

# Optimization For Grade Transitions In Polyethylene Solution Polymerization

Jun Shi<sup>1</sup>, Lorenz T. Biegler<sup>1</sup>

Intan Hamdan<sup>2</sup>, Sarat Munjal<sup>2</sup>, John Wassick<sup>2</sup>,  
Scott Bury<sup>2</sup>, Shawn Feist<sup>2</sup>, Alex Kalos<sup>2</sup>

<sup>1</sup>Center of Advanced Process Decision-making  
Department of Chemical Engineering  
Carnegie Mellon University

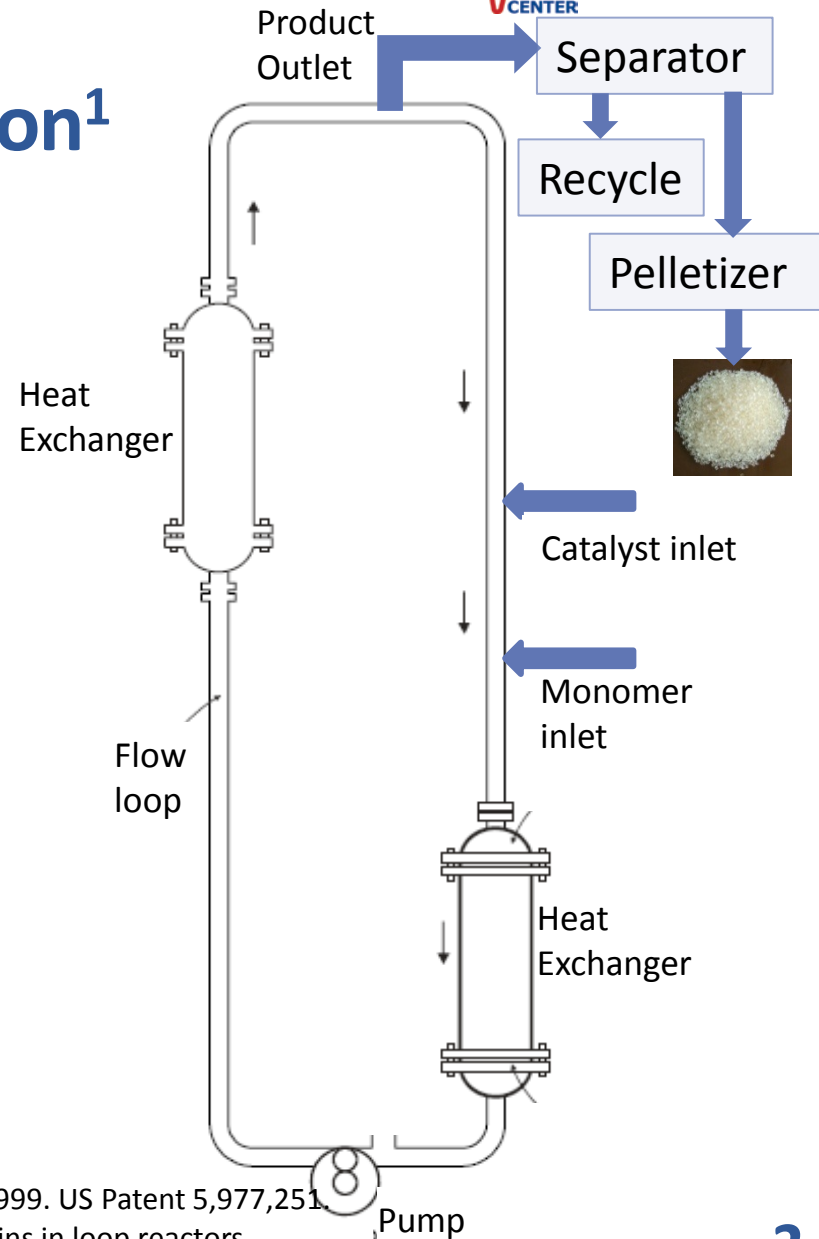
<sup>2</sup>The Dow Chemical Company

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# Background

## LLDPE Solution Polymerization<sup>1</sup>

- Linear low-density polyethylene (LLDPE)
- Made by copolymerization of ethylene with longer-chain olefins (octene, butene, hexene, propylene)
- Long loop with heat exchangers
- Continuous operation
- Multiple feed positions for:  
Ethylene, Comonomer, Catalyst, Solvent, Hydrogen



1. Che I Kao et al. Non-adiabatic olefin solution polymerization, November 2 1999. US Patent 5,977,251

2. J.J. Zacca and W.H. Ray. Modelling of the liquid phase polymerization of olefins in loop reactors.

Chemical Engineering Science, 48(22):3743–3765, 1993.

## Project Overview

# Motivation and Objectives

### Current Practice

- Different grades produced in a **single production line**
- Grade transition takes a **long time**
- **PID** controller for flowrate and temperature control
- Hard to implement complex transitions; Room for improvement

### Objectives

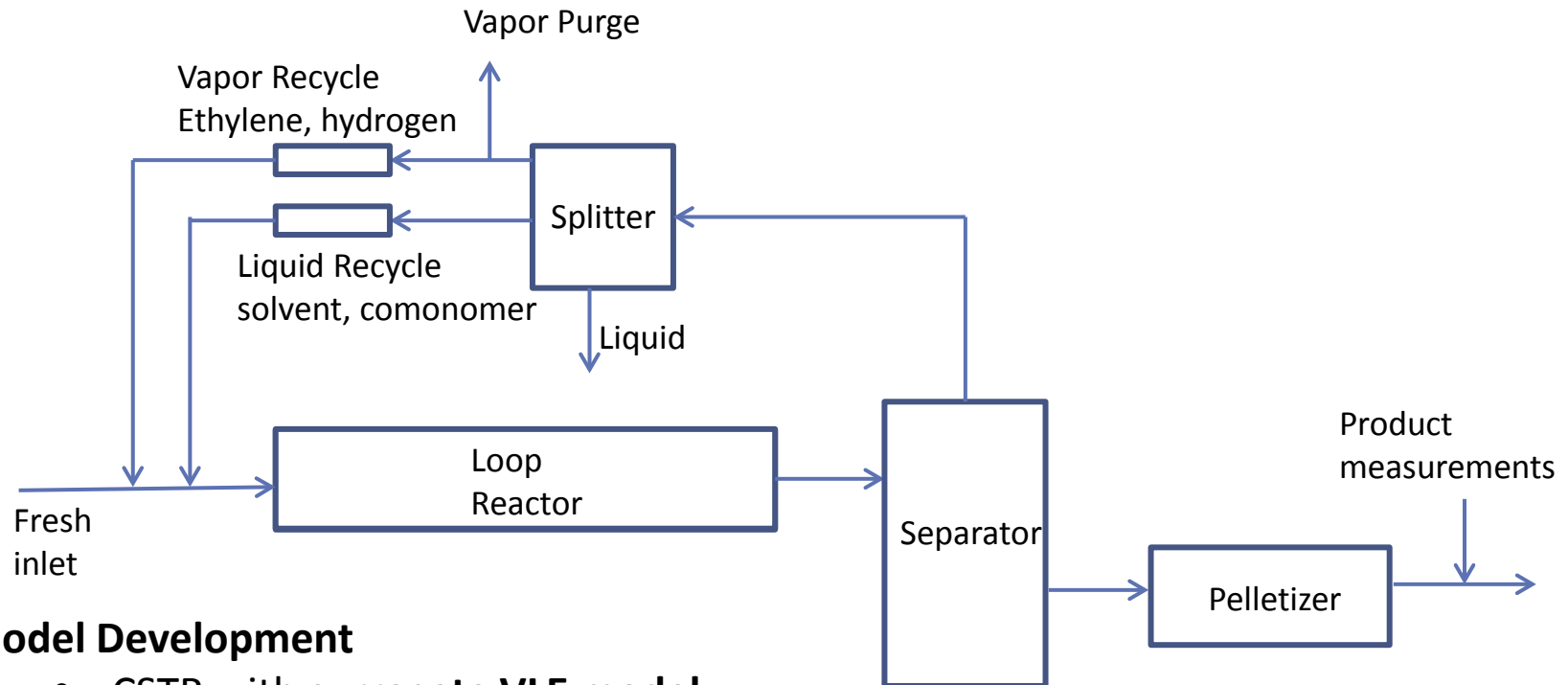
- Develop a model based control and optimization framework to
  - Minimize **transition time**
  - Minimize **offgrade products**

### Potential Value

- **Reduction** of transition time
- **Guided** complex transitions
- Increased **flexibility** in production wheel

## Project Progress

# Model Development and Offline Optimization



### Model Development

- CSTR with **surrogate VLE model**
- Method of moment for product property prediction
- *Recycle time delay model*
- *Process constraints*

### Offline Dynamic Optimization

- Single stage optimization
- *Multistage optimization*

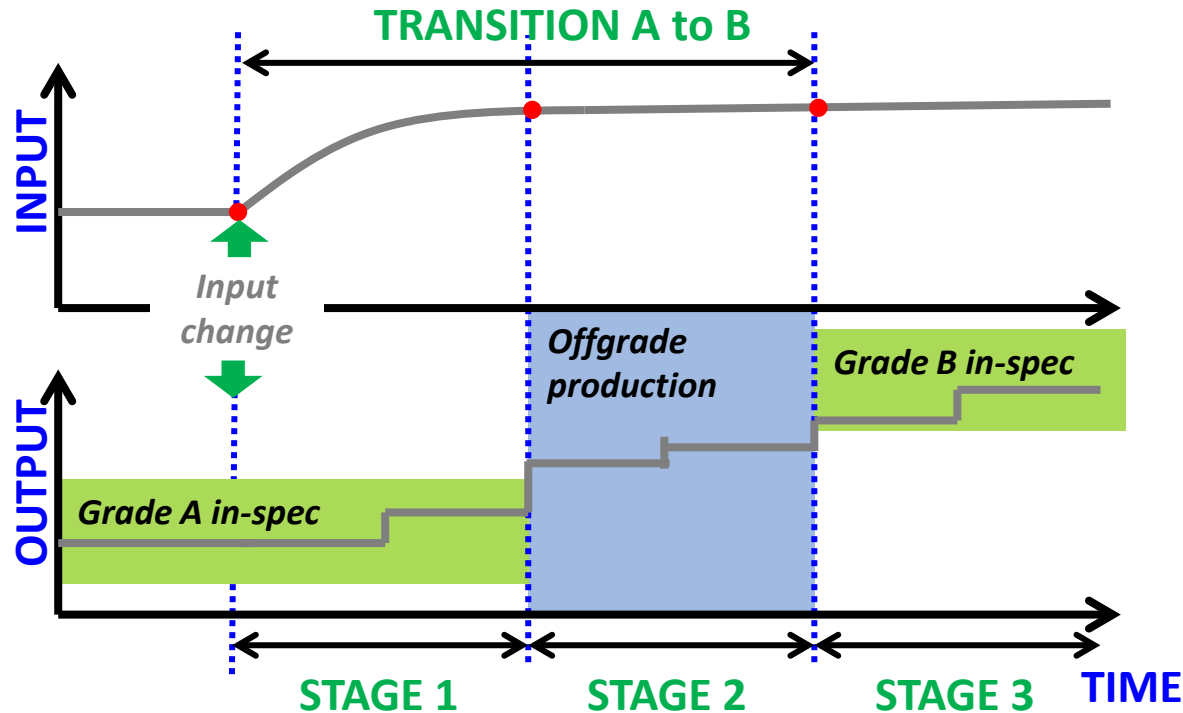
$$\min \int_0^{tf} \|x(t) - x^*\|_Q^2 + \|u(t) - u^*\|_R^2 dt$$

# Dealing with Specification Bands

## Multistage Optimization

$$\rho^* = 0.9 \pm 0.0025 \text{ g/cm}^3$$

instead of  $\rho^* = 0.9 \text{ g/cm}^3$



### Motivation:

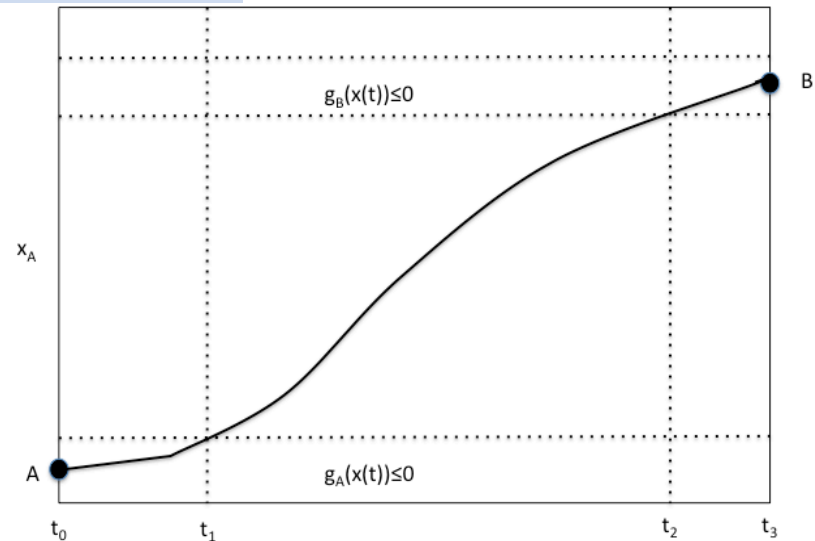
- In-spec product is qualified for sale.
- Specification band should be taken into account when calculating off-grade.

# Dealing with Specification Bands

## Multistage Optimization

$$\text{Min } \left( \begin{array}{|c|} \hline \text{Off-} \\ \hline \text{spec} \\ \hline \end{array} \right) + \left( \begin{array}{|c|} \hline \text{Trans.} \\ \hline \text{Time} \\ \hline \end{array} \right) + \left( \begin{array}{|c|} \hline \text{Regularizing Term} \\ \hline \end{array} \right)$$

- s.t.*
- Dynamic model
  - Grade A in-spec in Stage1
  - Grade B in-spec in Stage3
  - Continuity between stages
  - Initial and Final Conditions



- **3 stages:**  
in-spec of A, out-of-spec and in-spec of B.
- Minimize a combination of **the off-spec product between t1 and t2** and **the transition time t2-t0**. A regularizing term that promotes a smooth unique solution.
- Application of 3-point collocation on 18 finite elements over 4.5 hours
- An NLP problem with over 63000 equations and over 63000 variables
- Simultaneous dynamic optimization with moving finite element

## Case Studies

# Grade Transitions between Two Grades

## Operation conditions for two different grades<sup>4</sup>

|                              |                   | Meaning                  | Units             | Grade A               | Grade B               |
|------------------------------|-------------------|--------------------------|-------------------|-----------------------|-----------------------|
| <b>Properties</b>            | <b>MI</b>         | Melt index               | g/10min           | 1.0                   | 12.0                  |
|                              | <b>Conversion</b> | Ethylene conversion rate |                   | 0.980                 | 0.850                 |
|                              | <b>Density</b>    | Product density          | g/cm <sup>3</sup> | 0.908                 | 0.864                 |
| <b>Manipulated Variables</b> | <b>Tji</b>        | Inlet cooling water temp | °C                | 133.37                | 131.36                |
|                              | <b>F2</b>         | Ethylene inlet flow      | L/s               | 3.43                  | 3.26                  |
|                              | <b>F8</b>         | Comonomer inlet flow     | L/s               | 0.18                  | 1.30                  |
|                              | <b>FH</b>         | Hydrogen inlet flow      | L/s               | 3.38*10 <sup>-4</sup> | 5.37*10 <sup>-4</sup> |
|                              | <b>Fc</b>         | Feed catalyst            | L/s               | 0.93*10 <sup>-2</sup> | 2.65*10 <sup>-2</sup> |
|                              | <b>Fs</b>         | Solvent inlet flow       | L/s               | 0.167                 | 0.158                 |

For each transition, step change simulation is performed as a baseline

- Typical way to perform grade transitions; May go to infeasible region

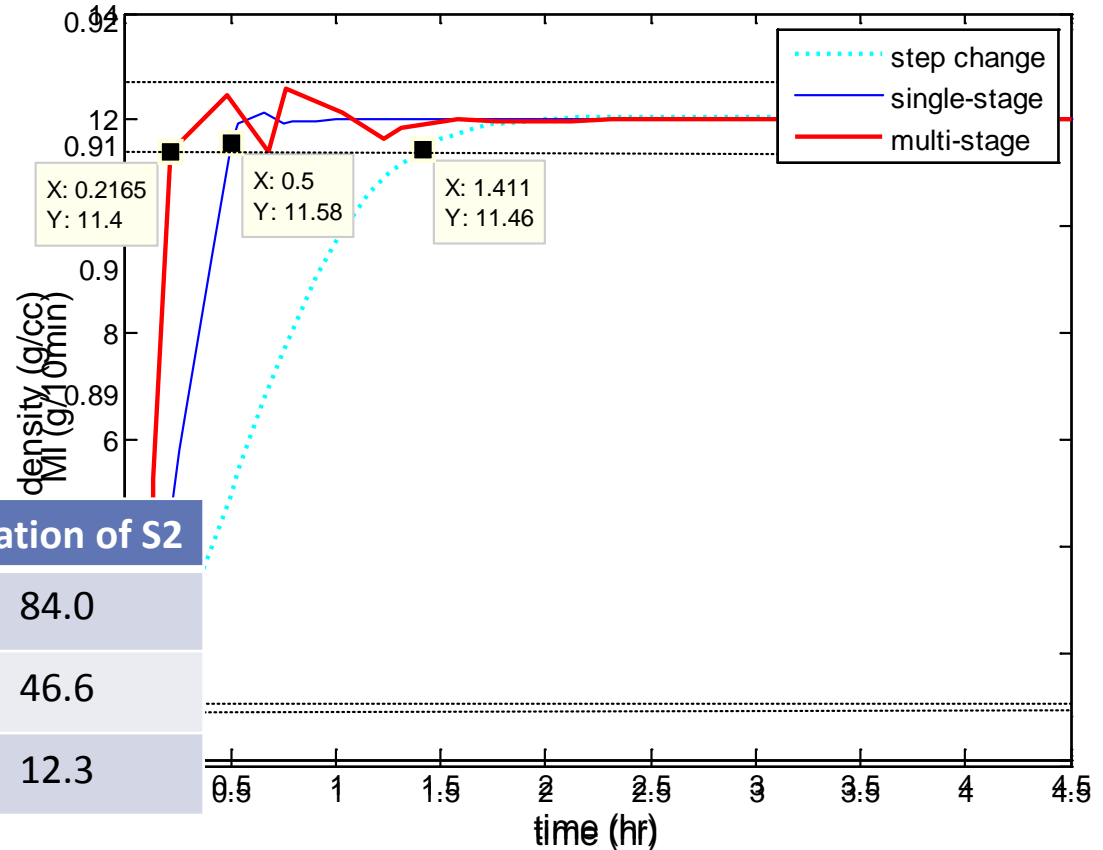
Specification bands:  $\pm 0.0025 \text{ g/cm}^3$  for density,  $\pm 5\%$  for melt index.

# To Lower Density and Higher MI

## Comparison of Output Profiles

### The multistage solution

- A faster transition to reach the boundary of the second band
- More oscillations within the specification band
- Better performance



| in min       | Trans. Time | Duration of S2 |
|--------------|-------------|----------------|
| Step change  | 84.7        | 84.0           |
| Single-stage | 47.3        | 46.6           |
| Multistage   | 13.0        | 12.3           |



# Novelty

## **Built and integrated a surrogate VLE model**

- Accurate predictions with reduced model complexity

## **Single-stage formulation**

- A common approach in dynamic optimization of grade transitions
- But, not minimizing transition time or off-grade product directly.
- Also, single value target is not practical.

## **Multistage formulation**

- Specification bands are considered in some studies where integrated scheduling and dynamic optimization problem is solved.
- Takes specification bands into account
- Capable of minimizing transition time and off-grade product directly
- Has better performance (greatly reduces the transition time and the off-grade product)

# Potential Value and Future Work

## Potential Value

- **Reduction** of transition time and off-grade product
- **Guided** complex transitions
- Increased **flexibility** in production wheel

## Future Work

- With accurate model and constraints we obtained, the resulting optimal transition profiles can be used as optimal trajectories.
- The performance can be further improved by tuning parameters and refining the model.
  - Identifying all the constraints and evaluating the solutions are necessary
- Online optimization and control issues will be considered in next step.
  - Computational time should be lowered if repeated optimization runs are performed during the process
  - Uncertainties/disturbances need to be taken into account