

PrOMMiS overview

Advances in Modeling Capabilities for Critical Mineral Separation Technologies

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NETL

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Disclaimer

This presentation and comments are based on my personal experiences

**Please note that they are not the official statement by Department of
Energy/NETL**



A little bit about myself...

- **Ph.D. in Chemical Engineering – CMU**
 - Process optimization
- **ExxonMobil Upstream Research Company (Houston, TX)**
 - Supply chain optimization
- **ExxonMobil Research & Engineering (Fairfax, VA)**
 - Refinery scheduling optimization
- **BASF (Florham Park, NJ)**
 - Operations research manager
- **NETL – Systems Analysis / Research & Innovation Center (Pittsburgh, PA)**
 - Process Systems Engineering

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- **University of Wisconsin:** Victor Zavala Tejeda (PI), Joe Flory

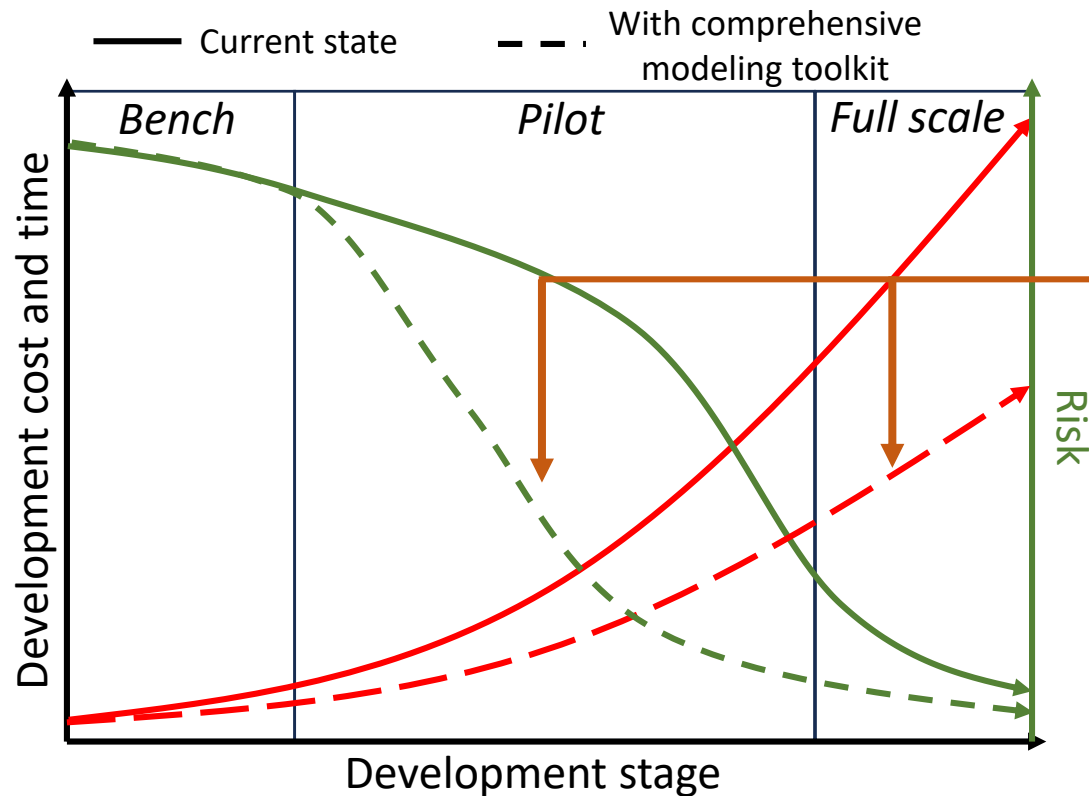
PrOMMiS: Process Optimization and Modeling for Minerals Sustainability



PROMMIS
Process Optimization and Modeling
for Minerals Sustainability

Objective: Accelerate scale-up and deployment of innovative CM & REE processes and establish the toolkit to compress future RD timelines by leveraging IDAES and a decade of DOE CM & REE investment.

Typical R&D roadmap and blocks



Prior DOE investments

CM & REE process experience



Process modeling capabilities



PROMMIS

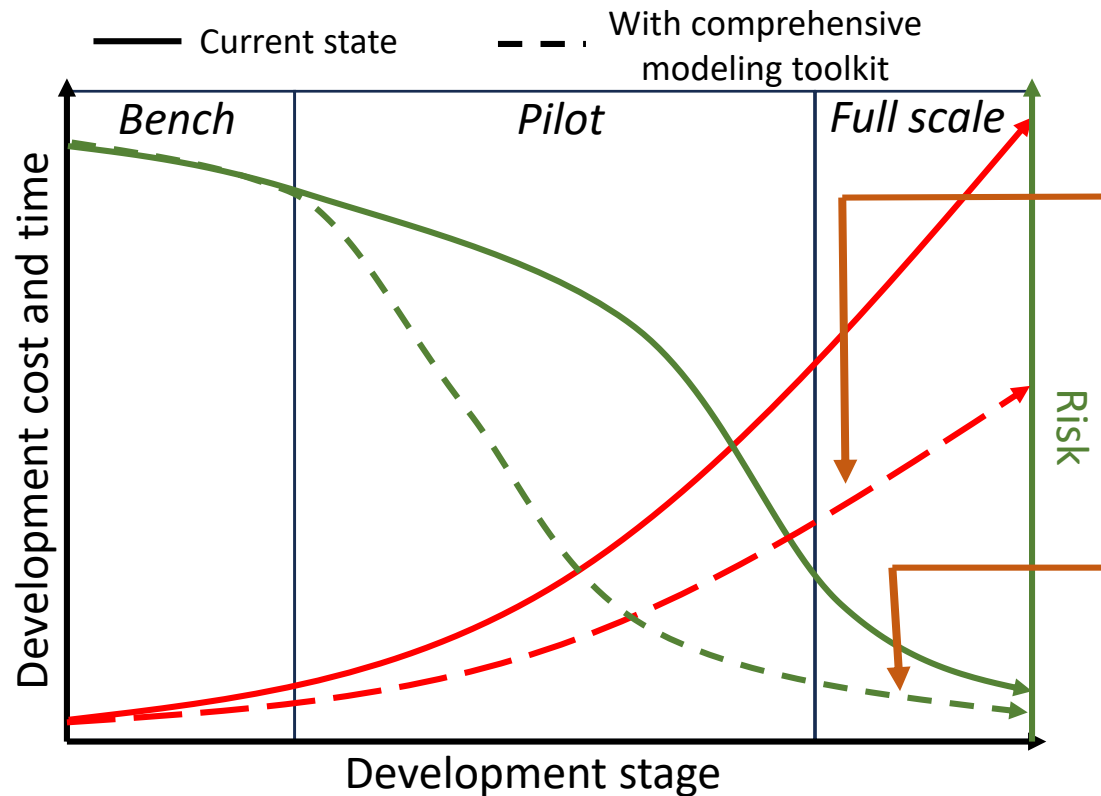
A long-lasting tool set for accelerating development of CM & REE technologies

- Open-source
- Equation-oriented
- Multi-hierarchical
- Unified modeling structure

PrOMMiS: Process Optimization and Modeling for Minerals Sustainability

Objective: Accelerate scale-up and deployment of innovative CM & REE processes and establish the toolkit to compress future RD timelines by leveraging IDEAS and a decade of DOE CM & REE investment.

Typical R&D roadmap and blocks



1. Simulating and optimizing process design and operation
2. Reduce risk from uncertainties in process design, feedstock, etc.
3. Enable workforce development for future CM & REE facilities
4. Enable long-term planning for process integration and supply chain planning

1. Optimize separation processes trains
2. Quantify parameter and process uncertainty
3. Reduce manufacturing inconsistency risk

Reduce modeling timeline



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Framework



Properties:

- Implemented as modular blocks
- Flexibility to choose state variables, use different property packages in the same flowsheet
- Flexible formulation of equations

Ports:

- Can connect to any other Port with the same members automatically
- Translator blocks to connect Ports with different state variables

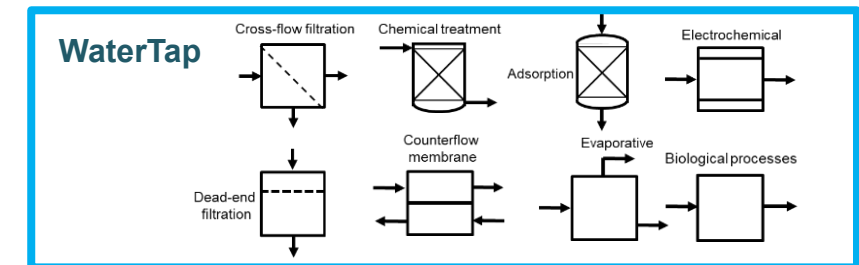
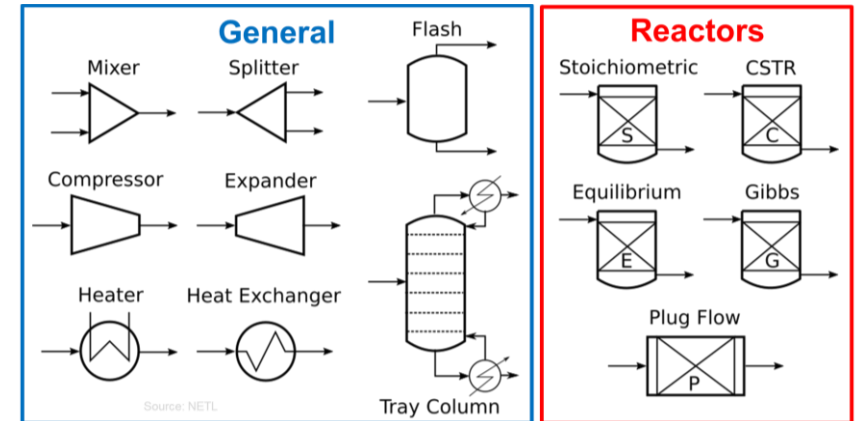
Control Volumes:

- Control Volumes can be connected together to develop complex multi-scale models
- Prebuilt **methods** for common forms of **balance equations**

Initialization:

- Custom initialization routines
 - Reliability and convergence tools
- IDAES diagnostics toolset (structural analysis, ...)

Extensive model and property library





Standardize costing utilizing NETL's QGESS

Data Management

NETL QGESS
Reports¹

FEED Studies

Legacy Models

Public
References



Costing Correlations – Equipment

Excel

Step 1: Identify/select reference source to obtain RP, RC, EXP values
Step 2: Fit data for a given expression (Guthrie's method)
Step 3: Validation/Verification to system

$$SC = RC \left(\frac{SP}{RP} \right)^{EXP} \quad EXP = \frac{\ln \left(\frac{RC1}{RC2} \right)}{\ln \left(\frac{RP1}{RP2} \right)}$$

SC: Scaled Bare Erected Cost
RC: Reference Bare Erected Cost
SP: Scaled Parameter
RP: Reference Parameter
EXP: Cost scaling exponent

Obtained from
reference source

Obtained from multiple data
points of reference source,
or typical values



Implementation

Excel



Python Dictionary



IDAES Costing
Framework



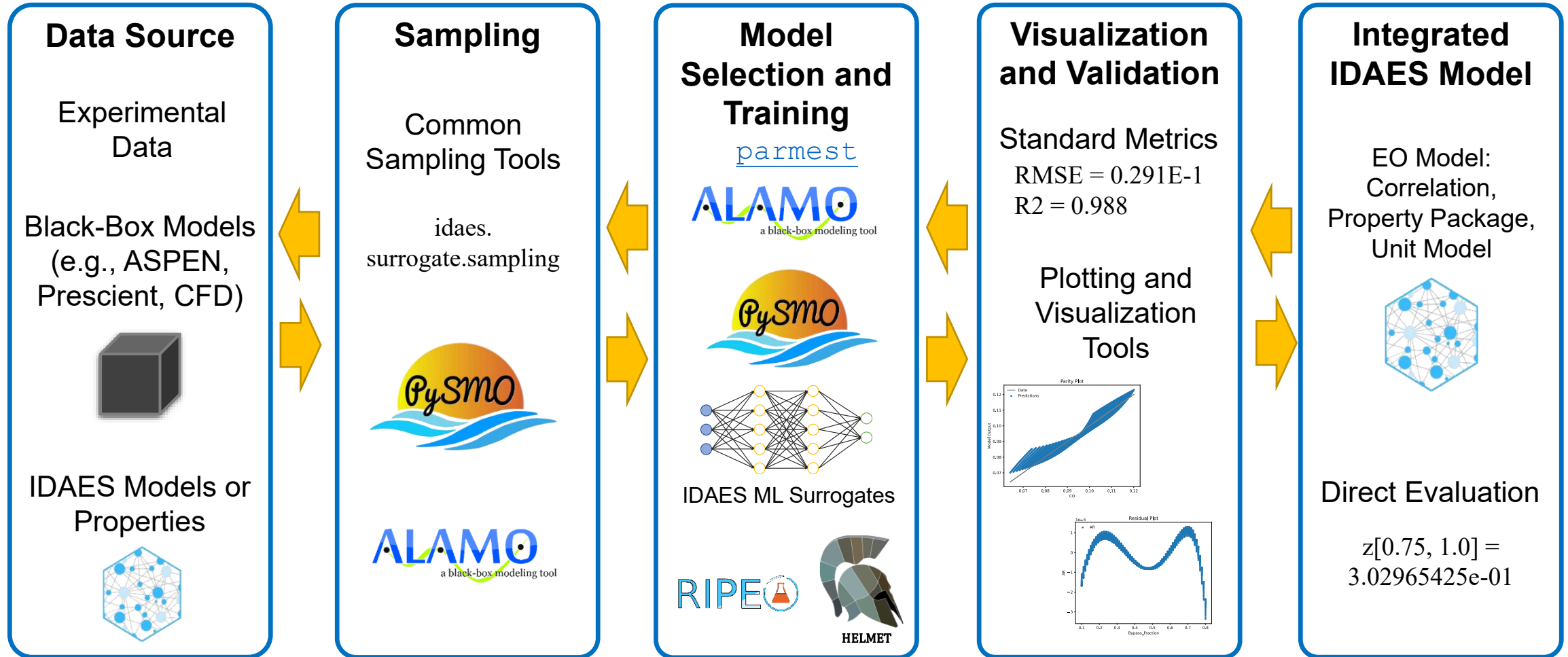
Total Plant Costing &
Optimization

¹ NETL's QGESS: Capital Cost Scaling Methodology Revision 4

Data driven model parametrization and development



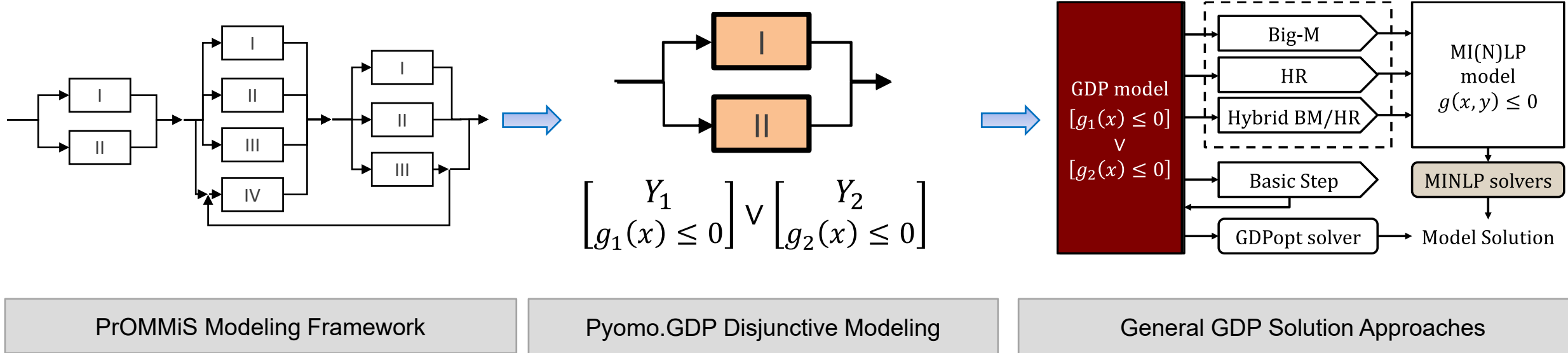
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Automated design of optimal separation trains



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- Models built using IDAES framework and process model library
- High-level representation of superstructure with disjunctions
- Automatic conversion to MINLP with Pyomo.GDP
- Gives access to rigorous, competitive MINLP solvers



IDAES
Institute for the Design of
Advanced Energy Systems





Design of processes under uncertainty

Industrial processes must be able to perform satisfactorily in light of **model uncertainties**.

Two types of variables in **robust process design**:

- **Design Variables** (set during construction):
 - Membrane stage length
- **Control Variables** (adjustable during operation):
 - Flows (feed, diafiltrate, recycle, products)

Potential Sources of Uncertainty

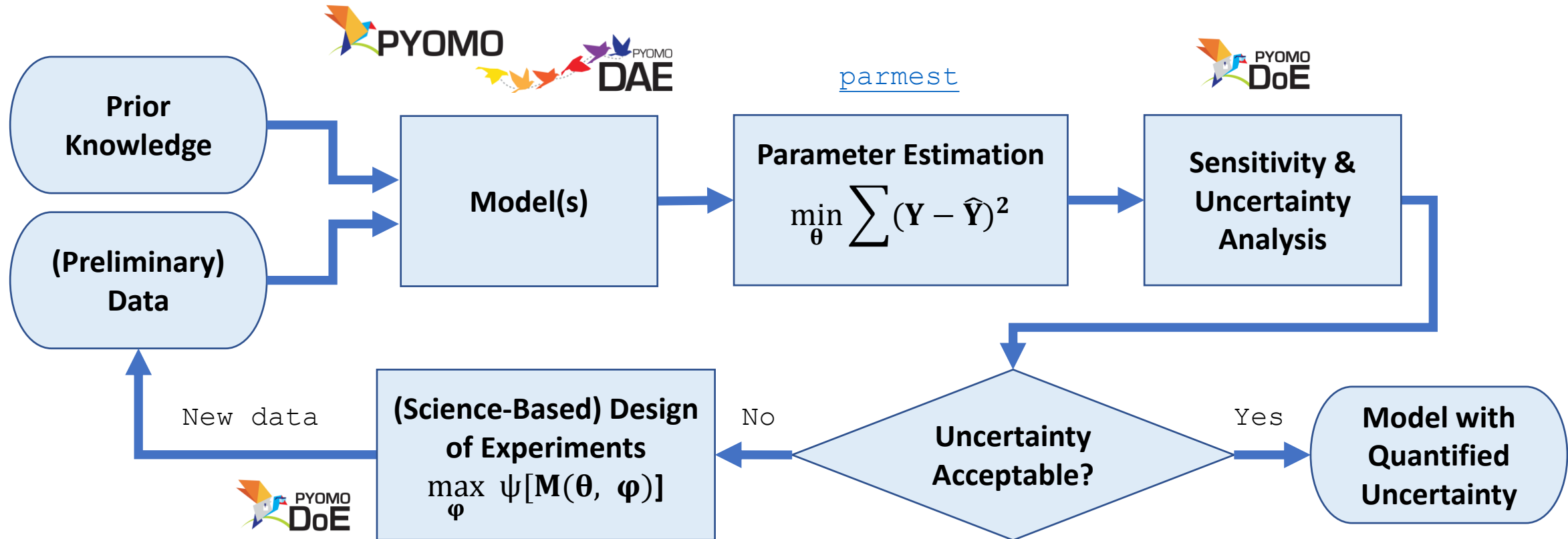
- Location and rate of **fouling**
- **Feedstock** flow rate and solute concentrations
- **Manufacturing variation**
 - Seek to ensure optimal performance for up to N units underperforming

Pyomo Robust Optimization Solver (PyROS) can obtain **robust optimal solutions** that are feasible for all realizations of uncertainty^[3,4]

$$\begin{array}{lll} \min_{x \in \mathcal{X}} & \max_{q \in Q} & \min_{\substack{z \in \mathbb{R}^{n_z}, \\ y \in \mathbb{R}^{n_y}}} & f_1(x) + f_2(x, z, y, q) \\ & & \text{s.t.} & g_i(x, z, y, q) \leq 0 & \forall i \in \mathcal{I} \\ & & & h_j(x, z, y, q) = 0 & \forall j \in \mathcal{J} \end{array}$$



Accelerated experimental efforts



θ = unknown parameters (sieving coefficients), $\hat{Y}$ = model prediction of measured variables, Y = observed values of measured variables, M = Fischer information matrix, ϕ = design vector containing control variables, ψ = scalar measure (determinant/trace/minimum eigenvalue)



Integration with advanced chemistry models

Reaktoro is a platform for simulation of chemical reactions:

- Access to large number of databases
- Access to a number of activity models
- Estimates a large number of chemical, thermodynamic, and aqueous properties

Provides access to direct derivatives as a function of user inputs:

- Enables integration into Pyomo via Graybox modeling approach

OLI cloud API integration



Reaktoro-PSE

Inputs from
Pyomo
model



Reaktoro
for Python and C++

Output property
values

Jacobian

IPOPT

- Available on WaterTAP-org GitHub:
<https://github.com/watertap-org/reaktoro-pse>

Leveraging existing PSE+ tools for PrOMMiS



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DOE developed modeling toolkit

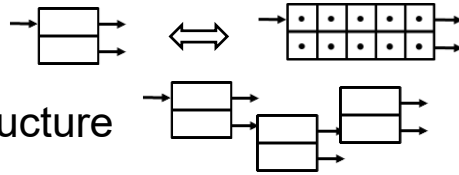


IDAES
Institute for the Design of
Advanced Energy Systems

- Open-source
- Equation oriented
- Multi-hierarchical
- Unified modeling structure



$$f(x) = 0$$



Rich model libraries



IDAES : Common unit operations



: Water treatment unit operations



PrOMMiS : CM & REE unit models

Advanced capabilities

Model fitting tools
Surrogate model tools
Superstructure optimization
Robust Optimization
Science based design of experiments
External chemistry software integration



PySTAR



PyROS



Open source and accessible

Publicly accessible on GitHub

- <https://github.com/Pyomo>
- <https://github.com/IDAES>
- <https://github.com/watertap-org>
- <https://github.com/prommis>



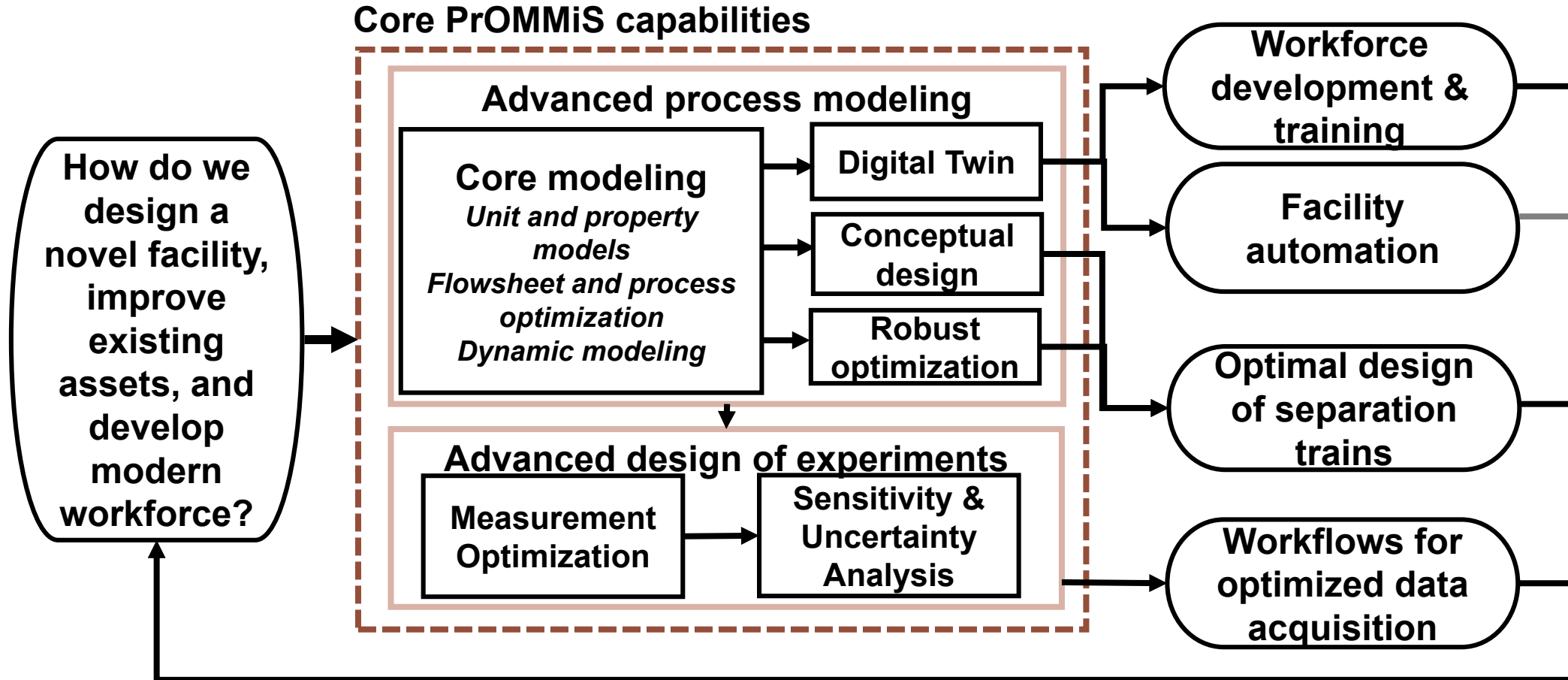
User interfaces

- Code based interface (primary)
- Limited graphical user interface (secondary)

PrOMMiS core capabilities

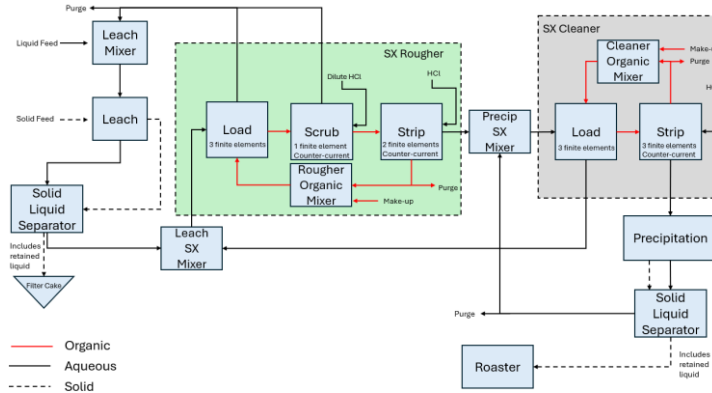


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PrOMMiS case studies

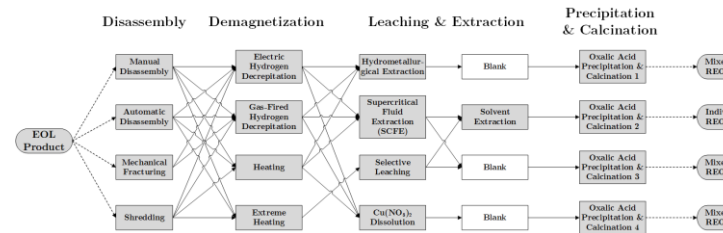
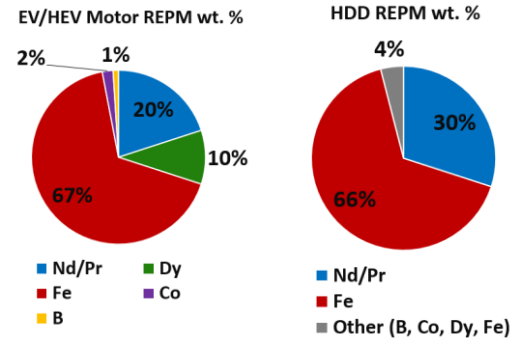
University of Kentucky pilot



- Model library
- Costing library
- Model fitting tools
- Superstructure optimization
- Surrogate model tools



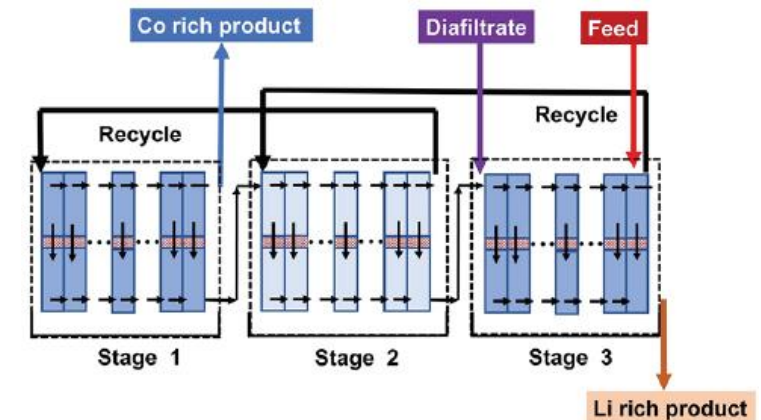
End Of Life CM recovery



Superstructure optimization



Separation of Lithium and cobalt through diafiltration



- Robust Optimization
- Science based design of experiments



Code base tutorial

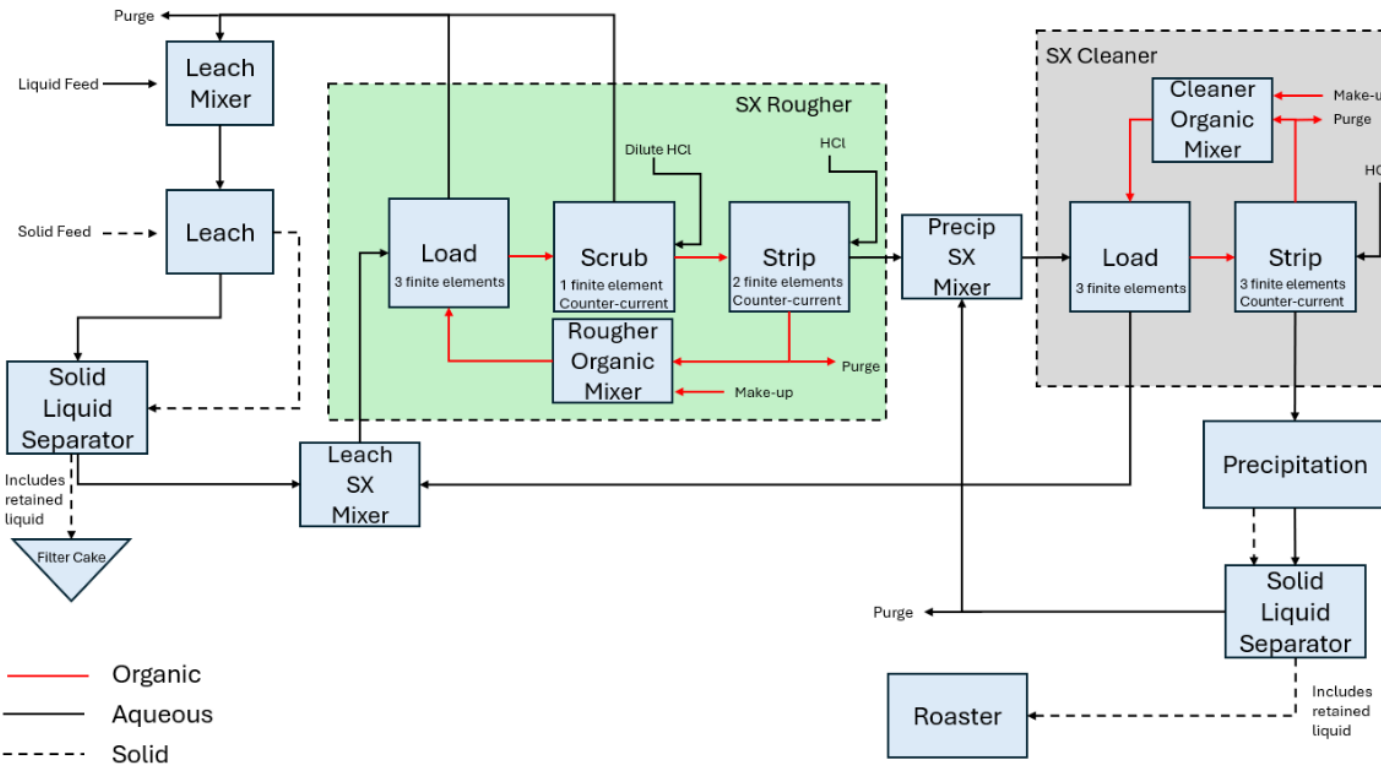


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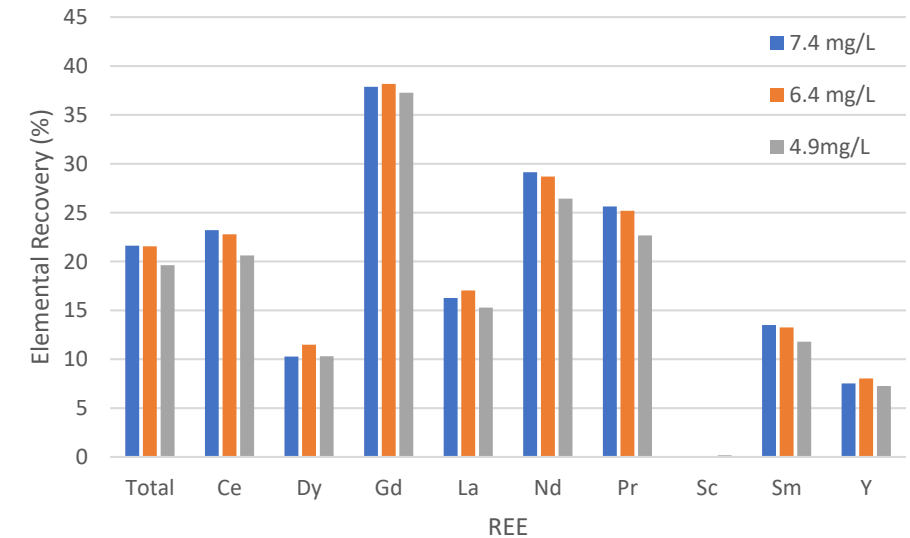
UKy Flowsheet Tutorial

This tutorial will show how to build, initialize, and simulate the West Kentucky No.13 Coal Refuse flowsheet. The inputs into this flowsheet are case study-specific, so users should not expect the flowsheet to solve if the values are significantly altered.

- Useful Links:
 - Public Github Repository: <https://github.com/prommis/prommis/tree/main>
 - UKy Flowsheet Code: https://github.com/prommis/prommis/blob/main/src/prommis/uky/uky_flowsheet.py



Precipitator recovery vs. Oxalic Acid Dosage



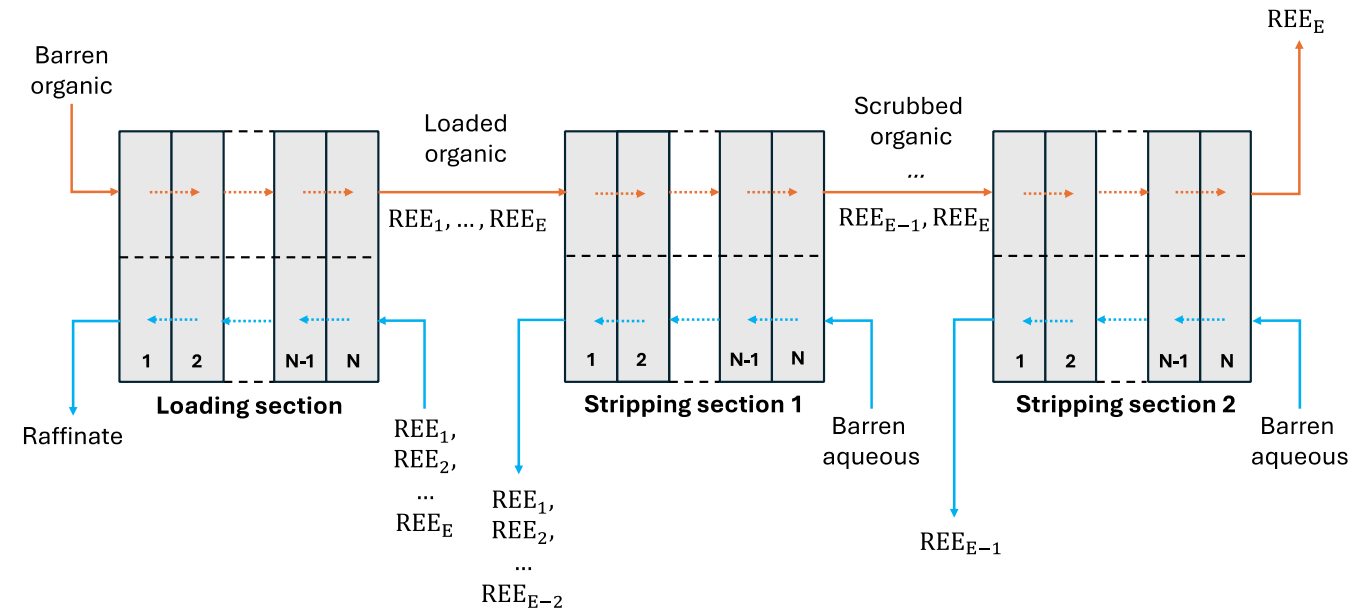
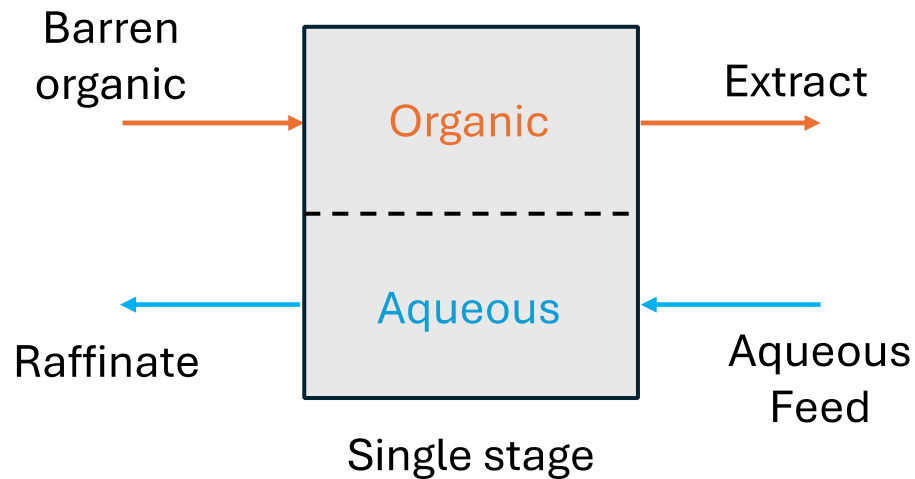
https://github.com/prommis/prommis/blob/main/docs/tutorials/uky_flowsheet-solution.ipynb

Conceptual Design of Solvent Extraction



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- Solvent extraction refers to the distribution of solute between two *immiscible phases*
 - The system does not form a single phase after mixing

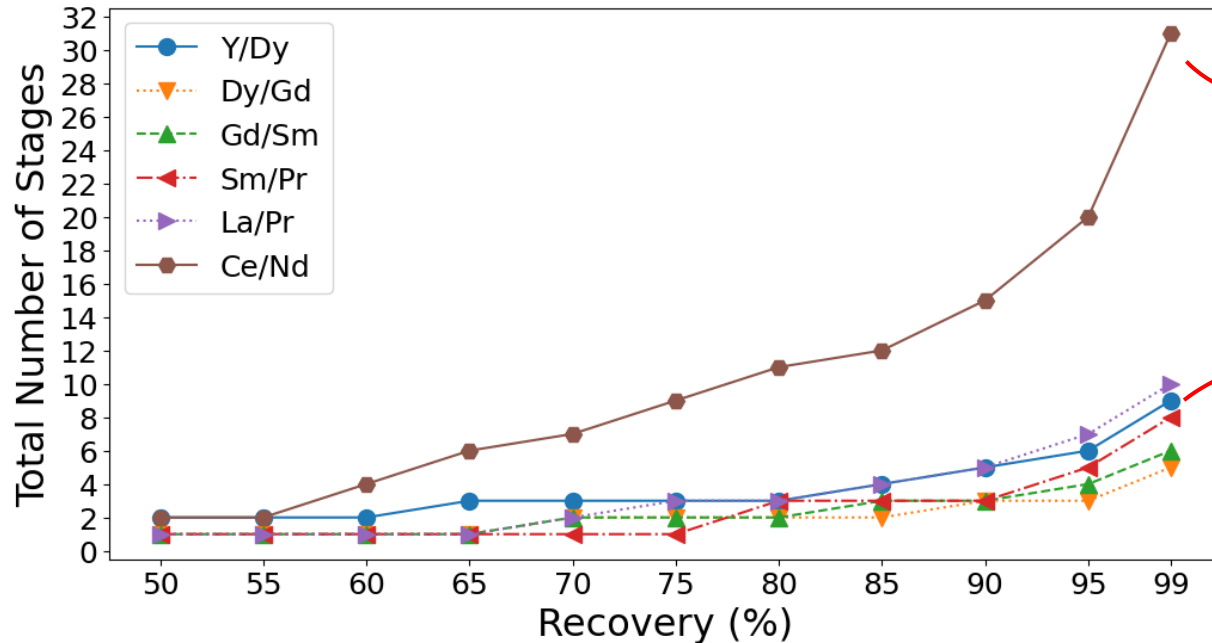


Conceptual Design of Solvent Extraction



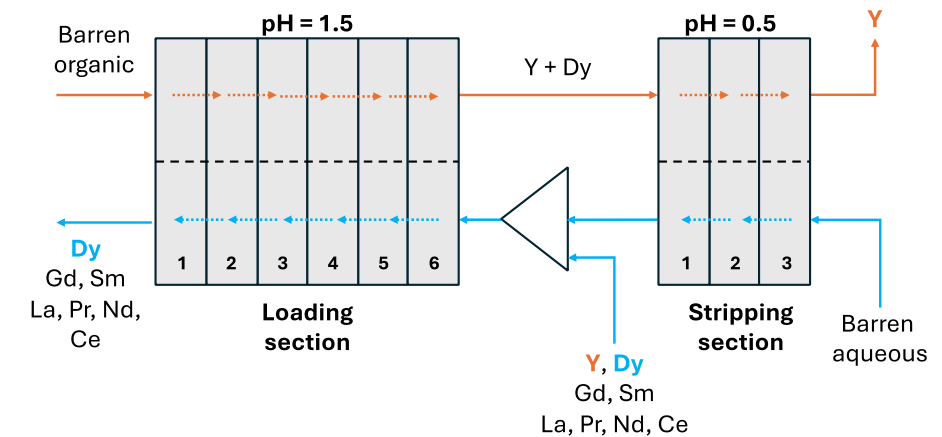
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5% DEPHA 10% TBP



Solved to global optimality with average runtime of 20s per node

Cerium (Ce) – Neodymium (Nd) Separation		
85%	7 L.Stages at pH 5.0,	5 S.Stage at pH 2.5
90%	10 L.Stages at pH 5.0,	5 S.Stage at pH 2.0
95%	16 L.Stages at pH 5.0,	4 S.Stage at pH 0.5
99%	14 L.Stages at pH 5.0,	17 S.Stages at pH 3.0



Enhancement of costing libraries

Front End Loader (2 yd ³)	Front End Loader (10 yd ³)	Bucket Elevator	Jaw Crusher	VSI Crusher	Roll Crusher
Vibrating Screen	Storage Bins	Dry Ball Mill	PE Tanks	Steel Tanks	Tank Mixer
Elevator Motor	Process/Slurry Pump	Thickener	Filter Press	Conveyor	Roaster
Gas Scrubber	Spray Chamber Quencher (77k-60k cfm)	Spray Chamber Quencher (60k-230k cfm)	Chiller	Solution Heater	Belt Filter
BioLeach Tanks	Blower	Mixer Settler	HDD Recycling Shredder (2700 drives/hour)	HDD Recycling Furnace (Hydrogen Decrepitation)	Membranes*
	Nanofiltration*	Reverse Osmosis*	Ion Exchange*		

References:

- ² Keim, Steven Anthony, and Naumann, Hans. Production of Salable Rare Earths Products from Coal and Coal Byproducts in the U.S. Using Advanced Separation Processes (Final Technical Report). United States: N. p., 2019. Web. doi:10.2172/1569277.
- ³ Honaker, Rick, Werner, Joshua, Yang, Xinbo, Zhang, Wencai, Noble, Aaron, Yoon, Roe-Hoan, Luttrell, Gerald, and Huang, Qingqing. **Pilot-Scale Testing of an Integrated Circuit for the Extraction of Rare Earth Minerals and Elements from Coal and Coal Byproducts Using Advanced Separation Technologies**. United States: N. p., 2021. Web.
- ⁴ Honaker, Rick Q., Werner, Joshua, Nawab, Ahmad, Zhang, Wencai, Noble, Aaron, Free, Michael, and Yang, Xinbo. **Demonstration of Scaled-Production of Rare Earth Oxides and Critical Materials from U. S. Coal-Based Sources (Final Report)**. United States: N. p., 2023. Web. doi:10.2172/1971736.
- ⁵ Garrett, D.E. (1989). Chemical Engineering Economics.
- ⁶ Ames National Laboratory. (2020, March 26). It's all part of the Grind: CMI's new hard drive Shredder serves up plenty of material for recycling science. Ames Laboratory. <https://www.ameslab.gov/news/it-s-all-part-of-the-grind-cmi-s-new-hard-drive-shredder-serves-up-plenty-of-material-for>
- ⁷ Loh, H.P., Lyons, Jennifer, White, Charles W.. Process Equipment Cost Estimation Final Report. United States: N. P., 2002. Web.

PrOMMiS Costing Library:

$$SC_i = \alpha_i * RP_i^{Exp_i}$$

- SC – scaled cost
- α – reference cost / performance
- RP – reference parameter
- Exp – exponential factor
- i – ith unit operations in the library

* WaterTap library

Costing results and tutorial



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REE Costing Framework Part 3 - UKy Flowsheet Demo

The purpose of this tutorial is to demonstrate defining, adding, and solving costing for the University of Kentucky flowsheet. It is assumed that the user is already familiar with the flowsheet, which is introduced in detail in the [UKy Flowsheet Tutorial](#). The user should have an understanding of the basic features and structure of the costing framework in PROMMIS, which is introduced in detail in [Part 1](#) of this tutorial.

The tutorial will take users through the following:

- Adding capital costing to equipment in an existing flowsheet
- Build total plant and operating costs

Useful Links:

- Public GitHub Repository: <https://github.com/prommis/prommis/tree/main>
- REE Costing Module Code: <https://github.com/prommis/prommis/blob/main/src/prommis/uky/costing/re>

1 Import the necessary tools

First, import the required Python, Pyomo, IDAES, and PROMMIS packages. These will be implemented at various

For installation instructions, please refer to the public GitHub repository linked above.

Total bare erected cost (MUSD): 49.632
Total overnight (installed) equipment cost:
Total annualized capital cost (MUSD): 16.898

Total annual fixed O&M cost (MUSD): 11.325
Total annual variable O&M cost (MUSD): 4.182
Total annual O&M cost (MUSD): 15.507
Total annual O&M cost per kg REE recovered (USD/kg): 54.127

Total annualized plant cost (MUSD): 32.405
Annual rate of recovery (kg/year): 286493.408
Cost of recovery per kg REE recovered (USD/kg): 113.110

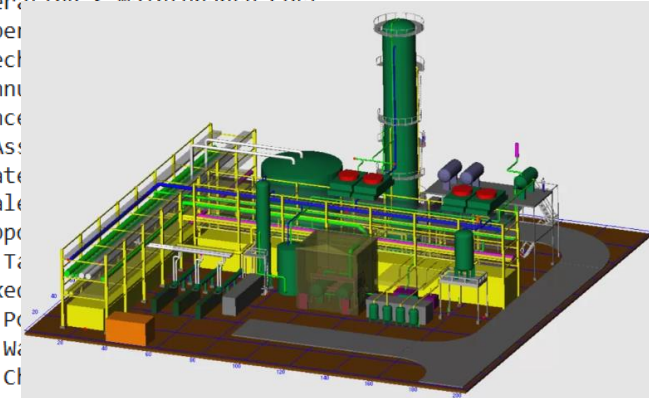
ProMMiS Costing Library:

$$SC_i = \alpha_i * RP_i^{Exp_i}$$

- SC – scaled cost
- α – reference cost / performance
- RP – reference parameter
- Exp – exponential factor
- i – i^{th} unit operations in the library

costing

	Value
Plant Cost Units	MUSD_2023
Total Plant Cost	147.42
Total Bare Erected Cost	49.632
Total Installation Cost	97.776
Total Other Plant Costs	0.0083065
Total Fixed Operating & Maintenance Cost	11.325
Total Annual Operating & Maintenance Cost	3.8090
Total Annual Technical Support Cost	1.8294
Summation of Annual Operating & Maintenance Cost	5.6384
Total Maintenance Cost	2.9483
Total Quality Assurance Cost	0.38090
Total Sales, Patent & Royalty Cost	0.12106
Summation of Sales, Patent & Royalty Cost	2.3570
Total Admin Support Cost	0.76181
Total Property Tax Cost	1.4742
Total Other Fixed Costs	1.0000e-12
Total Variable Plant Costs	0.38536
Total Variable Working Capital Costs	5.1396e-06
Total Variable Costs	0.0000
General Plant Overhead Cost	2.5845
Total Plant Overhead Cost, Including Maintenance & Quality Assurance	5.9137
Total Variable Operating & Maintenance Cost	4.1823
Total Land Cost	1.2124
Total Sales Revenue Cost	24.211
Cost of Recovery (USD/kg REE)	113.11



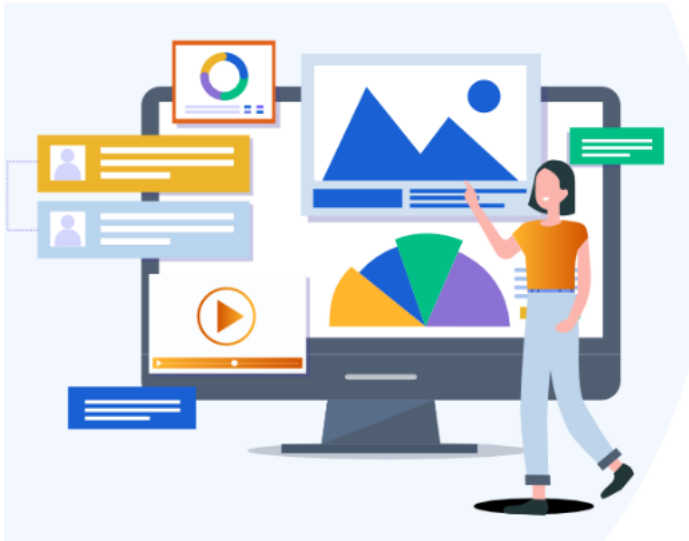
https://github.com/prommis/prommis/blob/ad8ef5e79740ef073f6ce2b797712cb04040ad8b/docs/tutorials/ree_costing_framework_uky_flowsheet_demo-solution.ipynb

Developed flowsheet runner UI



PROMMIS
Process Optimization and Modeling
for Minerals Sustainability

- One-click native install
- Lowers the barrier for new users to run PrOMMiS optimizations
- Provides a vehicle for outreach and tutorials
- Mechanism for facilitating collaboration with partners (without requiring Python-coding expertise)



UKy

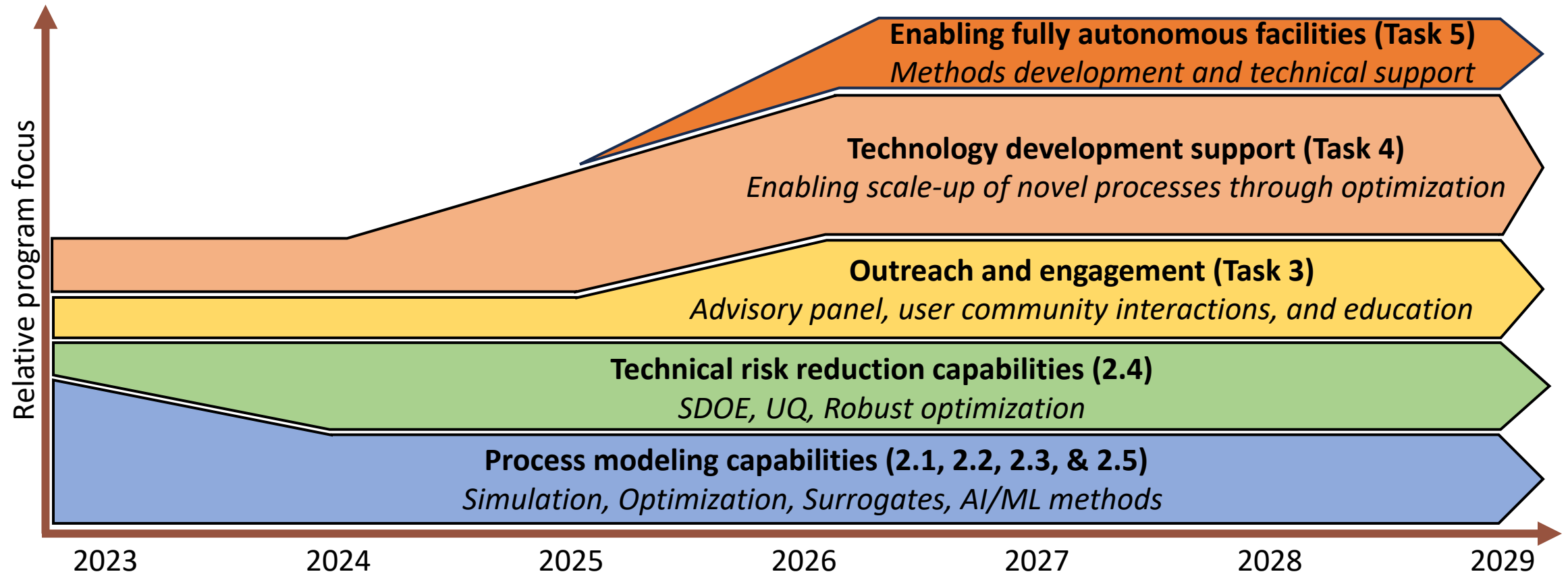
DEGREES OF FREEDOM: 0

The screenshot displays the Flowsheet Processor UI. At the top, a process flowsheet is shown with various unit operations like Leach, Load, Scrub, Strip, SX Washer, SX Cleaner, Organic, and Precipitation, connected by streams. Below the flowsheet are three tabs: INPUT, OUTPUT, and COMPARE. The INPUT tab is active, showing two main sections: 'Leaching liquid feed' and 'Leaching solid feed'. Each section contains several input fields with values and units, and a 'Fixed' dropdown menu. The 'Leaching liquid feed' section includes: Leach liquid feed rate (224.3 L/h), Leach liquid feed hydrogen (100 mg/L), Leach liquid feed SO4 (4800 mg/L), and Leach liquid feed HSO4 (0 mg/L). The 'Leaching solid feed' section includes: Leach solid feed inerts (0.695), Leach solid feed Y2O3 (0), Leach solid feed Nd2O3 (0), Leach solid feed Gd2O3 (0), Leach solid feed Pr2O3 (0), and Leach solid feed Al2O3 (0.237). At the bottom right, there is an 'Analysis Type' dropdown set to 'optimization', a 'RESET' button, and a 'RUN' button.

Section	Parameter	Value	Unit	Fixed
Leaching liquid feed	Leach liquid feed rate	224.3	L/h	Fixed
	Leach liquid feed hydrogen	100	mg/L	Fixed
	Leach liquid feed SO4	4800	mg/L	Fixed
	Leach liquid feed HSO4	0	mg/L	Fixed
Leaching solid feed	Leach solid feed inerts	0.695		Fixed
	Leach solid feed Y2O3	0		Fixed
	Leach solid feed Nd2O3	0		Fixed
	Leach solid feed Gd2O3	0		Fixed
	Leach solid feed Pr2O3	0		Fixed
	Leach solid feed Al2O3	0.237		Fixed

Flowsheet Processor UI to parameterize and solve existing flowsheets.

PSE+ ecosystem enabled rapid development of PrOMMiS capabilities and focus on application



Conclusion

- **Accomplishments**
 - Empowering industry users with modeling environment
 - Accelerate speed of implementation
 - Open source for collaboration and extension
- **Future Work**
 - Physical/Chemical property model
 - Collaboration for pilot plant
 - Licensing opportunity





Q & A