

Optimization For Grade Transitions In Polyethylene Solution Polymerization

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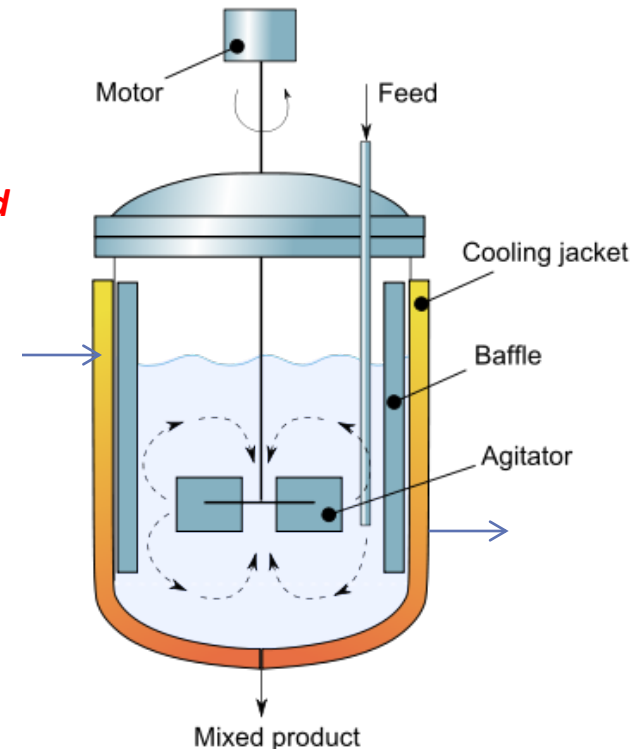
Dynamic Optimization Models

Grade Transition for LLDPE

- **Continuous Stirred-Tank Reactor (CSTR)**
(represents two actual processes)
- Assume perfect mixing
- Three types of variables F_1, F_2, F_h, F_c
 - Manipulated variables
 - *Ethylene, comonomer, hydrogen and catalyst feed flowrates*
 - *Inlet temperature of cooling media*
 - Output variables
 - *Product properties: MI and density*
 - *Process requirement: ethylene conversion and reactor temperature*
 - State variables
 - *Concentrations and moments*
- **Method of moments**
 - predict product properties from state variables

Reactions:

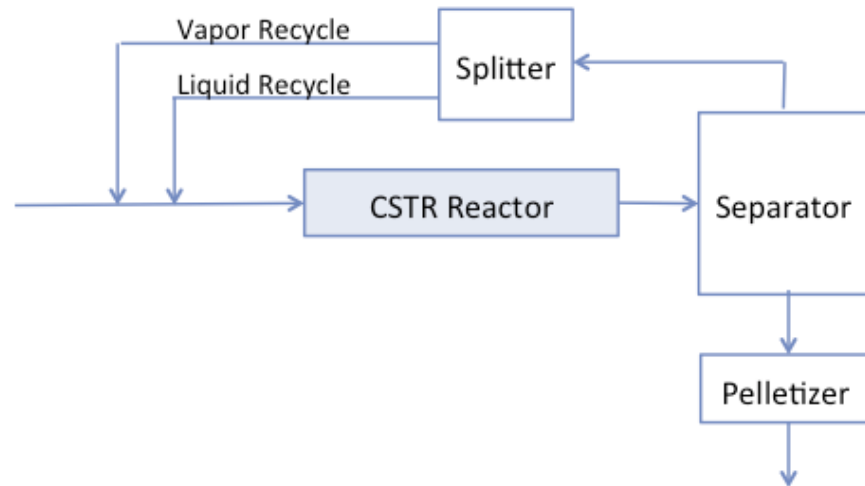
- Chain initialization
- Chain propagation
- Chain transfer
- Site deactivation



Process Model Development

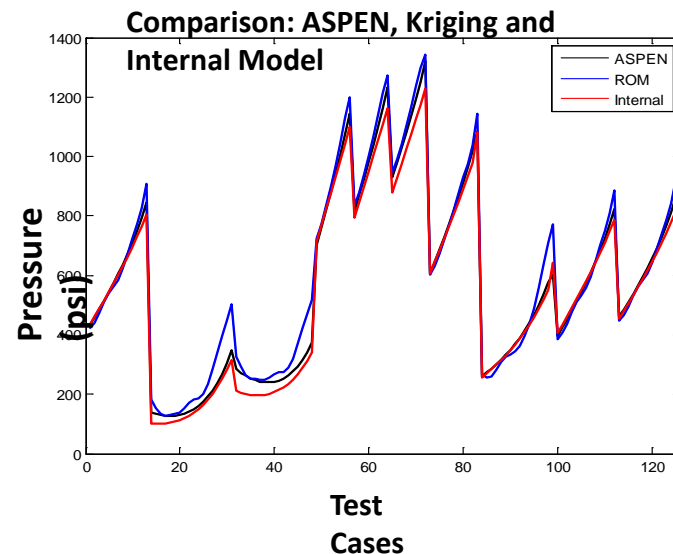
Assumptions and Components

- Perfect mixing
- Chain Initiation,
- Chain Propagation,
- Chain Transfer,
- Site Deactivation.

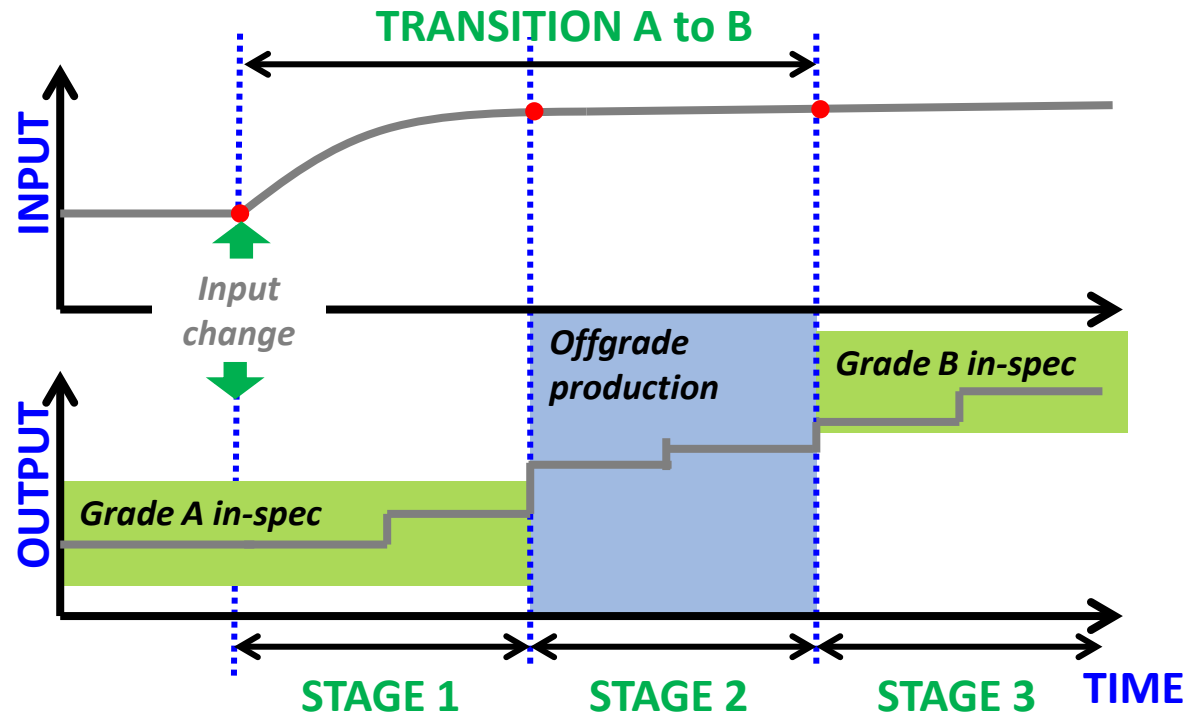


- **The model has five parts**

- Mass and heat balance
- Moment model
- *Surrogate model for VLE*
- *Recycle time delay model*
- *Process constraints*



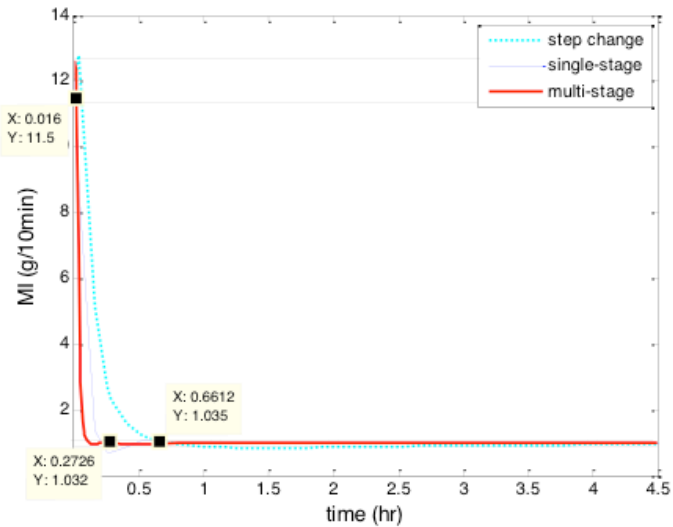
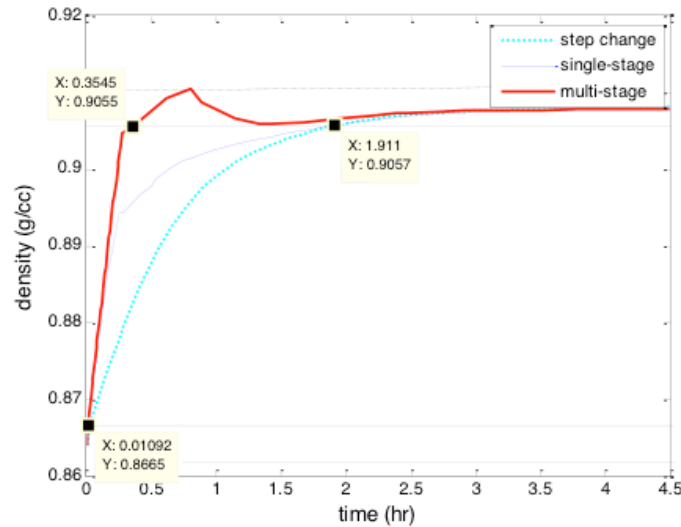
Dealing with Specification Band Multistage Optimization



Motivation:

- In-spec product is qualified for sale.
- Specification band should be taken into account when calculating off-grade.

Results and Analysis



	Transition Time	Duration of Stage 2
Multistage	21.3 min	20.3 min
Single-stage	114.7 min	113.7 min

**Fast transition in S2
Oscillations within
the specification band**

The multistage solution

- A faster transition to reach the boundary of the second band
- More oscillations within the specification band
- Better performance