



**Carnegie Mellon**



# **Integration of Reservoir Modelling with Oil Field Planning and Infrastructure Optimization**

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- ❖ **Goal:** To optimize the investment and operations decisions for oil and gas field development problem with computational ease and sufficient accuracy.
- ❖ Recent simultaneous models assume fixed linear reservoir production profiles or piecewise linear approximations that led to suboptimal solutions.
- ❖ **Objective:** Develop models to incorporate detailed reservoir profile for accurate planning.

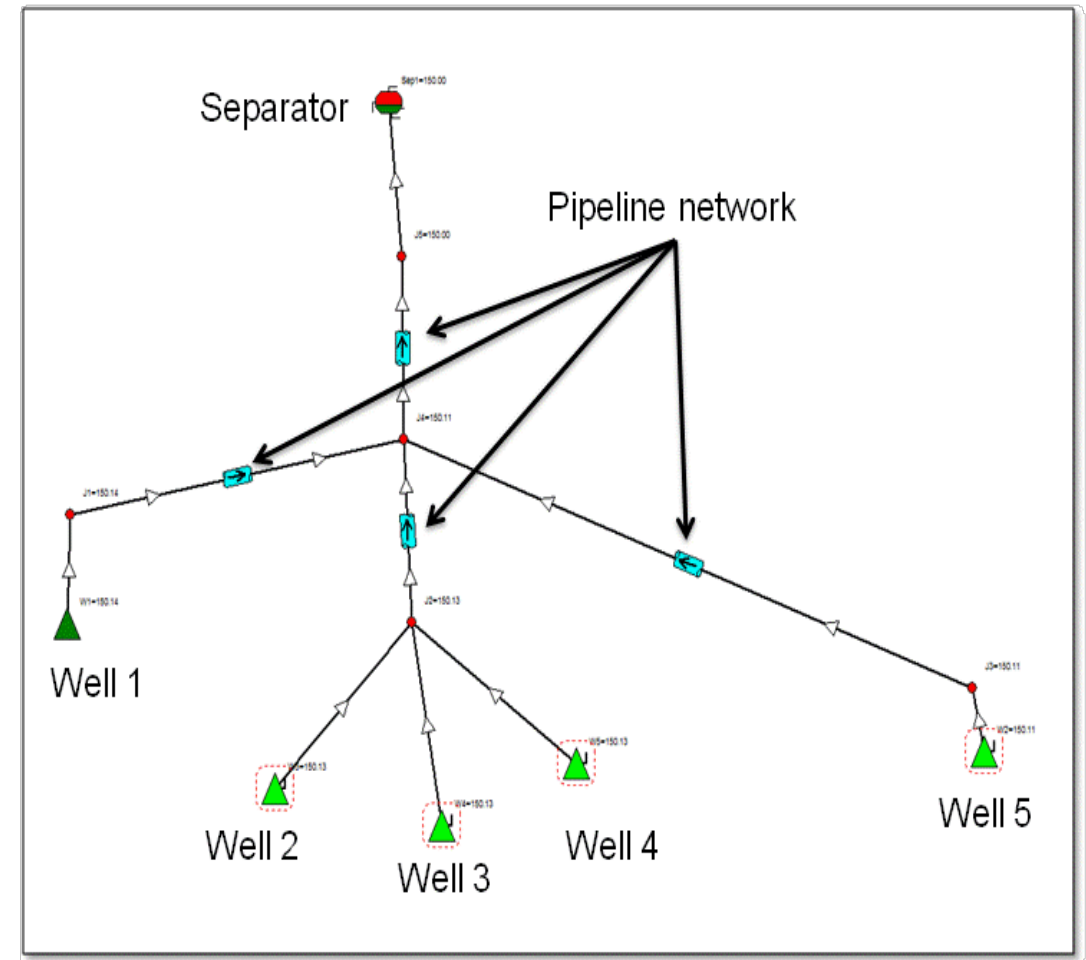
❖ **Given information:**

- ✓ Number and location of wells.
- ✓ Productivity indices and Pressure Profiles.
- ✓ Variation of GOR and WOR.
- ✓ Maximum Separator Capacity of 8000 bbl./year.
- ✓ Selling prices and Costs.

- ❖ **Objective** is to **maximize the NPV** in the long term horizon.
- ❖ Initial investment of **150 MUSD** is not included in the objective function since it is constant and is paid up-front.

❖ **Assumptions:**

- Natural Depletion of the reserves.
- Pipeline network is already established.
- Planning horizon is discretized into a number of time periods 't', typically 1 year.
- Water is re-injected into the well after separation and gas is sold.

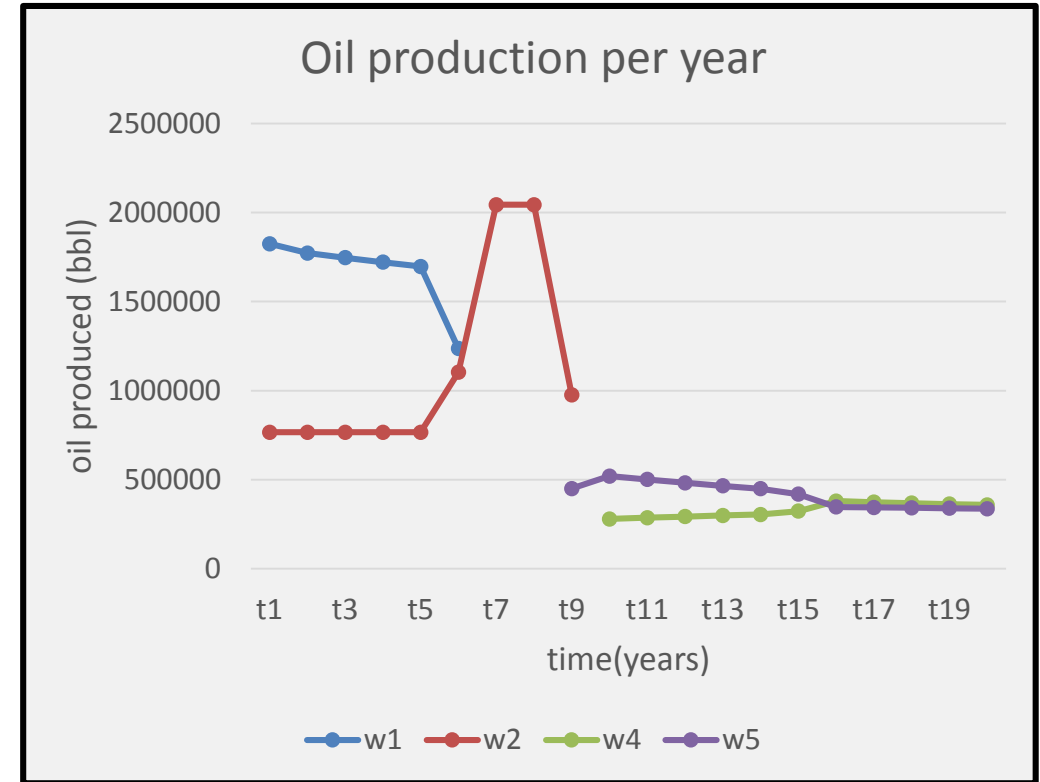


- Objective function: Maximize NPV,  $NPV = \sum_{\text{time}} [\text{REV}(t) - \text{COST}(t)] * \text{disc}(t)$
- Total Revenue:  $\text{REV}(t) = \text{del}(t) * (\text{oil price}(t) * \text{oil produced}(t)) + (\text{gas price}(t) * \text{gas produced}(t))$
- Total costs:  
 $\text{COST}(t) = \text{del}(t) * (\text{gas compression cost} * \text{gas produced}(t)) + (\text{water treatment} * \text{water produced}(t))$
- Total Liquid Produced:  
 $\text{Liquid produced (well, time)} = \text{Productivity index (well)} * \text{Pressure variation(well, time)}$
- Oil produced(well, time) =  $\text{Liquid produced} * (1 - \text{wct\%}(well, time))$  ← Nonlinearity
- Gas produced(well, time) =  $\text{Oil produced}(well, time) * \text{GOR}(well, time)$
- Total liquid produced(time) =  $\sum_{\text{well}} \text{Liquid produced}(well, time)$
- Upper bound for liquid produced:  $\text{Total liquid produced}(t) \leq \text{Maximum separation capacity}(t)$
- Upper bound for Oil production:  $\sum_{\text{well}} \text{Oil recovered}(well, time) \leq \text{Cumulative Oil produced (well)}$

❖ NPV = 1119 MUSD

❖ Model Statistics (BARON 14.4):

- ✓ Number of wells: 5
- ✓ Number of time periods: 20 time periods of 1 year each.
- ✓ Number of Variables: 1303
- ✓ Number of single equations: 1408
- ✓ Solver CPU time: 67.54 seconds (1% relative optimality gap)



## ❖ *Allowing:*

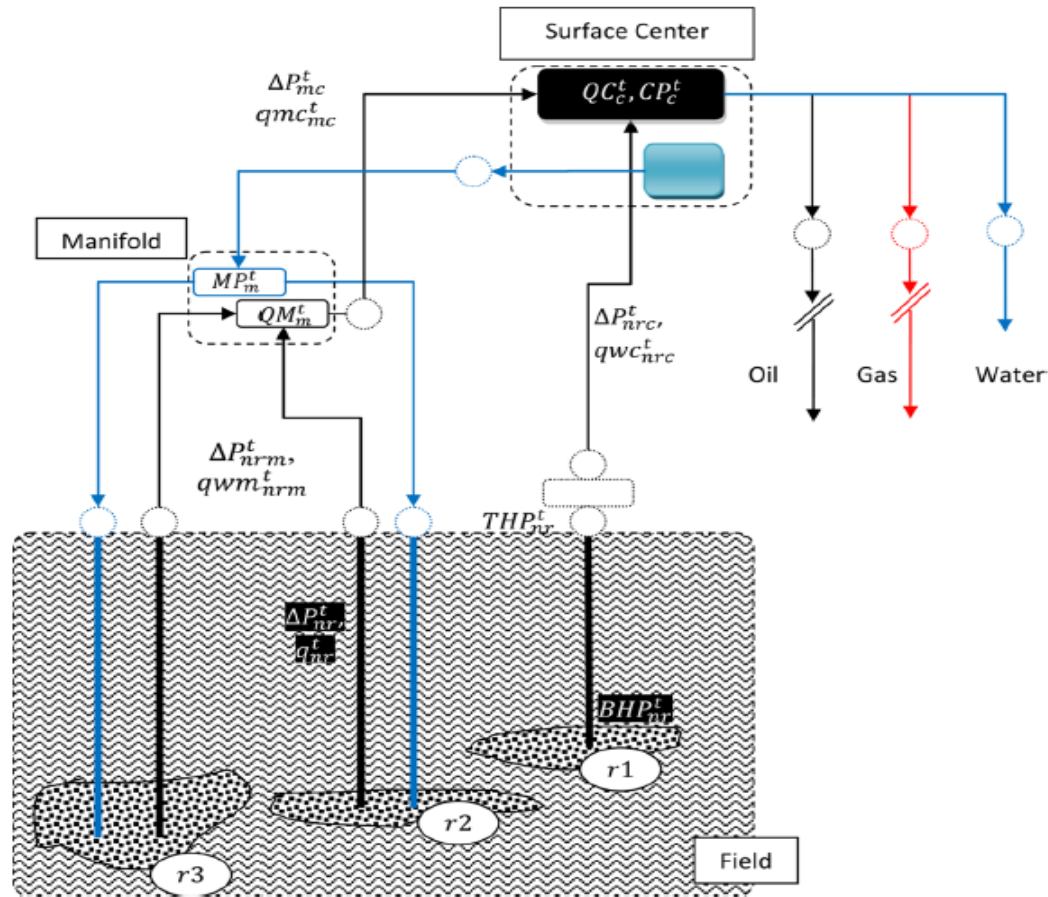
- Reservoir may have arbitrary and irregular shapes.
- Existing manifolds and centers can make/receive new connections.
- Processing centers can receive fluids from wells directly or through manifolds.

## ❖ *Following:*

- Each well must be beyond some minimum distance from all other wells.
- A well that hits its water-cut limit is shut in.

## ❖ *Assumptions:*

- Reservoirs are horizontal and planar. Field surface elevation may vary from point to point.
- Wells are vertical, can pass through multiple reservoirs, but can be perforated to access only one reservoir.
- A wellhead may be connected to one or more manifolds/ centers.
- Each well(existing or potential) is preallocated to some manifolds/centers (existing or potential) based on distance, from which best allocations will be selected.
- Each reservoir may have different pressure and saturation distribution.



Schematic of a hydrocarbon field, with three different reservoirs in the same field. *Blue lines* are injector wells and *black lines* are producer wells.

## ❖ Given:

- Geological information such as dimensions, porosity, permeability.
- PVT information such as formation volume factor and fluid properties.
- Existing wells and their types.
- Minimum allowable well to well distance.
- Operational data such as water cut limits, max injection pressure, capacity expansion plans for surface facilities.
- Production horizons for 'H' years.
- Demand curve, drilling budget and costs.

## ❖ Obtain:

- **Number and location of new producer wells and their production profiles.**
- Number and location of manifolds and processing centers and incremental capacity expansion plan for surface processing centers.
- Potential well-to-manifold, well-to-surface, and manifold-to-surface-center allocations.
- Dynamic pressure profiles along the network at processing centers, manifolds, wellheads, well bore holes.
- Dynamic pressure and saturation profiles for each reservoir.

## Model:

### ❖ Maximize NPV

#### considering

- Reservoir Dynamics and spatial discretization
- Drilling and infrastructure Design Decisions
- Well and surface Network flow management

### ❖ Solution Strategy: Using the Modified Outer Approximation Algorithm



## Dynamic multiphase flow in a reservoir

$$\frac{\partial}{\partial t} \left[ \varepsilon \frac{S_f}{B_f} \right] + q_f - \nabla \cdot \left[ \frac{k r_f}{\mu_f B_f} \mathbf{K} \left( \nabla P_f - \rho_f \frac{\mathbf{g}}{g_c} \nabla z \right) \right] = 0$$

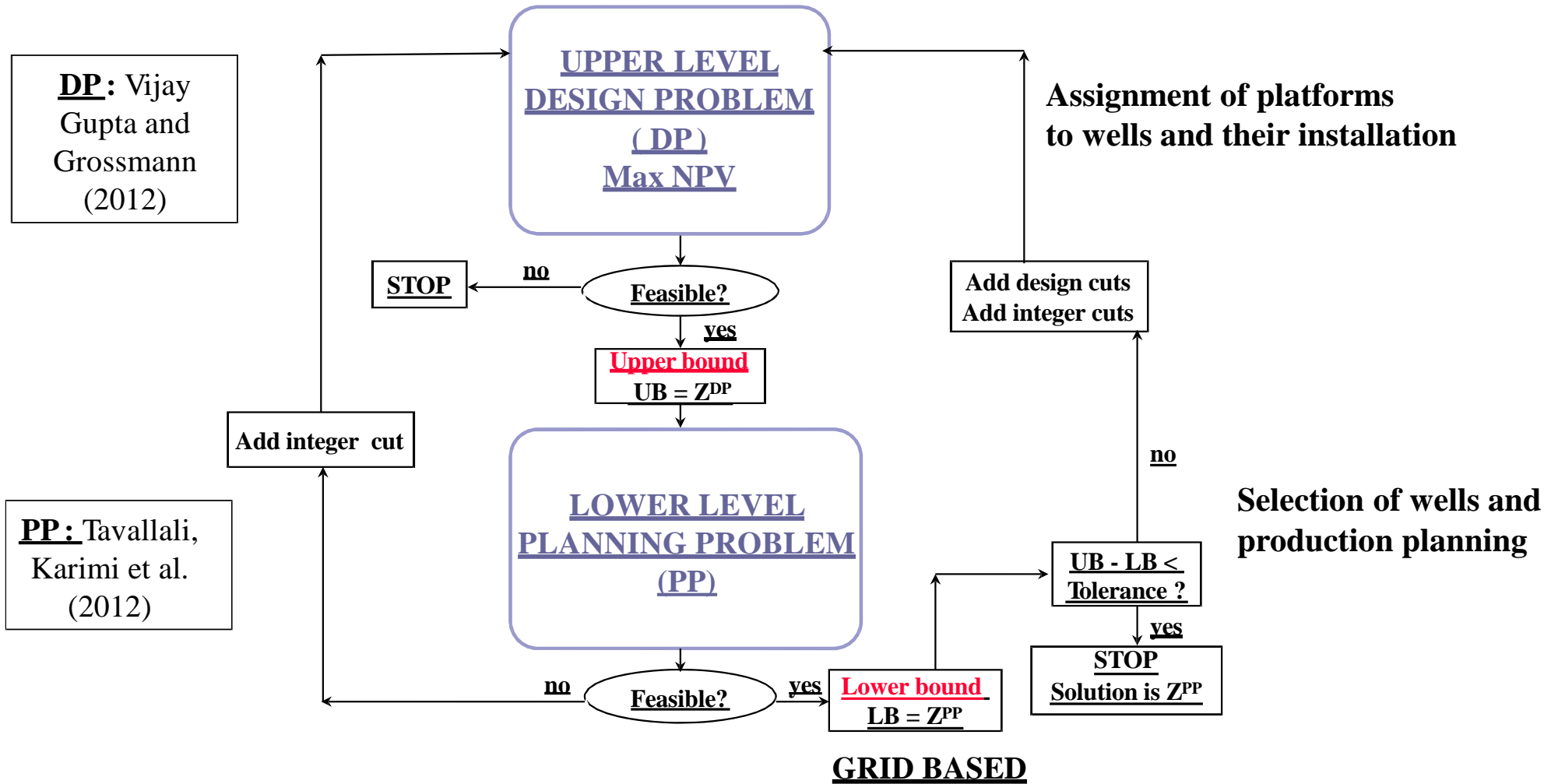
## Backward finite difference approximation

$$\begin{aligned} & \left( \frac{V_n}{dh^t} \right) \{ d_{o,1,n}^t [P_n^t - P_n^{t-1}] + d_{o,2,n}^t [S_n^t - S_n^{t-1}] \} + q_{0,n \notin \text{IW}}^t \\ & + ( \{ M_{o,x-}^t \cdot T_{n-1}^x \cdot [P_n^t - P_{n-1}^t] \}_{(n-1) \in \text{IX}} + \{ M_{o,x+}^t \cdot T_n^x \cdot [P_n^t - P_{n+1}^t] \}_{n \in \text{IX}} \\ & + \{ M_{o,y-}^t \cdot T_{n-1}^y \cdot [P_n^t - P_{n-1}^t] \}_{(n-1) \in \text{IY}} + \{ M_{o,y+}^t \cdot T_n^y \cdot [P_n^t - P_{n+1}^t] \}_{n \in \text{IY}} ) \\ & = 0 \end{aligned}$$

- Binary variable :  $y(n) \rightarrow 1$  if a well should exist in cell 'n'
- Empirical equations for estimating BHP.
- Allow upstream mobility values for convective flows to be chosen dynamically based on pressure time map at time (t-1).

## 2-D discretization of reservoir

N1	N2	N3	N4
N5	N6	N7	N8
N9	N10	N11	N12
N13	N14	N15	N16



- Two-level Optimization approach
  - Upper level minimization of error (with data)  
 $\min \phi(u,v,\Theta)$   
s.t.  $\max \text{NPV}(u,v,\Theta)$  Lower level maximization NPV  
s.t.  $g(u,v,\Theta) \leq 0$   
Fitting error  $\phi(\Theta) = \frac{1}{2}(u-u^\alpha)^2$   
select  $\Theta$  to minimize the error function.
  - Lower level optimization of model (as shown in previous slide)

This approach ensures that we are not compromising on the number of degrees of freedom.

- ❖ Model development for Production planning:
  - Add Gas lift operations to the model.
  
- ❖ Well placement model:
  - Implementation of an improved optimization approach in the well placement model.
  - Validation of the results from historical production data and ECLIPSE simulation.
  - Integration of PETEX suite for well simulations.