

# Optimization of Crude-Oil Blending Operations

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# Introduction

## Goal

Optimize the schedule of operations for the crude-oil problem using a MINLP scheduling model

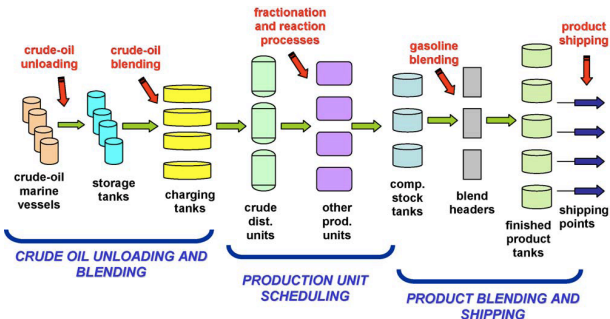
## Tools

- MINLP: Mixed Integer NonLinear Programming
- MILP: Mixed Integer Linear Programming
- NLP: NonLinear Programming

- 1 Problem statement
  - Oil refinery
  - Crude-oil blending scheduling
  - Scheduling formulations
- 2 Proposed approach
  - Basic idea
  - MINLP model
  - Search procedure
- 3 Results and comparisons
  - Computational results
- 4 Conclusion

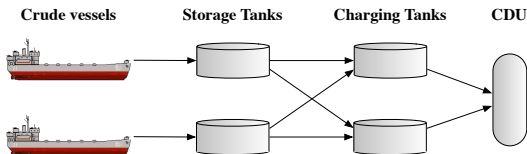
# A typical oil refinery

- Refining crude-oil into useful petroleum products:
  - LPG, gasoline, diesel fuel, kerosene, heating oil, asphalt base
- 3 phases:
  - Crude-oil unloading and blending
  - Fractionation and reaction processes
  - Product blending and shipping



# Crude-oil operations scheduling problem

- Scheduling horizon  $[0, H]$
- 4 types of resources:
  - Crude-oil marine vessels
  - Storage tanks
  - Charging tanks
  - Crude Distillation Units (CDUs)
- 3 types of operations:
  - **Unloading**: Vessel unloading to storage tanks
  - **Transfer**: Transfer from storage tanks to charging tanks
  - **Distillation**: Distillation of charging tanks



# Problem definition

## Given

- Refinery configuration
- Logistics constraints
- Initial tank inventory and composition
- Vessel arrival time, inventory level and composition
- Distillation specifications and demands (planning decisions)

## Determine

- Required operations
- Timing decisions
- Transfer volumes

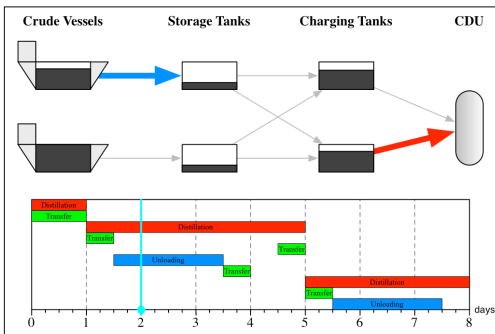
## Minimize

- Costs of distilled crude-oil mixtures

# Example of crude-oil operations schedule

## Common logistics constraints

- Only one docking station available for vessel unloading
- No simultaneous inlet and outlet operations on tanks
- Continuous distillation



Refinery operations

Gantt chart

# Scheduling formulations

- **Fixed Time Grid**
  - Kondili et al. (1993), Shah et al. (1993), Pantelides (1994)
  - **Crude-oil scheduling**: Shah (1996), Lee et al. (1996)
- **Variable Time Grid**
  - Zhang and Sargent (1996), Schilling and Pantelides (1996), Mockus and Reklaitis (1997)
  - **Crude-oil scheduling**: Moro and Pinto (2004)
- **Single-Operation Time-Slots (event-based formulation)**
  - Ierapetritou and Floudas (1998a, 1998b)
  - **Crude-oil scheduling**: Jia et al. (2003)
- *Multi-Operation Time-Slots*



# Basic Idea

## Basic steps

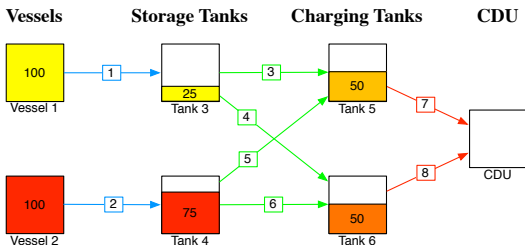
- 1 **Postulate** the number of **time-slots** that are needed
- 2 **Define** an ordered set of **time-slots**
- 3 **Define** the set of all transfer **operations**
- 4 **Assign** exactly one **operation** to each **time-slot** and **determine** the **timing** and **volume** decisions

## MINLP model

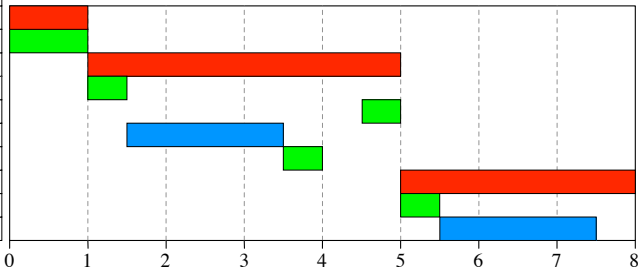
- Binary variables: **assignment** variables
- Continuous variables: **time**, **volume** and **level** variables

## Basic idea

## An example of time-slots assignment



Task	Operation	Volume
1	Distillation 7	5
2	Transfer 6	50
3	Distillation 8	100
4	Transfer 3	25
5	Transfer 5	19.5
6	Unloading 1	100
7	Transfer 3	5.5
8	Distillation 7	95
9	Transfer 6	5.5
10	Unloading 2	100

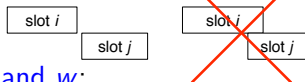


# Main sets and variables

- Ordered set of unspecified time-slots  $i \in \{1, \dots, n\}$ 
  - Start time:  $TS^i \in [0, H]$
  - End time:  $TE^i \in [0, H]$
- Set of operations  $v \in \{1, \dots, N_v\}$
- Assignment variables  $Z_v^i \in \{0, 1\}$ 
  - Operation  $v$  is assigned to time-slot  $i$  iff  $Z_v^i = 1$
  - Exactly one operation for each time-slot:  $\sum_v Z_v^i = 1$

# Non-overlapping constraints

- For each ordered pair of time-slots  $i \prec j$  and for each pair of non-overlapping operations  $v$  and  $w$ :



$$\left\{ \begin{array}{l} Z_v^i = Z_w^j = 1 \Rightarrow NO_{ij} = 1 \\ NO_{ij} = 1 \Rightarrow TE^i \leq TS^j \end{array} \right. \Rightarrow \left\{ \begin{array}{l} NO_{ij} \geq Z_v^i + Z_w^j - 1 \\ TE^i \leq TS^j + M \cdot (1 - NO_{ij}) \end{array} \right.$$

- For example,
  - Vessel unoadings 1 and 2:

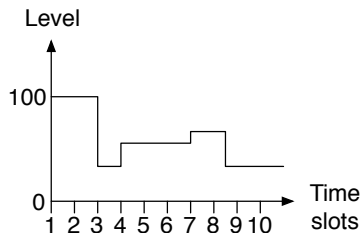
$$NO_{ij} \geq Z_1^i + Z_2^j - 1$$

- Distillation transfers 7 and 8 (use same CDU):

$$NO_{ij} \geq Z_7^i + Z_8^j - 1$$

# Tank inventory and composition constraints

- Tanks  $t \in \{1, \dots, N_t\}$
- Crude-oil types  $c \in \{1, \dots, N_c\}$
- Volume variables  $V_v^i, V_{vc}^i \geq 0$
- Level variables  $L_t^i, L_{tc}^i \geq 0$
- Tank inventory constraints:
  - $L_t^{i+1} = L_t^i + \sum_{v \in IN(t)} V_v^i - \sum_{v \in OUT(t)} V_v^i$
  - $\underline{L}_t \leq L_t^i \leq \bar{L}_t$
- Tank composition constraints:
  - $Z_v^i = 1 \Rightarrow \frac{V_{vc}^i}{V_v^i} = \frac{L_{tc}^i}{L_t^i}$  (nonlinear)
  - $\left. \begin{array}{l} L_t^i = \sum_c L_{tc}^i \\ V_v^i = \sum_c V_{vc}^i \end{array} \right\}$  linear relaxation



# Other constraints

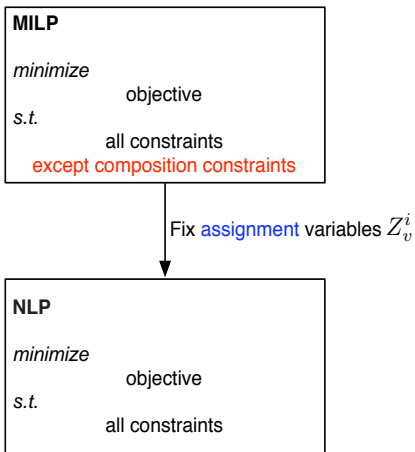
- Continuous distillation
- Flowrate limitations:  $\underline{FR}_v \cdot (TE^i - TS^i) \leq V_v^i \leq \overline{FR}_v \cdot (TE^i - TS^i)$
- Scheduling constraints:
  - Vessels availability time window
  - Precedence constraints
- Crude-oil mixture specification and demand
- Objective function:

$$OBJ = \sum_{t \in CDUs} \sum_c COST_c \cdot L_{tc}^n$$

# MILP-NLP decomposition

## Decomposition steps

- 1 **Master problem:** find optimal solution for the MILP relaxation
- 2 Solution may not satisfy the **nonlinear composition constraints**
- 3 Fix **assignment** variables
- 4 **Slave problem:** find optimal solution for the resulting NLP **(with nonlinear composition constraints)**



## Sensitivity to the number of time-slots

- MILP-NLP decomposition tested on case-study with 5 to 13 slots
- Size of the MINLP with 13 time-slots:  
1575 binary variables, 1419 continuous variables, 4429 constraints
- Feasible schedule obtained with 9 time-slots
- Optimal schedule obtained with 10 time-slots

Nb of slots	LP	MILP	CPU	Nb of Nodes	NLP	Gap
5	Infeas					
6	117.5	Infeas	0s	1		
7	83.7	Infeas	1s	29		
8	82.5	Infeas	2s	115		
9	82.5	120.28	3s	147	121.25	0.8%
10	82.5	120.25	4s	116	120.25	0%
11	82.5	120.25	7s	97	120.25	0%
12	82.5	120.25	6s	75	120.25	0%
13	82.5	120.25	2s	17	120.25	0%



# Comparison with other algorithms

- Number of time-slots: 13
- Algorithms used:
  - MILP-NLP decomposition: Xpress (MILP), CONOPT (NLP)
  - MINLP solvers: DICOPT, SBB, AlphaECP, BARON (global optimum)

Algorithm	Solution	CPU time
MINLP-NLP	120.25	2s
DICOPT	120.25	18s
SBB	120.25	81s
AlphaECP	120.25	468s
BARON	120.25	219s

⇒ Order of magnitude reduction for CPU time.

# Larger instances

- Approach tested on the 4 problems from Lee et al. (1996)
- Problems solved with the **maximum number of time-slots** needed
- Problem 3 shows a gap of **4.9%** between the MILP and NLP solutions

Example	Vessels/Storage/Charging/CDUs	Slots	MILP	NLP	Gap	CPU
1	2 / 2 / 2 / 1	13	120.25	120.25	0%	2s
2	3 / 3 / 3 / 2	21	198.83	198.83	0%	104s
3	3 / 3 / 3 / 2	21	59.60	62.50	4.9%	73s
4	3 / 6 / 4 / 3	26	107.47	107.47	0%	506s

# Conclusion and future work

## Conclusion

- New MINLP formulation for the crude-oil operations problem
- Handles logistics constraints and minimization crude-oil costs
- MILP-NLP decomposition algorithm compares well to MINLP solvers

## Future work

- Hybrid optimization: Constraint Programming as a symmetry-breaking branching tool
- Enhance the MILP-NLP decomposition
- Take into account stochastic parameters (vessels arrival time)
- Practical case-study

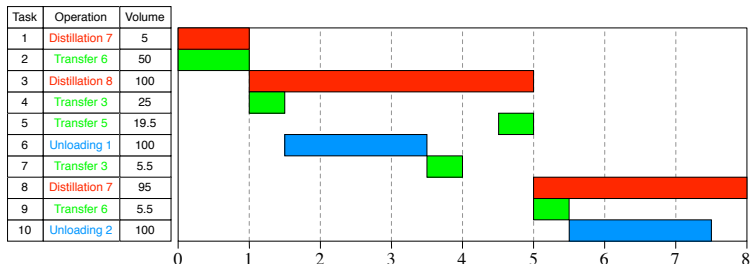
## Discrete formulation

- Discretization of the time horizon into  $n$  fixed-length adjacent time-slots
- Identical MILP-NLP decomposition
- Example 4 from Lee et al. (1996), optimal solution: 107.47

Nb of slots	LP	MILP	CPU	Nb of nodes	NLP	Gap
5	107.87	Infeas	0s	1		
10	107.49	107.80	385s	74627	107.80	0%
15	107.47	107.77	29s	1853	Local Infeas	
20	107.45	107.68	*3600s	*199800	107.68	0%
25	107.45	107.63	*3600s	*41300	107.63	0%

# Symmetry breaking

- Multiple operation assignment may lead to the same schedule
- For instance, exchanging operations assigned to slots 1 and 2 in the following gantt chart leads to the same solution

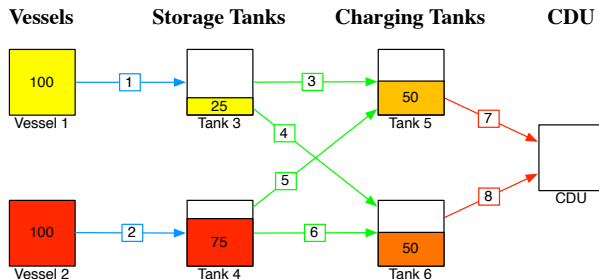


# Regular language derivation

- The possible sequences of operations are represented by a **regular language** (Regular constraint by Côté et al., 2007)
- Example 1 has 2 refinery states: distillation 7 or 8
- During distillation state 7:

$$L_7 = 7(\epsilon + 4)(\epsilon + 6)(\epsilon + 1 + 14)(\epsilon + 2 + 26)$$

- Overall:  $L = (\epsilon + L_7)(L_8L_7)^*(\epsilon + L_8)$



# Automaton representation

- The regular language  $L_7 = 7(\epsilon + 4)(\epsilon + 6)(\epsilon + 1 + 14)(\epsilon + 2 + 26)$  can be recognized by the following Deterministic Finite Automaton (DFA)
- Each node is equivalent to a state
- Each arc corresponds to an operation assigned to a task

