- If battery ≥ 500 USD/kWh \Rightarrow optimal solution never turn on the battery
- GAMS/IPOPT: 1 day analysis is very easy : 96 variables, 24 eq. const., 24 ineq. const.; solved PC i7 in sec

CASE STUDY-COMPLEX SMART TARIFF (Corengia & Torres, *Processes*, 2018)

- Southern California Edison (2018 TOU-GS-2-RTP).



- Days with moderate variation in prices

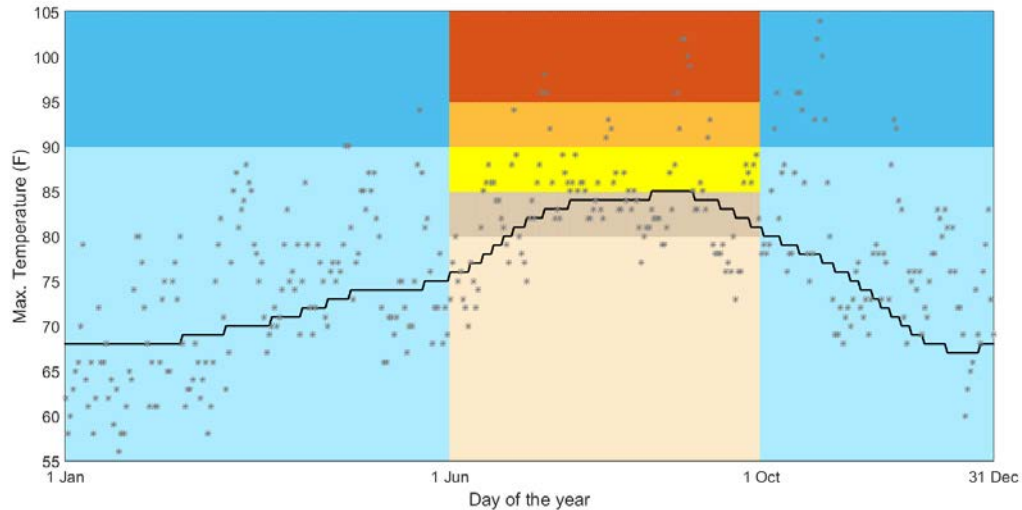


- Days with large variation in prices

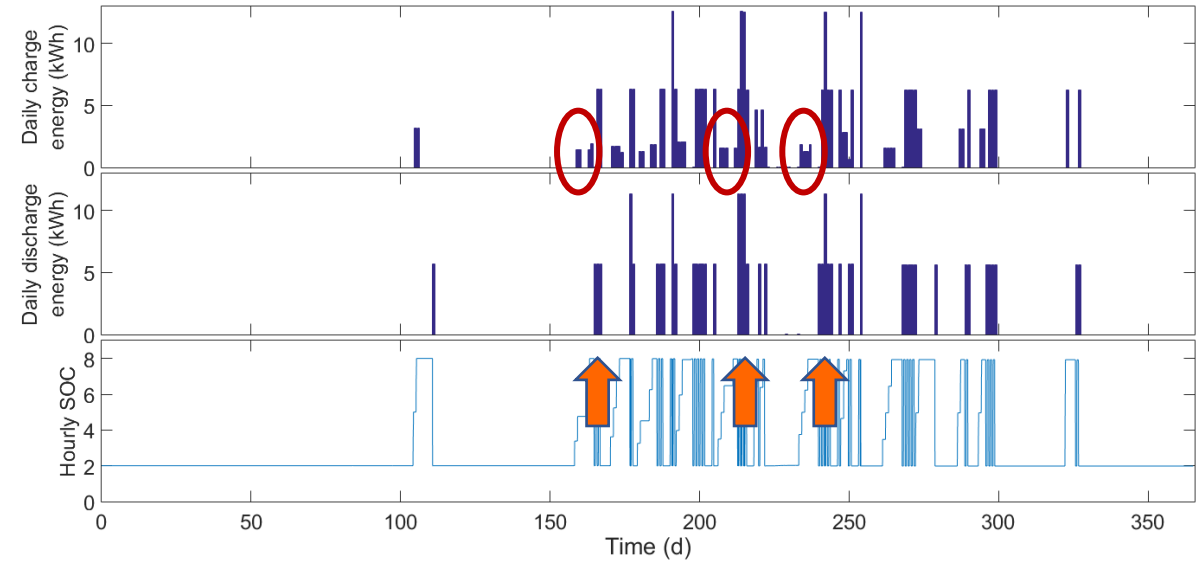
CASE STUDY-COMPLEX SMART TARIFF (Corengia & Torres, *Processes*, 2018)

- Long term behaviour

LA- Maximum temperatures 2017



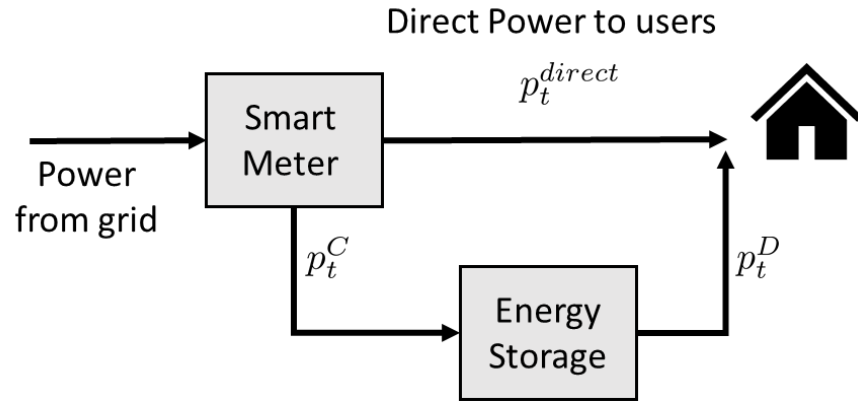
Background colors => limits for tariffs



- Strategy: use the battery in days with large differences between peak/ off-peak prices
- Start charging slowly the battery even days before to preserve battery => add constraint to limit this behavior
- 1 yr analysis 35405 variables, 9125 eq. const., 8760 ineq. constr., 26280 DOF; solved PC i7 in ~1h
- 5 yr analysis 177k variables, 45k eq. const., 219k ineq. constr., 131k DOF; solved PC i7 in hours , not solved before

CASE STUDY-MATCH CONSUMPTION PROFILES

(Corengia & Torres, *ENERLAC*, 2020)



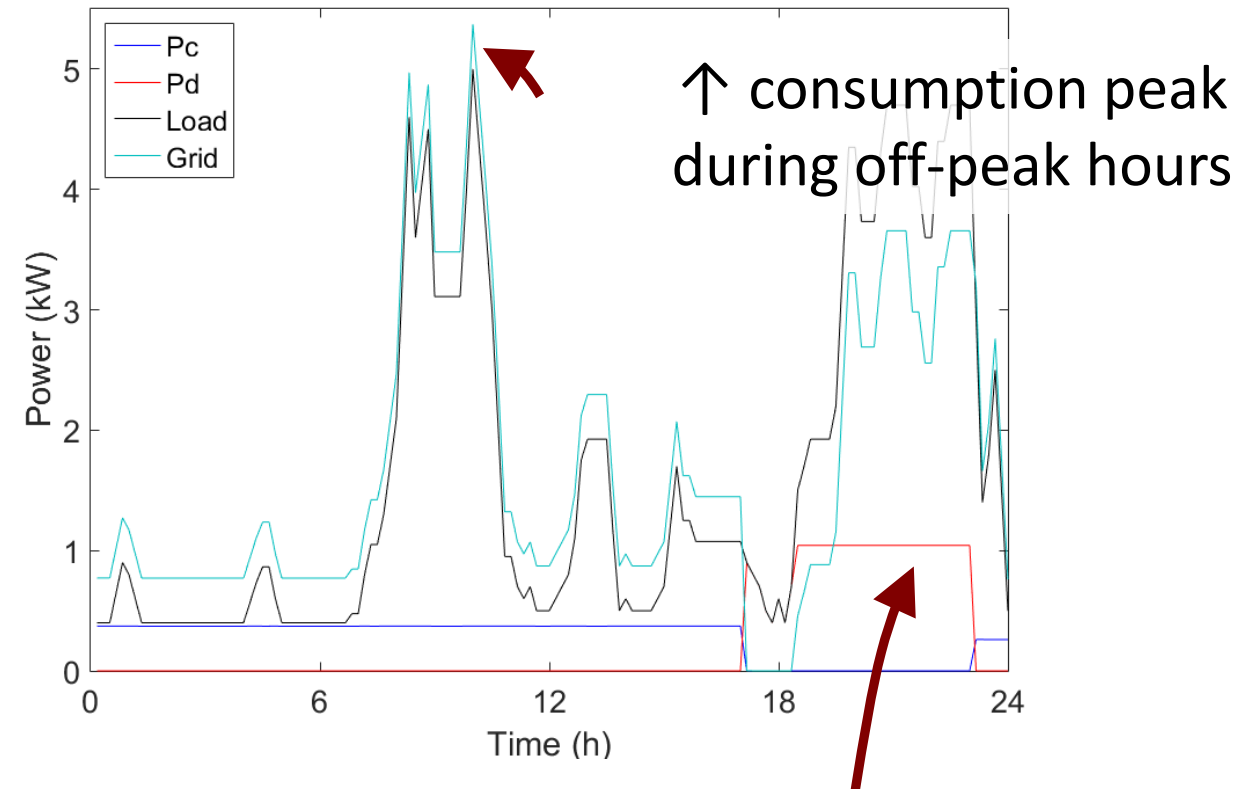
- Add constraint: always satisfy demand

$$p_t^{load} = p_t^{direct} + p_t^D$$

- Cap maximum power from the grid

$$p_t^{direct} \leq p^{contract}$$

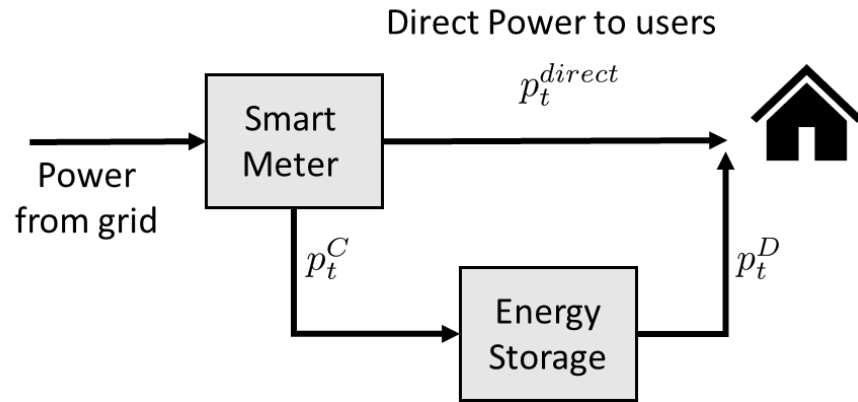
Student residency- TOU Uruguay 2H



- Discharge concentrated in part of the high price region

CASE STUDY-MATCH CONSUMPTION PROFILES

(Corengia & Torres, *ENERLAC*, 2020)

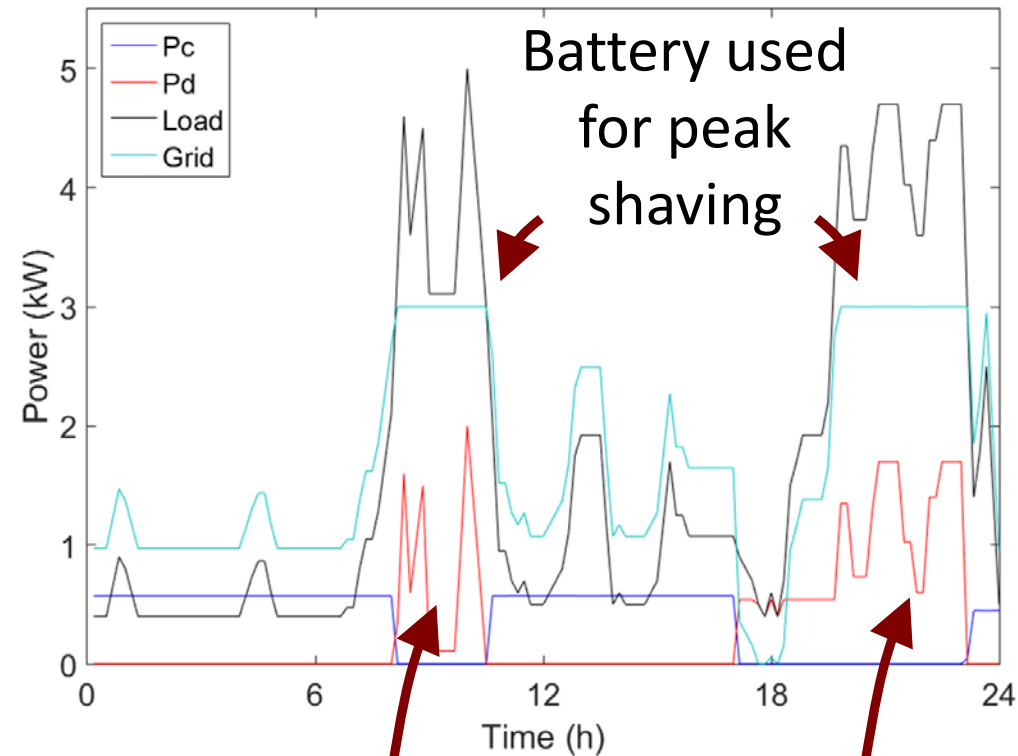


- Add constraint: always satisfy demand

$$p_t^{load} = p_t^{direct} + p_t^D$$

- Cap maximum power from the grid
 - $p_t^{direct} + p_t^C \leq p^{contract}$
 - Include penalty for consuming over contract

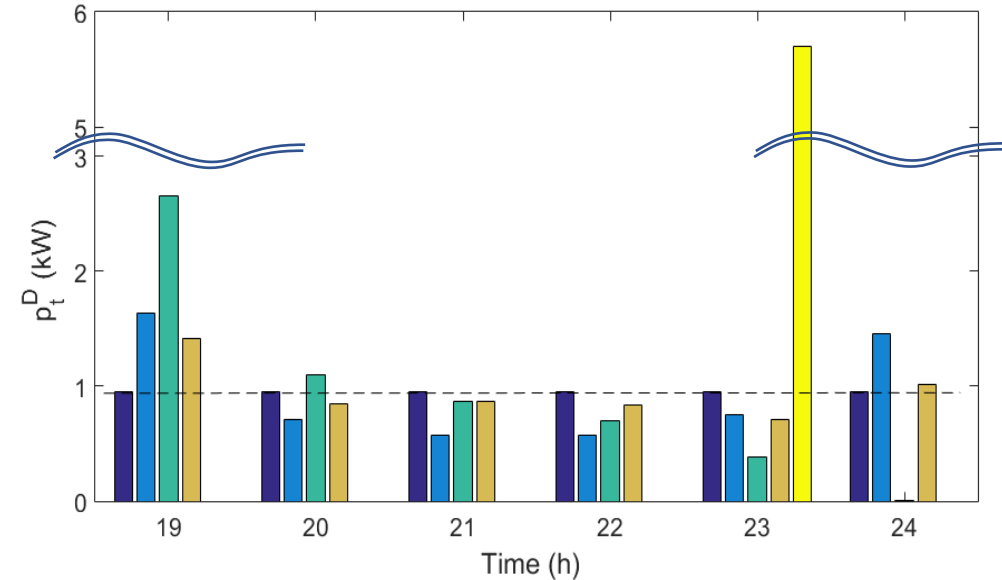
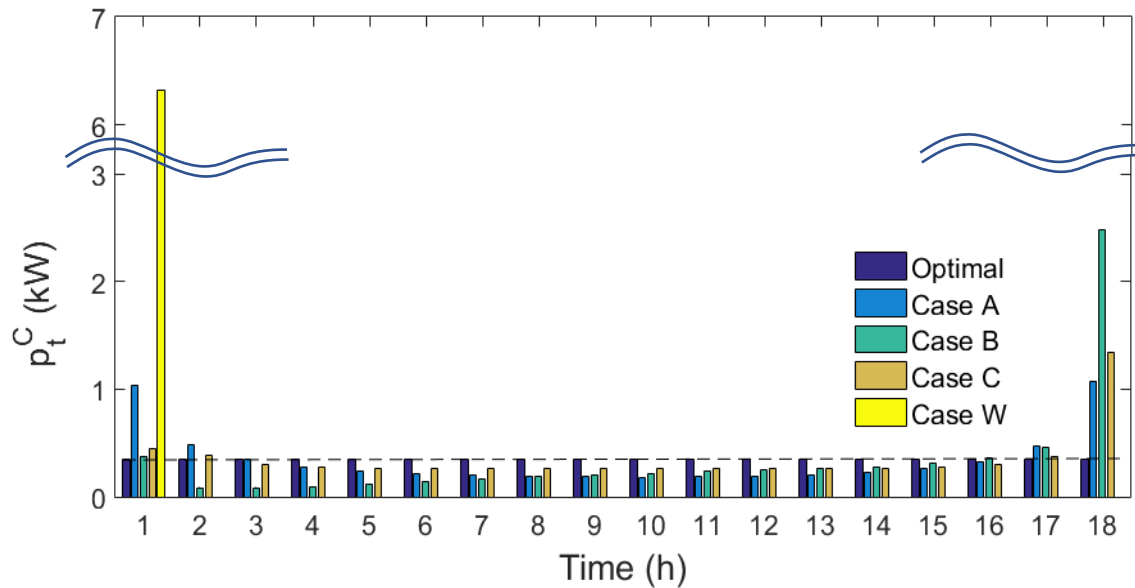
Student residency- TOU Uruguay 2H- cap peak



- Two charge/ discharge cycles- nonuniform discharge
- Use ES to contract less power

IS IT WORTH COMPLICATING OURSELVES WITH DEGRADATION TERMS? (Corengia & Torres, FOAPD, 2019)

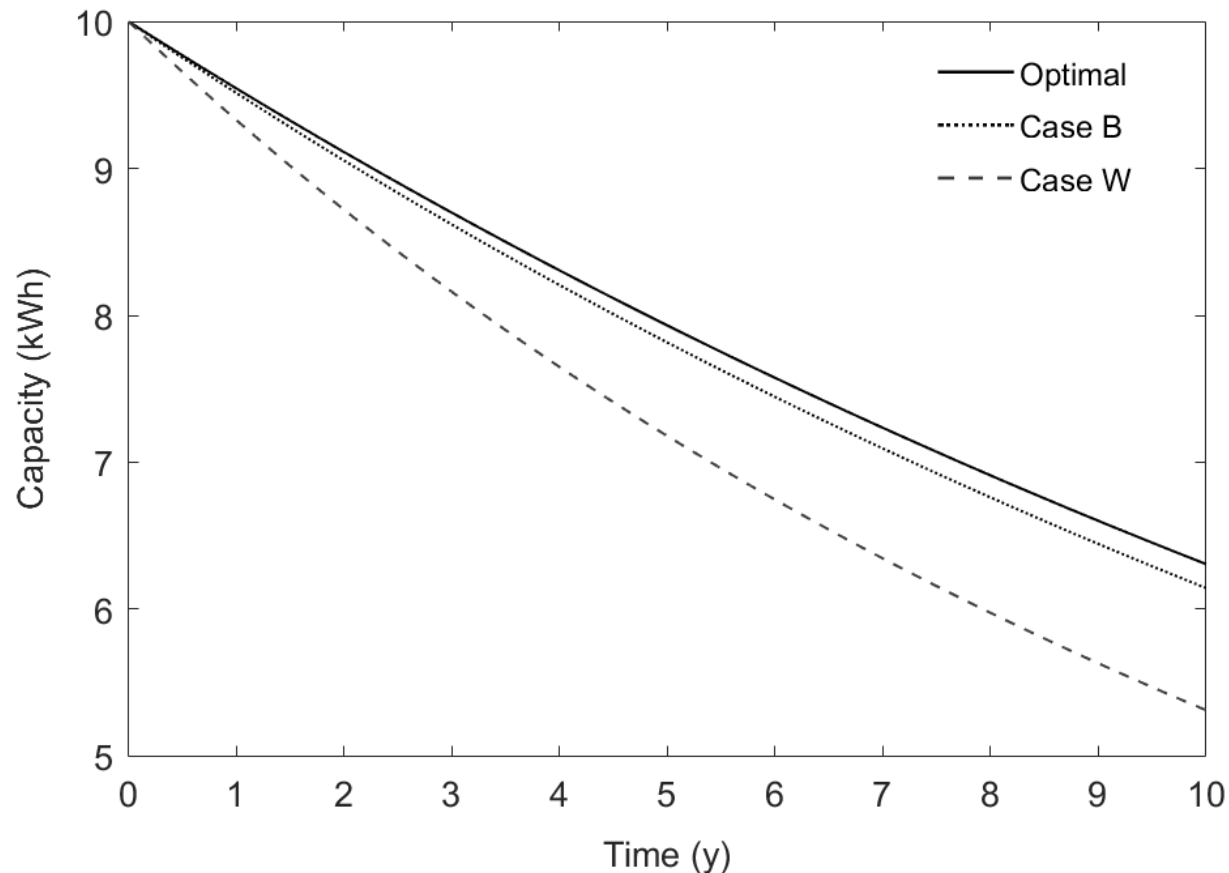
- Compare solutions to penalized and non-penalized problems



- Non-penalized problem not strictly convex \Rightarrow global optimum not unique
- Cases A, B, C, W several possible schedules, W =worst (single charge/discharge)

IS IT WORTH COMPLICATING OURSELVES WITH DEGRADATION TERMS? (Corengia & Torres, *FOCAPD*, 2019)

- Consequences of sub-optimal operation (for Li-ion battery, Sarker et al *Power Syst. Res.* 2017)



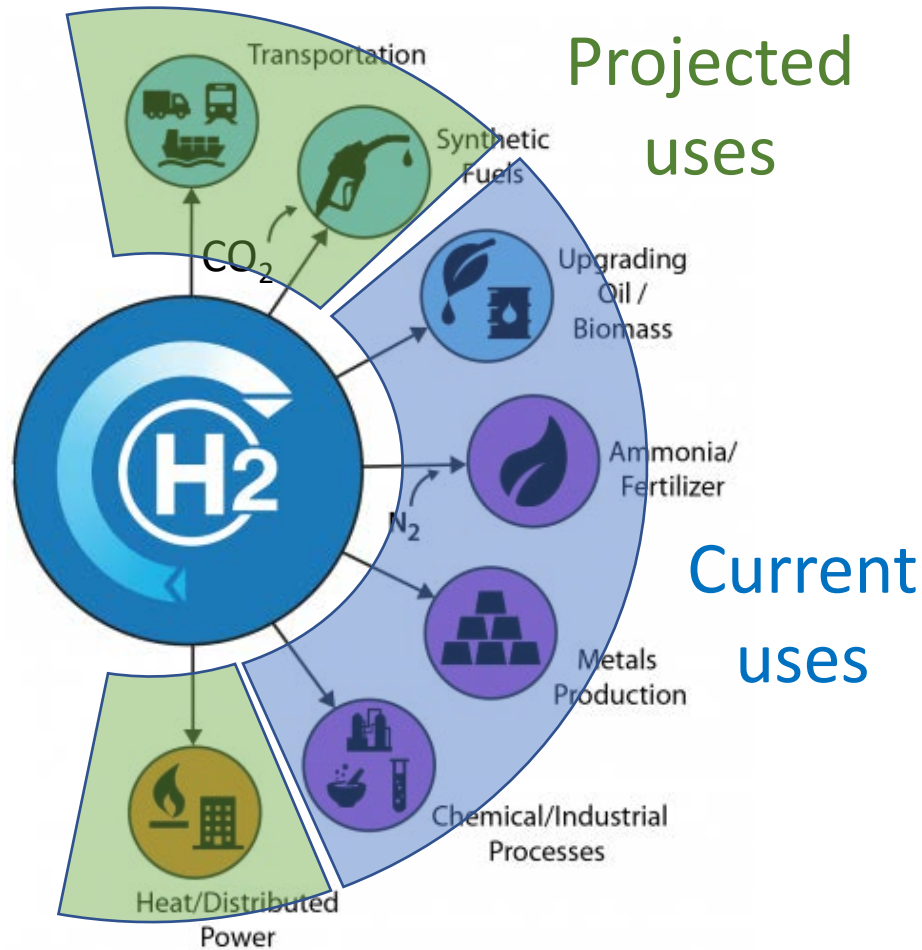
- What if degradation occurs but was not considered in optimization problem?
 - Algorithm stops at case B: not that different \Rightarrow Lucky case
 - Algorithm stops at case W \Rightarrow increased capacity loss

SUMMARY: BEHIND THE METER STORAGE IN BATTERIES

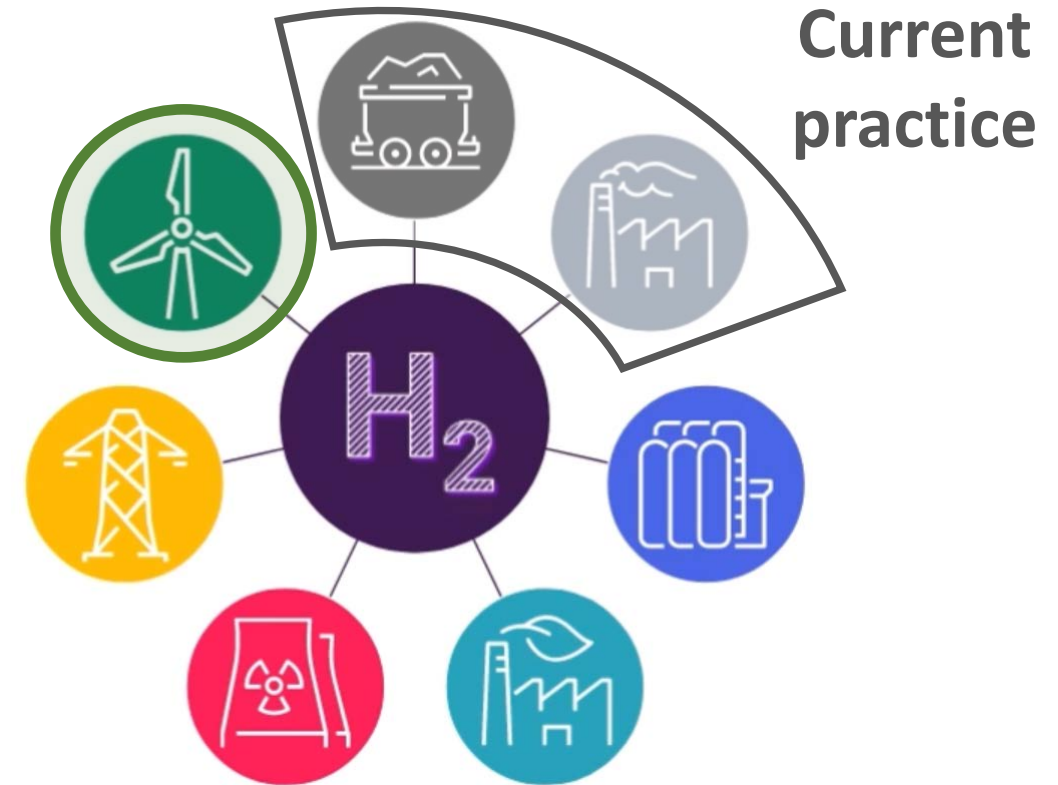
- Take advantage of TOU strategies w/o disruptive changes in habits
- Mostly studied outside ChemE
 - ⇒ include degradation effects in formulation of optimization problems
 - ⇒ convex formulations allows for solving for years vs day
- Case study new Li-ion batteries:
 - Only worth if large price differences in smart tariff ⇒ second life batteries?
 - Not considering degradation may lead to significant premature loss of capacity

PRODUCTION OF GREEN-HYDROGEN

- The hydrogen economy



- The colors of Hydrogen

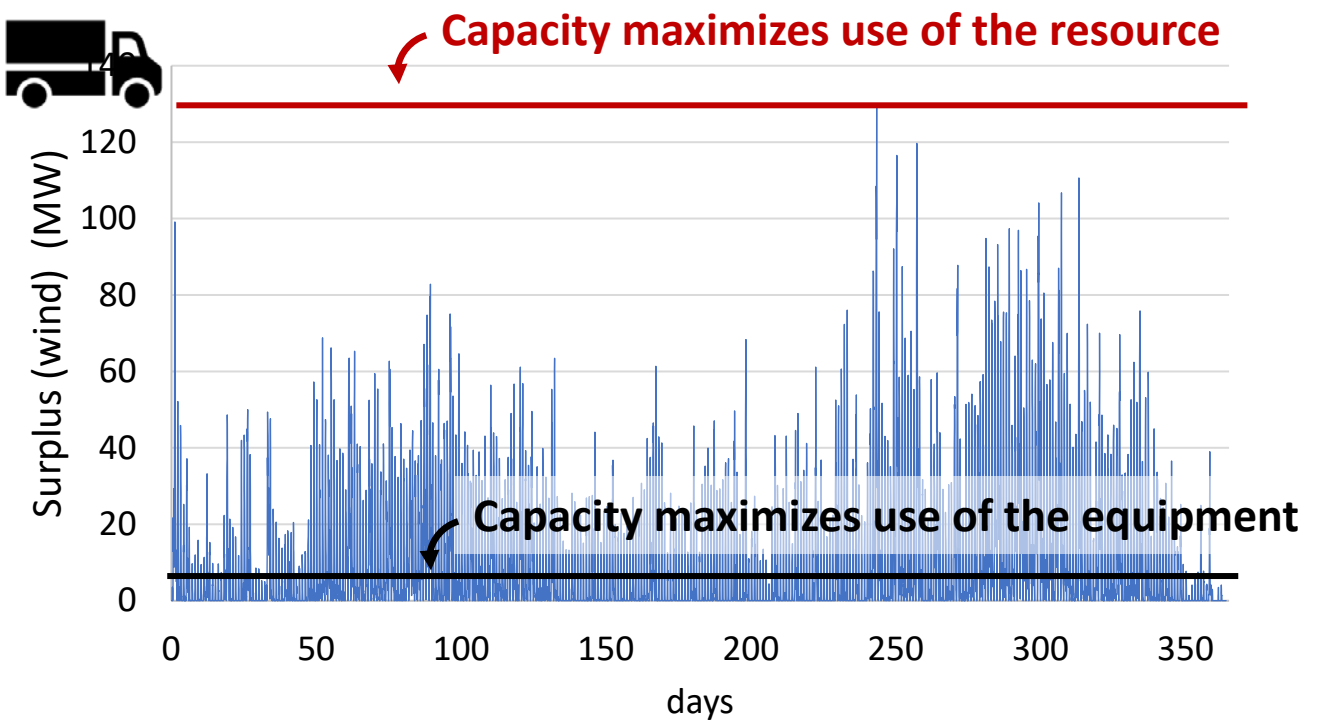
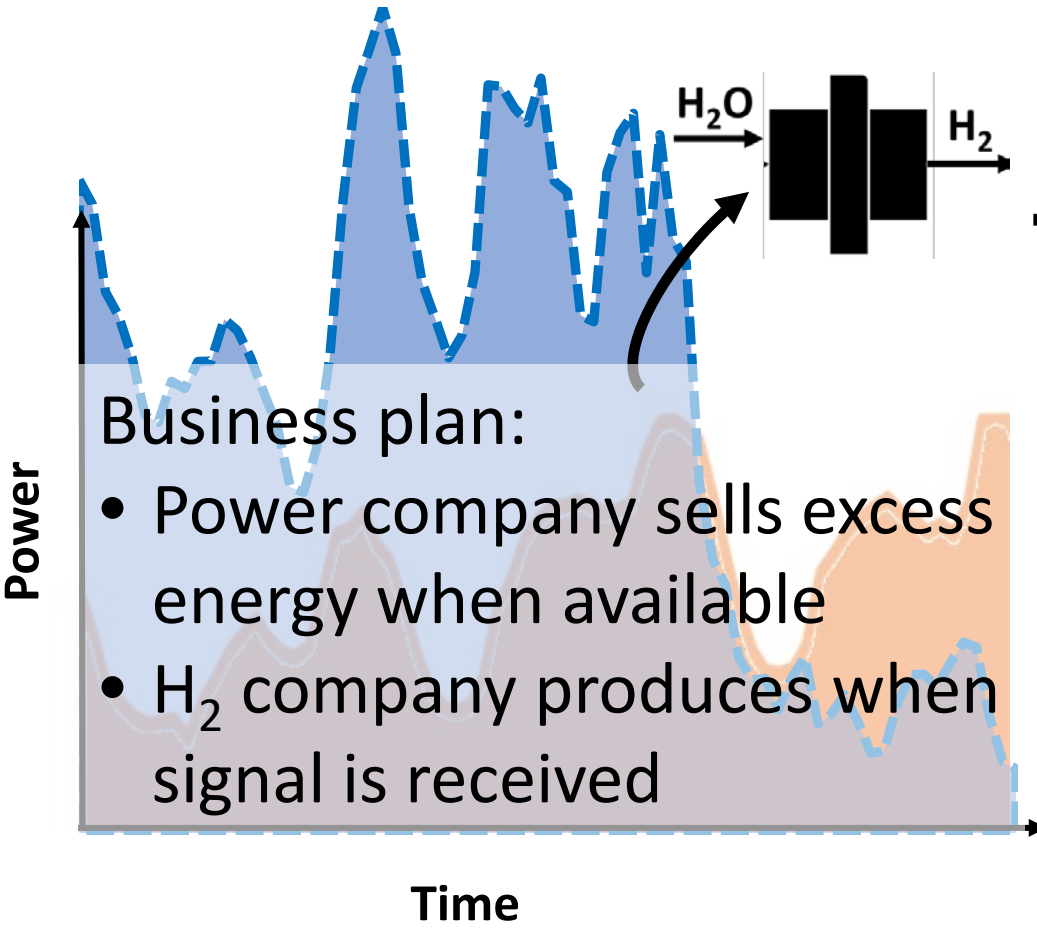


- Green H_2 : Water electrolysis powered by renewable sources

Figure made on the basis of <https://www.energy.gov/eere/fuelcells/h2scale>

THE VERNE PROJECT URUGUAY-PILOT FUEL STATION

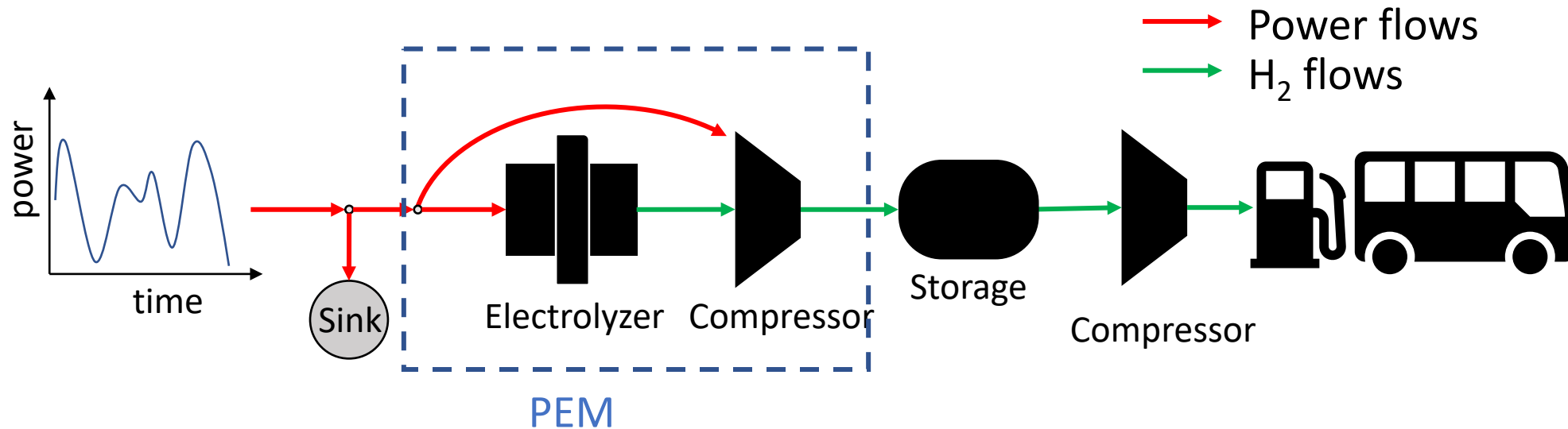
- H₂ production capacity?



- Surpluses → fuel H₂

- Trade-off => optimization

GREEN-H₂ CASE STUDY 1: SURPLUSES → PEM → Fuel H₂ ⁽¹⁾



- PEME:

- low temperature (80-100°C)
- fast on-off dynamics (startups ~2-3 min ⁽²⁾)
- work at any partial load

- Compression system:

- designed and costed offline (Aspen Plus/APEA)

(1) Corengia & Torres, *ESCAPE 30*, 2020 (2) Corengia & Torres, *PSE*, 2018

GREEN-H₂ CASE STUDY 1: SURPLUSES → PEM → Fuel H₂ ⁽¹⁾

Optimization Problems:

- **Objective functions**

1. max NPV for target $\$H_2$
2. max surplus usage for target $\$H_2$ (NPV \geq 0)
3. min $\$H_2$ for target H₂ production

- **Constraints:**

- $\dot{m}_{H_2,t} \leq IC_{H_2}$
- $\dot{p}_{H_2,t} + \dot{p}_{comp,t} \leq \dot{p}_{surplus,t}$
- $CAPEX(IC_{H_2})$ & $OPEX(IC_{H_2})$ ⁽¹⁾

- **DV:** IC_{H_2} , operation mode

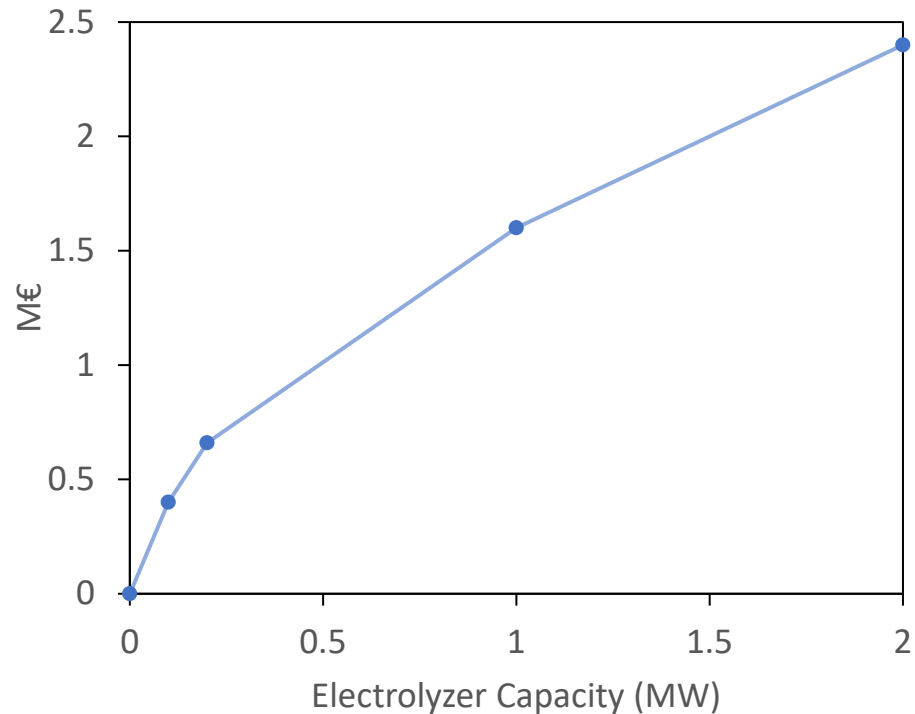
- LP problems, GAMS-CPLEX

- (MILP $IC_{H_2} < 2\text{MW}$)

(1) Electrolyzer costs J. Proost, 2019. *International Journal of Hydrogen Energy* 44 (9), 4406–4413

PEM ELECTROLYZER COSTS

- J. Proost, *International Journal of Hydrogen Energy* 44 (9), 4406–4413, 2019



- Equipments: stacks of cells up to 2 MW
- Beyond 2 MW: multiple stacks

=> Composite curve approximated by linear fitting: 1257 euros/kw

(costs include demineralizer, gas separators, vessels, purifying system, peripherals)

GREEN-H₂ CASE STUDY 1: SURPLUSES → PEM → Fuel H₂ ⁽¹⁾

Optimization Problems:

- **Objective functions**

1. max NPV for target \$H₂
2. max surplus usage for target \$H₂ (NPV ≥ 0)
3. min \$H₂ for target H₂ production

- **Constraints:**

- $\dot{m}_{H_2,t} \leq IC_{H_2}$
- $\dot{p}_{H_2,t} + \dot{p}_{comp,t} \leq \dot{p}_{surplus,t}$
- $CAPEX(IC_{H_2}) \ \& \ OPEX(IC_{H_2})$ ⁽¹⁾

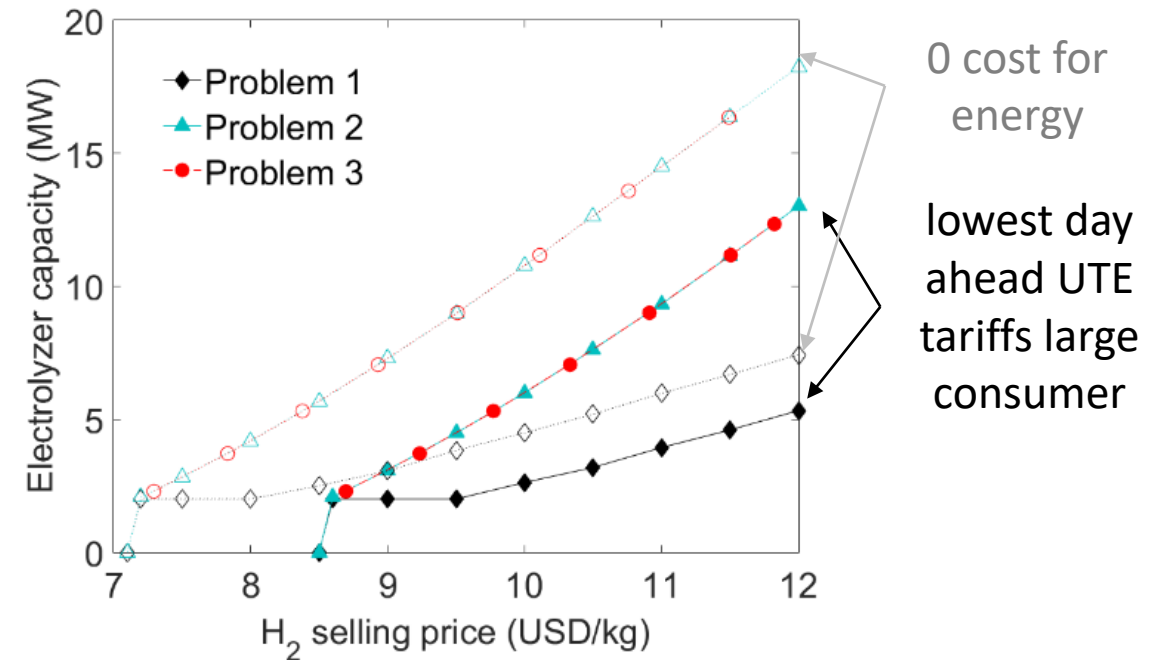
- **DV:** IC_{H_2} , operation mode

- LP problems, GAMS-CPLEX

- (MILP $IC_{H_2} < 2\text{MW}$)

(1) Electrolyzer costs J. Proost, 2019. *International Journal of Hydrogen Energy* 44 (9), 4406–4413

- **Results**



- Install only if \$H₂ > 7 USD/kg
- Threshold capacity 2 MW: largest single electrolyzer cost in Ref. (1)

GREEN-H₂ CASE STUDY 1: SURPLUSES → PEM → Fuel H₂ ⁽¹⁾

Optimization Problems:

- **Objective functions**

1. max NPV for target \$H₂
2. max surplus usage for target \$H₂ (NPV≥0)
3. min \$H₂ for target H₂ production

- **Constraints:**

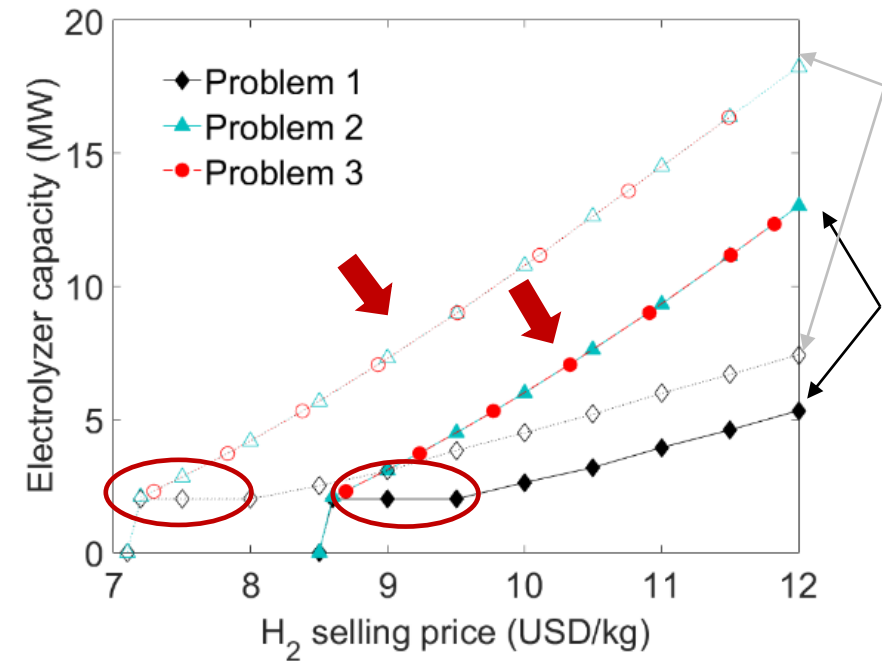
- $\dot{m}_{H_2,t} \leq IC_{H_2}$
- $\dot{p}_{H_2,t} + \dot{p}_{comp,t} \leq \dot{p}_{surplus,t}$
- $CAPEX(IC_{H_2}) \ \& \ OPEX(IC_{H_2})$ ⁽¹⁾

- **DV:** IC_{H_2} , operation

- LP problems, GAMS-CPLEX

(1) Electrolyzer costs J. Proost, 2019. *International Journal of Hydrogen Energy* 44 (9), 4406–4413

- **Results**



0 cost for energy

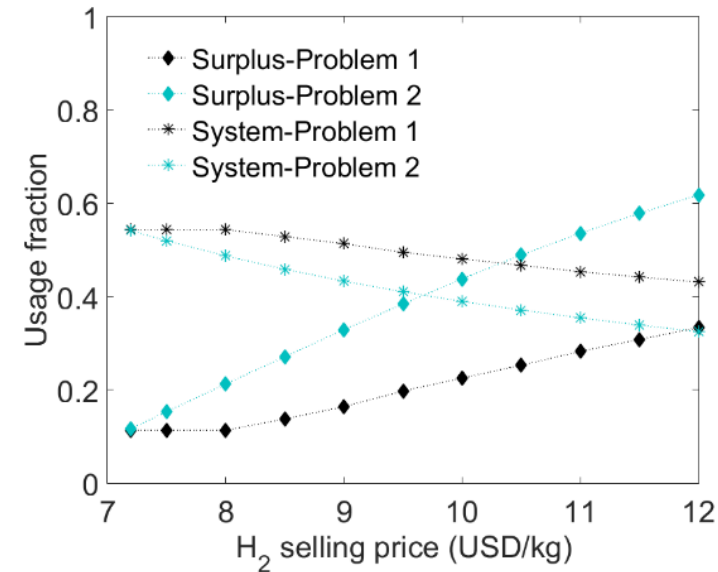
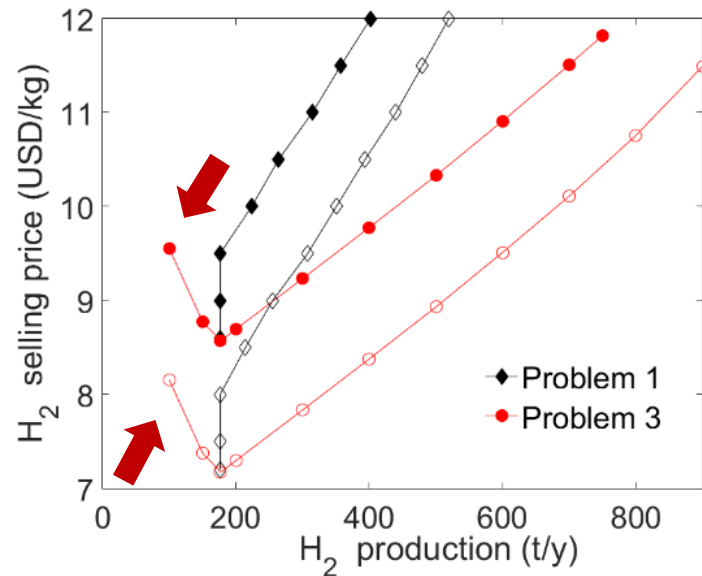
lowest day ahead UTE tariffs large consumer

- NPV ↑ wo ↑ IC
- Both optimize @ NPV= 0

GREEN-H₂ CASE STUDY 1: SURPLUSES → PEM → Fuel H₂ ⁽¹⁾

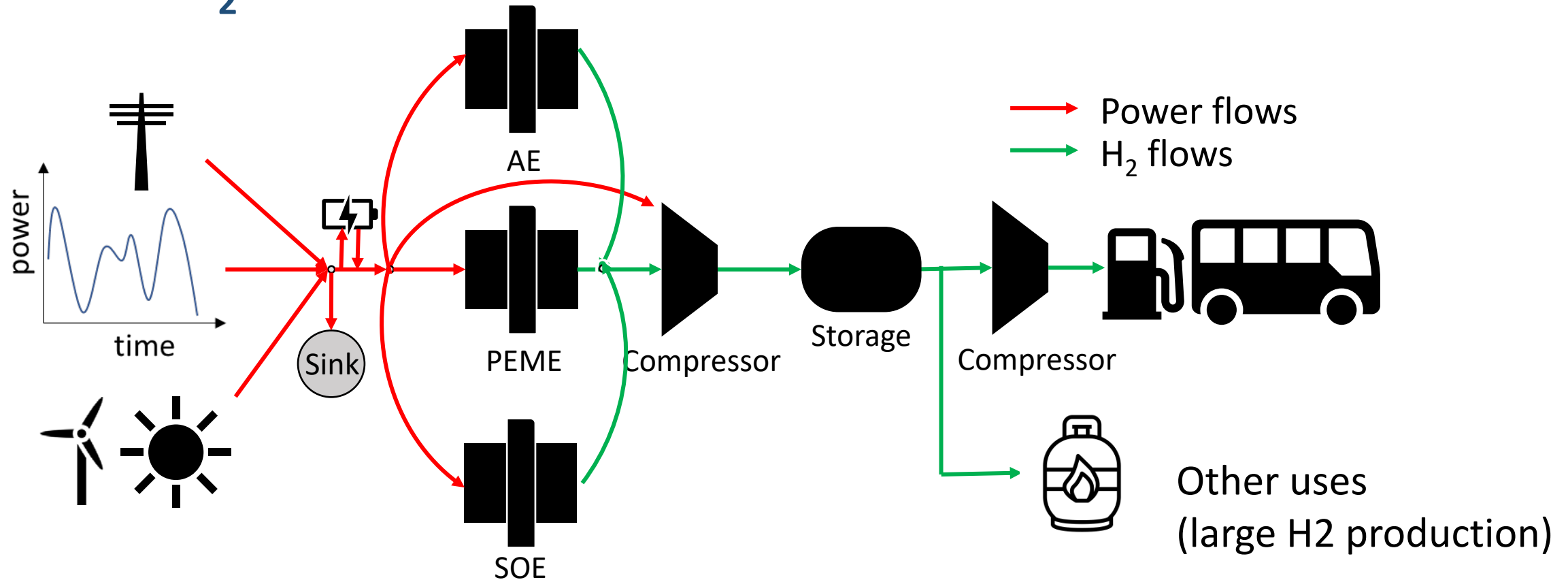
- **Results**

(P1) max NPV for target \$H₂ (P2) max surplus usage for target \$H₂ (NPV≥0) (P3) min \$H₂ for target H₂ production



- Forced IC < 2MW => small and costly equipments => ↑ H₂ prices
- ↑ H₂ prices favors ↑ IC to capture resource at the expense of not fully using IC

GREEN-H₂: ADD FLEXIBILITY



- PEME flexible but too expensive => combine (cheaper) AE for base operation + PEME peaks
- AE not at partial load => grid (not only surpluses) or install generator
- Also considered SOE: newer (not in the market) technology

Corengia & Torres, In preparation 2022

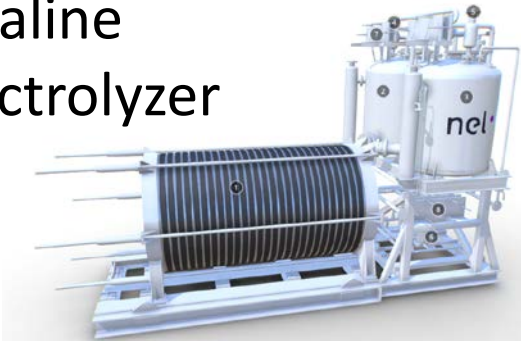
GREEN-H₂: TECHNOLOGY COMPARISON (1)

- PEME



- Low temperature (80-100 °C)
- Work at partial load
- In the market (NEL, Siemens)

- Alkaline Electrolyzer



- Low temperature, but lower current densities
- Efficiency ~PEME but low flexibility: minimum partial load for each stack 15-40% (safety)
- Old mature technology

- Solid Oxide Electrolyzer

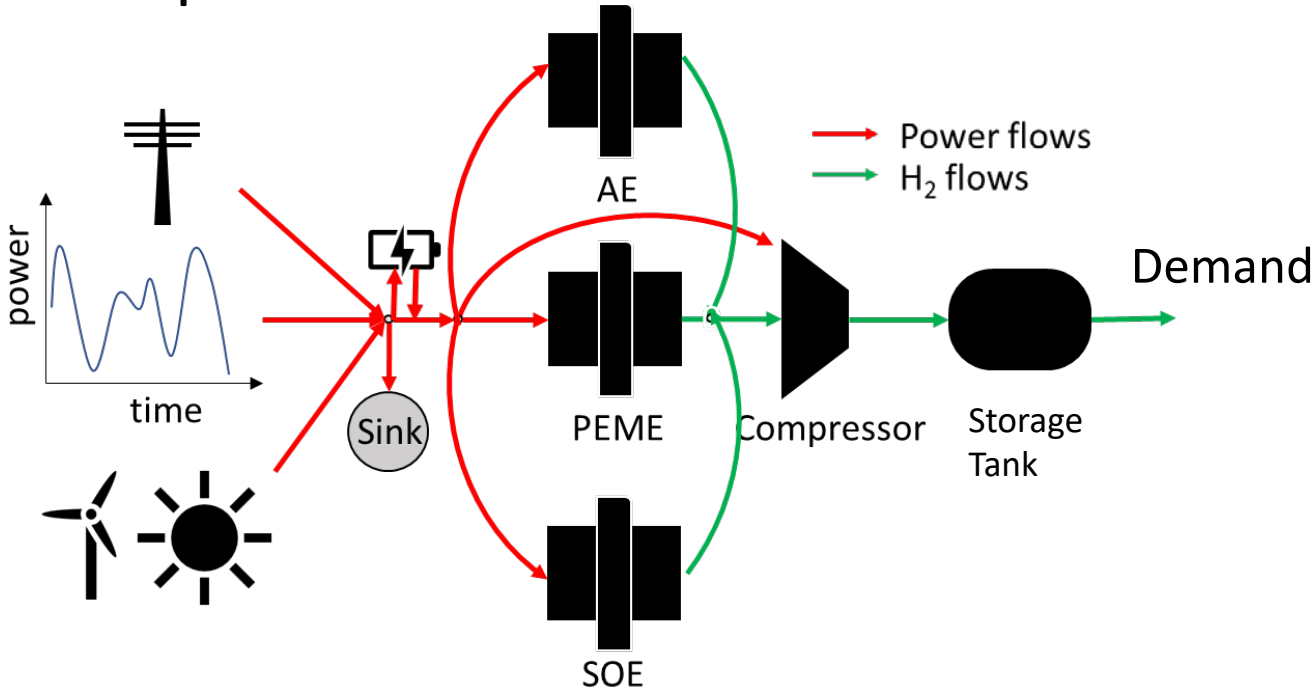


- High temperature (500-850 °C) => on-off not easy
- More efficient than AE and PEME, partial load > 60% does not require external heat
- Current densities comparable to PEME
- Market: lab scale

Figures: Siemens, NEL Technology, Oxoenergy
(1) Schmidt, *Int. J. Hyd. En*, 42, 2017

GREEN-H₂: OPTIMIZATION PROBLEM⁽¹⁾

- Superstructure



- Family of problems
- MILP (AE), Some LP
- All GAMS/CPLEX with SolnPool

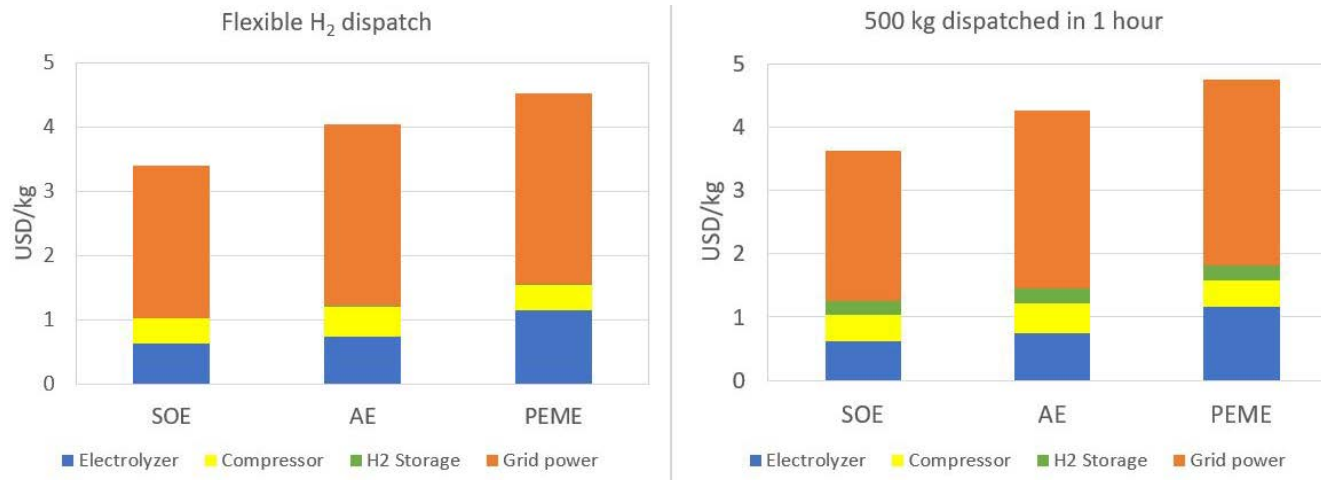
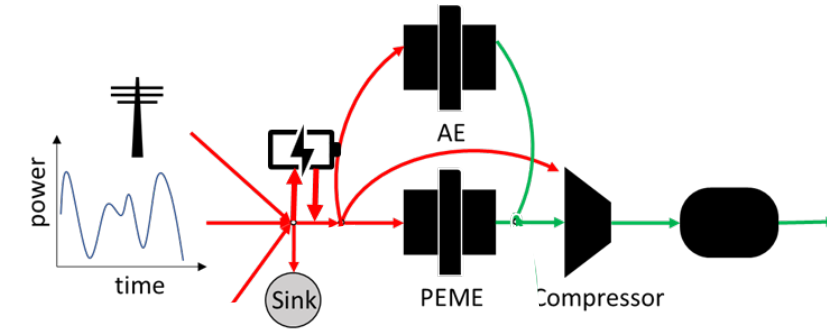
- Allow all technologies and power combinations
- Objective function: Annualized cost
 - CAPEX: Wind, Solar generators, AE, PEME, SOE, Compressor, Tank, Battery
 - OPEX: Electrolyzers, Compressor, penalty for using the battery
- Restrictions for the equipment loads:
 - SOE if selected always on: min. load $\geq 60\%$
 - AE: may turn on/off; min load 40%
- Costs: AE, PEM literature; SOE estimates² => worst case SOE~AE, then sensitivity analysis
- Demand curve: substitution of NG imports
- Wind/Sun availability, energy prices: real curves Uruguay

(1) Corengia & Torres, In preparation 2022

(2) Anghilante et al, *International Journal of Hydrogen Energy*, 43, 2018

GREEN-H₂: RESULTS LOW H₂ PRODUCTION (JUST GRID)

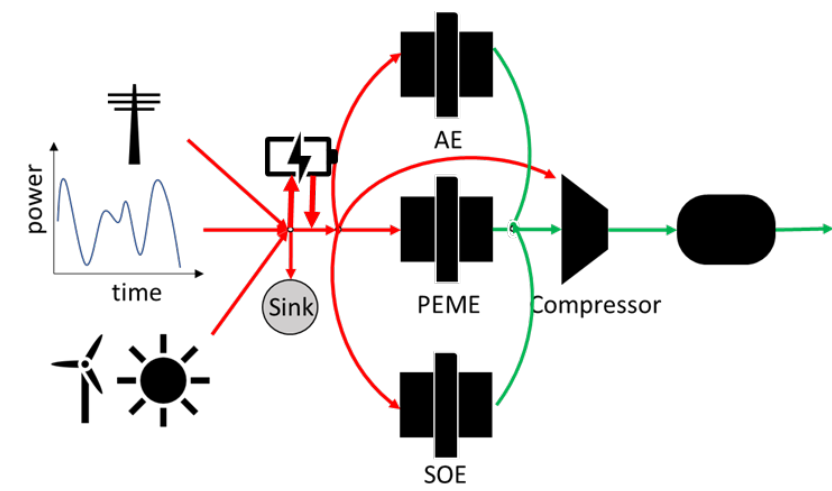
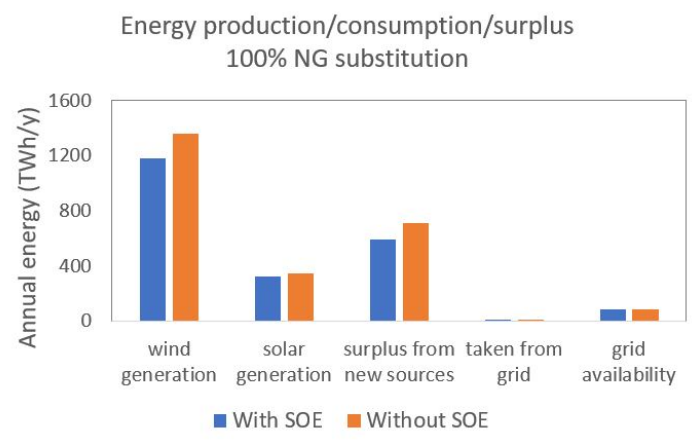
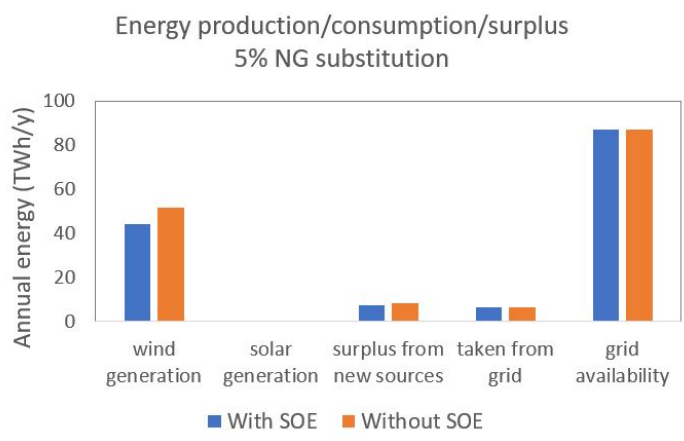
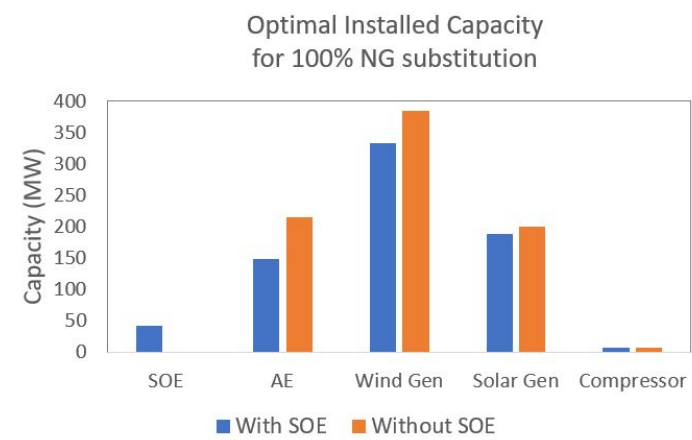
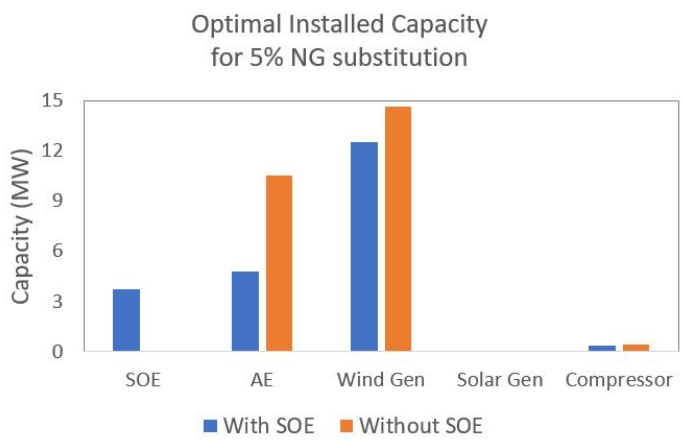
- SOE are preferred over AE, PEME
- Optimal solutions do not install batteries
 - pay large prices for electricity from the grid
 - Average usage factor SOE: ~90%
- Trend is valid until Cost SOE ~ 2 Cost AE
- If SOE not considered AE always preferred over PEME



- 1h dispatch considers bad case scenario for storage

GREEN-H₂: RESULTS LARGE H₂ PRODUCTION

- AE preferred; combines AE & SOE & storage in batteries (if batteries < 300 USD/kWh)



- Installation of wind generators is preferred over consuming from the grid
- Installation of solar => complementarity of the resource

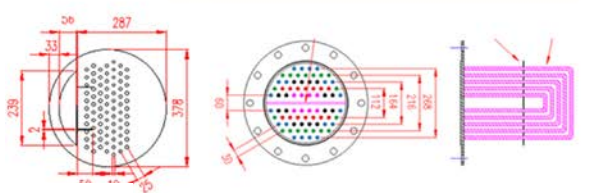
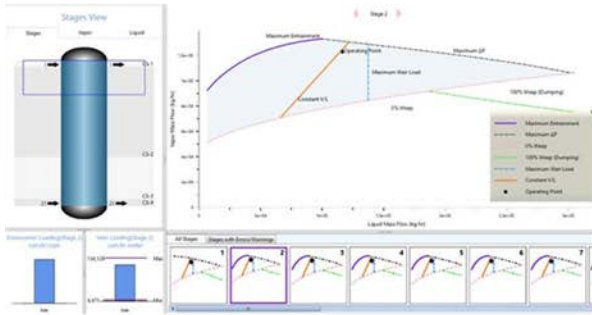
(Figures: batteries 100 USD/kWh—Tesla’s target)

SUMMARY: GREEN H₂

- Case study Uruguay: ~100 % renewable electricity
- Surplus → H₂ : not an option for current settings
- Options electricity :
 - (large) up to 50 tonH₂ /day install wind generators
 - beyond 50H₂ /day ton install wind + solar
 - consider batteries
- Electrolyzer technologies:
 - PEM's flexibility is not compensating its current cost => AE
 - SOE not yet in the market but look very promising

CO₂ CAPTURE & UTILIZATION-MOTIVATION

- Increasing pressure to lower CO₂ emissions
- Many capture & storage solutions: displace but not solve the problem



Development CO₂ capture process for a cement industry

- Tower directly connected to exhaust of clinker oven
- KEY: A *marketable* product that can be sold by the industry
- Solution is not universal
- Heat is required

• Design and evaluation in Aspen Plus

• A view of the pilot plant in operation

(Project ANII-HPI 147304, PI-Udelar: AI Torres, PI-Cementos Artigas: F. Gutiérrez)



ELECTROCATALYTIC REDUCTION OF CO₂ → CHEMICALS

- Very recent advances in chemistry

REVIEW | MATERIALS SCIENCE

Strategies in catalysts and electrolyzer design for electrochemical CO₂ reduction toward C₂₊ products

Lei Fan^{1,2,*}, Chuan Xia^{2,3,*}, Fangqi Yang⁴, Jun Wang⁴, Haotian Wang^{2,5,†} and Yingying Lu^{1,†}

Science Advances 21 Feb 2020; Vol. 6, no. 8, eaay3111; DOI: 10.1126/sciadv.aay3111

Article Figures & Data Info & Metrics eLetters PDF

Abstract

In light of environmental concerns and energy transition, electrochemical CO₂ reduction (ECR) to value-added multicarbon (C₂₊) fuels and chemicals, using renewable electricity, presents an elegant long-term solution to close the carbon cycle with added economic benefits as well.

REPORT

CO₂ electrolysis to multicarbon products at activities greater than 1 A cm⁻²

F. Pelayo García de Arquer^{1,*}, Cao-Thang Dinh^{1,*}, Adnan Ozden^{2,*}, Joshua Wicks^{1,3,*}, Christopher McCallum², ...

Science 07 Feb 2020; Vol. 367, Issue 6478, pp. 661-666; DOI: 10.1126/science.aay4217

Article Figures & Data Info & Metrics eLetters PDF

Graceful choreography for CO₂ and H₂O

One challenge for efficient electrochemical reduction of carbon dioxide (CO₂) is that the gas is hydrophobic, but many of its desirable reactions require water (H₂O). García de Arquer *et al.* addressed this problem by combining a copper electrocatalyst with an ionomer assembly that intersperses sulfonate-lined paths for the H₂O with fluorocarbon channels for the CO₂. The electrode architecture enables production of two-carbon products such as ethylene and ethanol at current densities just over an ampere per square centimeter.

Energy Reports

Volume 6, November 2020, Pages 761-770

Research paper

Impacts of deploying co-electrolysis of CO₂ and H₂O in the power generation sector: A case study for South Korea

Kosan Roh^a, Wonsuk Chung^b, Hyejin Lee^c, Seungman Park^d, Jay H. Lee^b

RETURN TO ISSUE | < PREV | **VIEWPOINT** | NEXT >

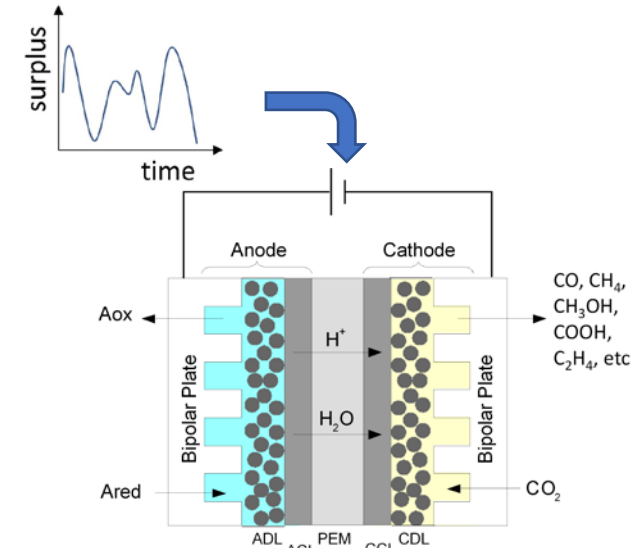
Integrating CO₂ Electrolysis into the Gas-to-Liquids–Power-to-Liquids Process

Svetlana van Bavel*, Sumit Verma*, Emanuela Negro, and Maarten Bracht

Cite this: ACS Energy Lett. 2020, 5, 8, 2597–2601
Publication Date: July 24, 2020
https://doi.org/10.1021/acsenergylett.0c01418
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Article Views: 2939 | Abstracts: 6 | Citations: 2

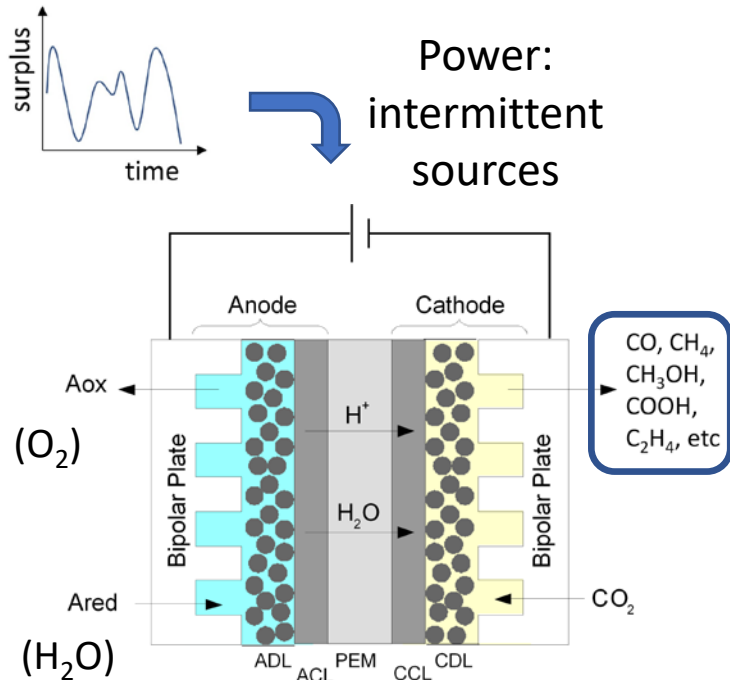
PDF (2 MB) | SUBJECTS: Oxides, Inorganic carbon compounds, Electrolysis, Power, Electrocatalysts



- Reactor can be coupled to intermittent energy sources => carbon negative chemicals

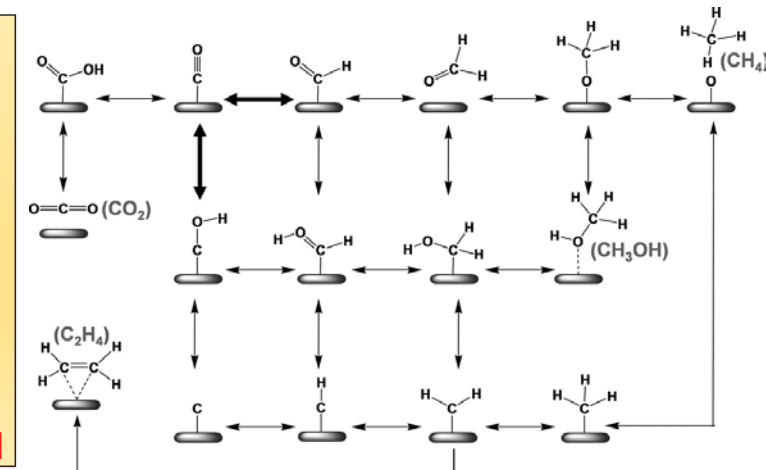
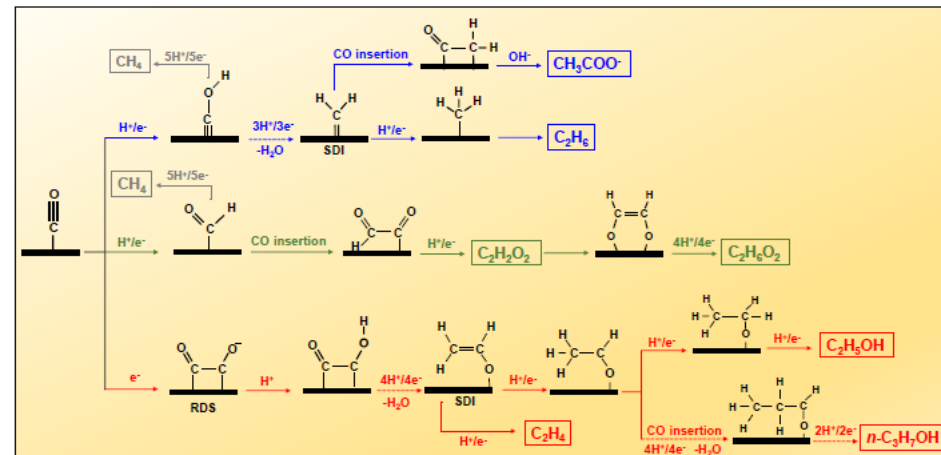
ELECTROCATALYTIC REDUCTION OF CO₂ (Work in Progress)

- Main challenge: Selectivity



Electro-catalysis:

- Catalytic surface promotes a series of elemental reactions
- Pathways on Cu surfaces



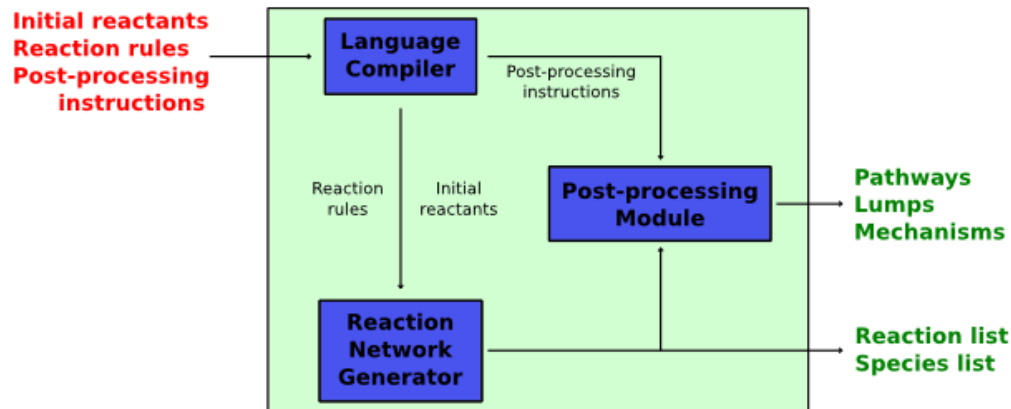
- Products and their distribution depend on catalyst, voltage, current density

=> Not a clear agreement on pathways/products

ELECTROCATALYTIC REDUCTION OF CO₂- BUILDING THE NETWORK

- Idea: use Rule Input Network Generator (RING¹) to build reaction network

RING (daoutidis.cems.umn.edu/software)



- Apply all reaction rules to all reactants, and species formed to generate all possible reaction pathways

- Screenshot of our code

```
input reactant "C(=O)=O"
input reactant "[H+]"
input reactant "{Cu}" <- A possible catalyst (M)
input reactant "{E1-}" <- electrons
//About global restrictions:
//No O-O, O-Ominus, O-electron allowed
//No electron-electron bonds
//No more than one O- connected to one same carbon
//We define a composite "atom" electron
define composite atom Cu
define composite atom E1

group electronAnyAtom (e1,carbon){
E1 labeled e1
C labeled carbon any bond to e1}
```

Some allowed reactions:

- Capture of an e-
- Form C-Metal bond
- Form C=Metal bond
- Form C≡Metal bond
- M-C-OH dehydration to form M-C-bond
- Form M-C-H bond (from M-C-)
- Desorption: breakage of C-M bond and formation of C-H bond
- etc

[1] Rangarajan & Daoutidis Rule Input Network Generator <https://daoutidis.cems.umn.edu/software>

ELECTROCATALYTIC REDUCTION OF CO₂- BUILDING THE NETWORK

- Partial view of the generated CO₂ -> chemicals network
- Compounds in squares show final stable products (>70)
 - Number of routes to different products:

Methanol	12	Oxalic acid	30	Propane	70
Formic acid	2	Ethylene	45	1-Propanol	67
Methane	12	Ethylenglycol	45	Acetic Acid	20
Ethane	40	Ethanol	40	glyoxal	32

- These products appear in the previous mechanisms and have been reported in different experimental contributions

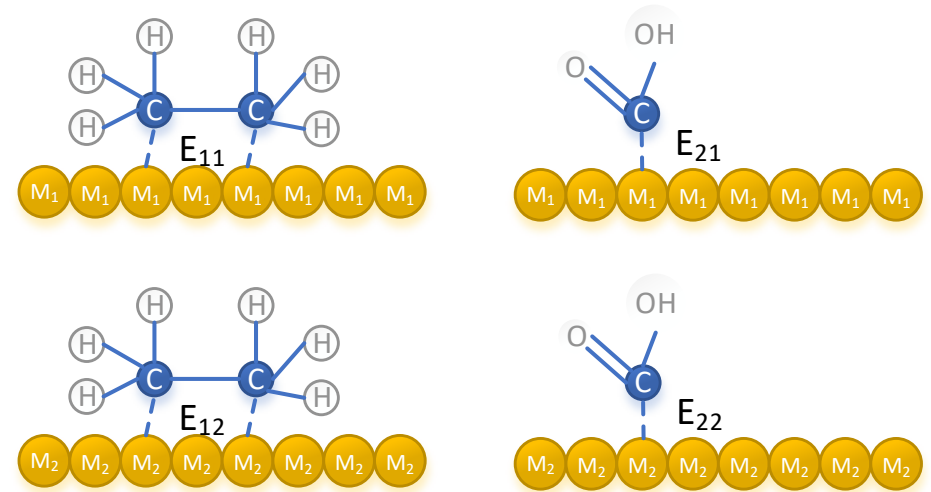
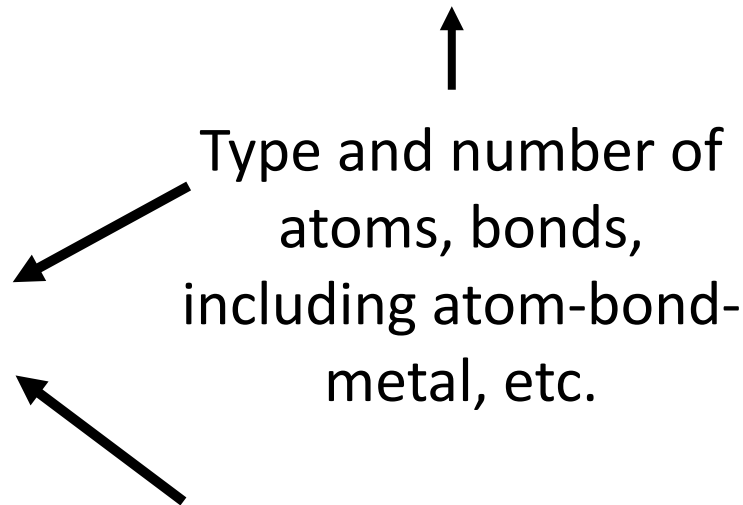
ELECTROCATALYTIC REDUCTION OF CO₂

- Next: assess which of these routes are thermodynamically feasible
 - Classical approach prediction using DFT calculations
 - DFT databases for a number of species/ surfaces
 - Can we use these databases to learn a model and predict for other species ?
- => Original idea Chowdury et al.,
Journal of Physical Chemistry, 2018
- Limitation just one DFT database

ELECTROCATALYTIC REDUCTION OF CO₂ – LEARNING A MODEL TO ESTIMATE ADSORPTION ENERGIES

- Model: $E_{ads} = f(\text{descriptors molecule, descriptors surface})$

Step 2: learn & validate model



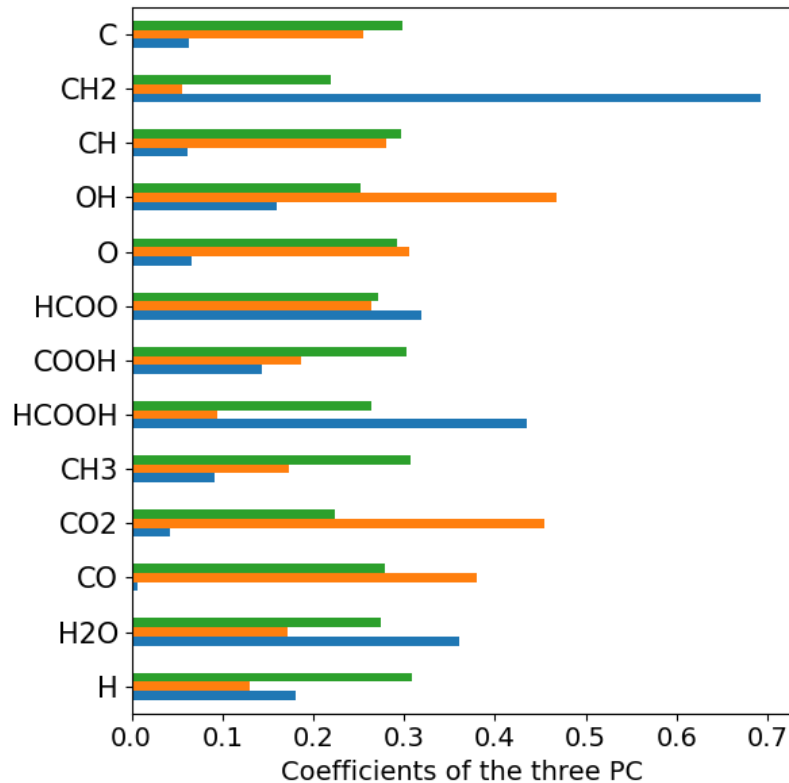
Step 0: Build database

Step 1: find the descriptors

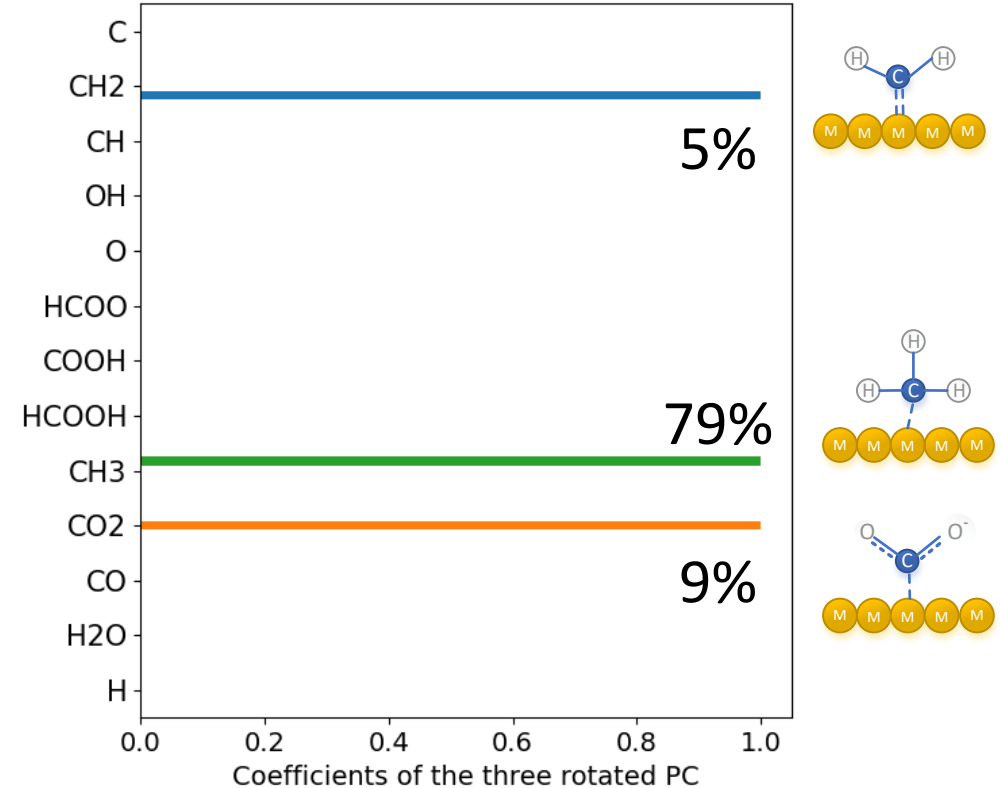
- Idea: Find the adsorbates whose E_{ads} vary the most for different surface
- Use those adsorbates as the descriptors

ELECTROCATALYTIC REDUCTION OF CO₂

- Step 1: Descriptors PCA 3 principal components 93% variation in data



Change of coordinates
 →
 (Varimax Rotation)

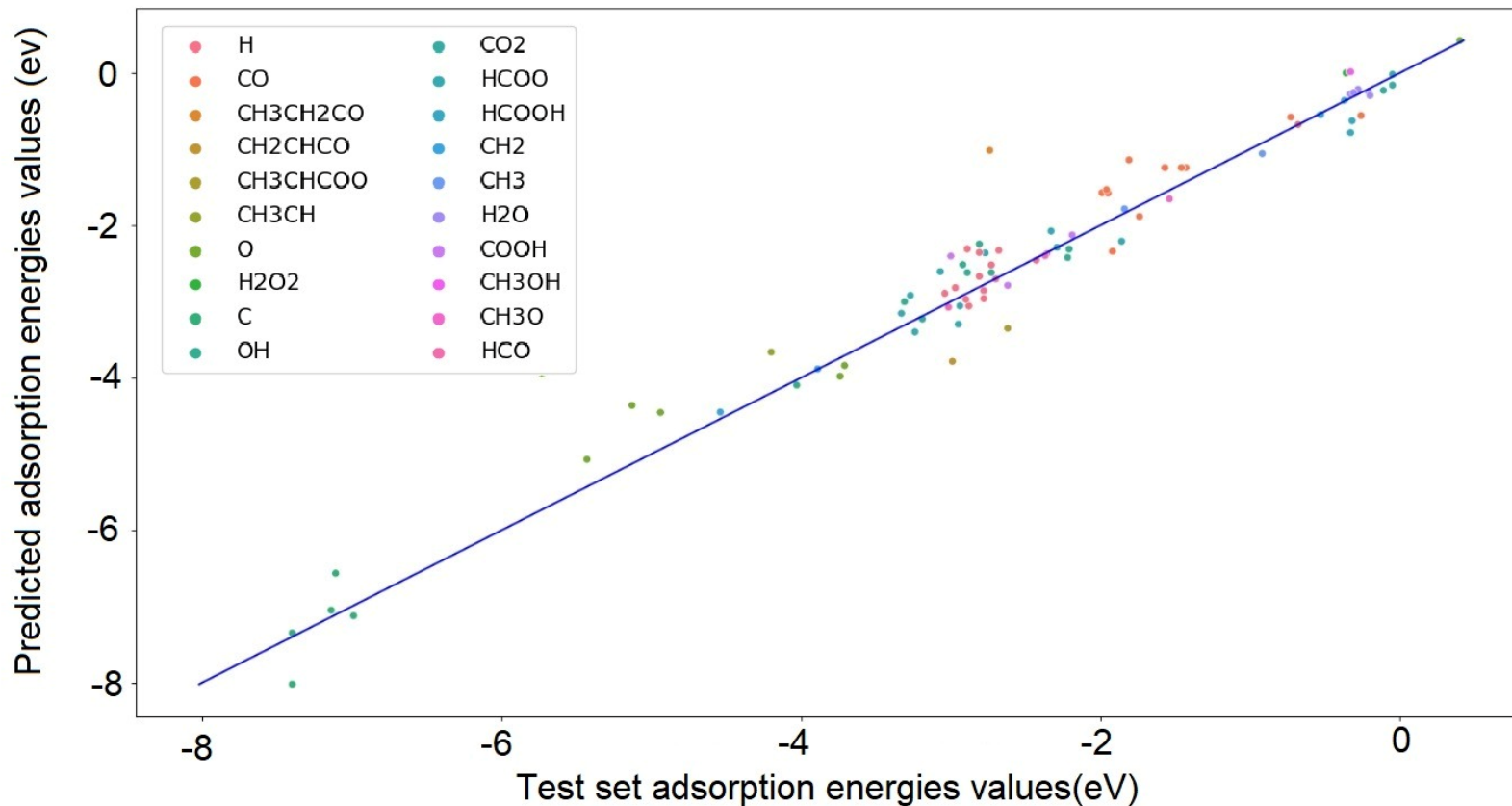


Surfaces: Cu, Pt, Pd, Rh, Re, Ru, Ag, Au, Fe, Ir, Os, Co, Ni

- If we want to test new surfaces, we need Eads from these 3 adsorbates

ELECTROCATALYTIC REDUCTION OF CO₂

- Step 2: Regression: tested several techniques; similar & good results
Predicted vs DFT data; validation set, KRR (radial basis functions)



- Expanded set of databases
- Next: combine model and CO₂ network

Arsuaga & Torres, submitted to ESCAPE 2022

SUMMARY: ELECTROREDUCTION OF CO₂

- Very promising route to capture CO₂ and produce green chemicals
- Electrocatalytic processes not well understood:
 - many products => lots of research opportunities,
 - many pathways collaboration with experimentalists
 - many possible cell geometries
- Initial work (in progress)
 - Building reaction network at metallic electrode
=> Find most favorable species and pathways

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J. Arsuaga



A. Porley

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M. Tejera



C. Phillipi



P. Ures



F. Mangone



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